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# **Turbulence and CFD models: Theory and applications**

# Organization of the lecture notes

- In the first part of this course, we are going to elaborate on the basic theory and many experimental observations.
- Then, we are going to build up on this knowledge to introduce turbulence models in CFD.
- Followed by validation and verification.
- That is, we are going to confirm many experimental and theoretical observations using turbulence models and CFD.
- We are going to address many applications. Ranging from academic cases to complex industrial applications.
- But regardless of the application and software used, the workflow is the same.

# Roadmap to Lecture 2

- 1. The turbulent world around us**
- 2. Turbulence, does it matter?**
- 3. Introduction to turbulence modeling – Basic concepts**
- 4. Wall bounded flows and shear flows**
- 5. A peek to the turbulence closure problem, some correlations in turbulence modeling, and the energy cascade**

# Roadmap to Lecture 2

- 1. The turbulent world around us**
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Leonardo da Vinci pioneered the flow visualization genre about 500 years ago. The illustrations to the left (*Studies of water passing obstacles and falling* c. 1508-1509) represents perhaps the world's first use of visualization as a scientific tool to study a turbulent flow.

The following da Vinci's observation is close to the Reynold's decomposition.

*“Observe the motion of the surface of the water, which resembles that of hair, which has two motions, of which one is caused by the weight of the hair, the other by the direction of the curls; thus, the water has eddying motions, one part of which is due to the principal current, the other to the random and reverse motion.”*

Leonardo da Vinci pioneered the flow visualization genre about 500 years ago. The illustrations to the left (*Studies of water passing obstacles and falling* c. 1508-1509) represents perhaps the world's first use of visualization as a scientific tool to study a turbulent flow.

The following da Vinci's description is maybe the earliest reference to the importance of vortices in fluid motion.

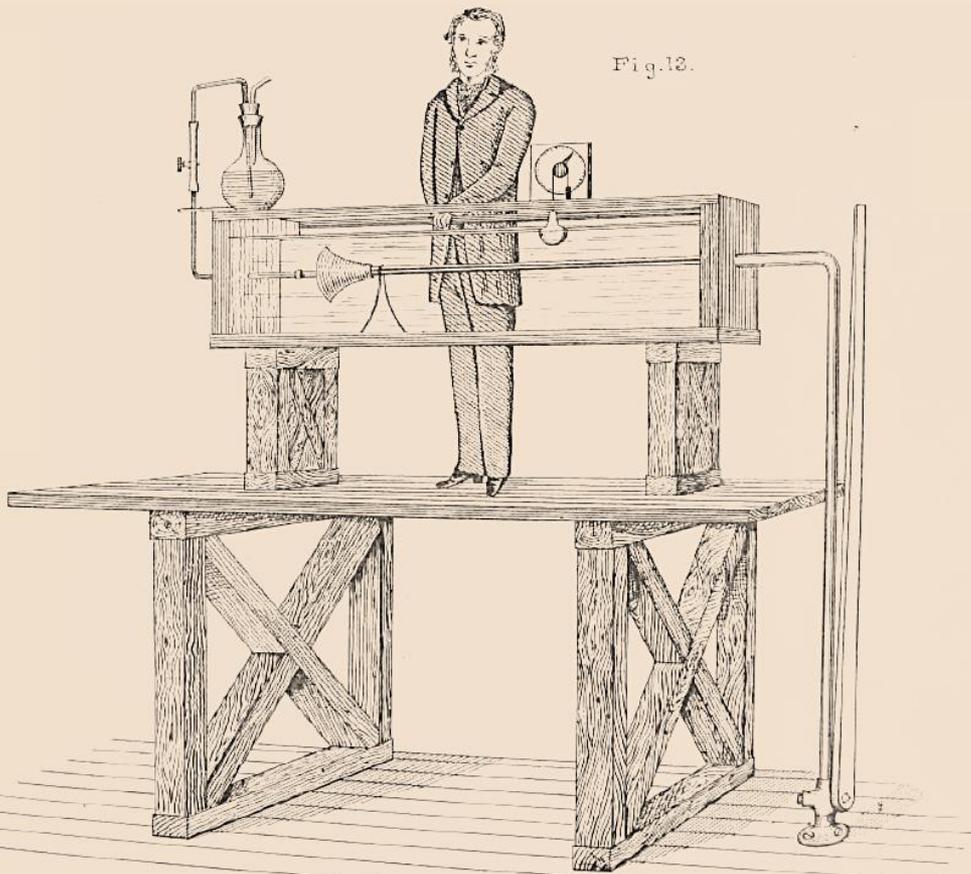
*“So moving water strives to maintain the course pursuant to the power which occasions it and, if it finds an obstacle in its path, completes the span of the course it has commenced by a circular and revolving movement.”*

Leonardo da Vinci pioneered the flow visualization genre about 500 years ago. The illustrations to the left (*Studies of water passing obstacles and falling* c. 1508-1509) represents perhaps the world's first use of visualization as a scientific tool to study a turbulent flow.

The following da Vinci's observation is an analogy to the energy cascade and coherent structures.

*“...the smallest eddies are almost numberless, and large things are rotated only by large eddies and not by small ones and small things are turned by small eddies and large”*

Fig. 12.



In 1883, Osborne Reynolds published his famous paper entitled,

*“An Experimental Investigation of the Circumstances which determine whether Motion of Water shall be Direct or Sinuous and of the Law of Resistance in Parallel Channels.”*

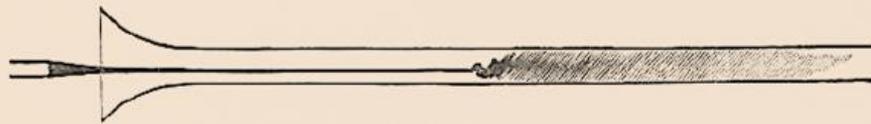
This work had a profound effect on the development of fluid mechanics and hydrodynamic linear stability theory.

In this work, Reynolds introduces a dimensionless group, what we call today the Reynolds number.

Fig. 3.



Fig. 4.



*“It seemed, however, to be certain, if the eddies were owing to one particular cause, that integration would show the birth of eddies to depend upon some definite value of—”*

$$\frac{c\rho U}{\mu}$$

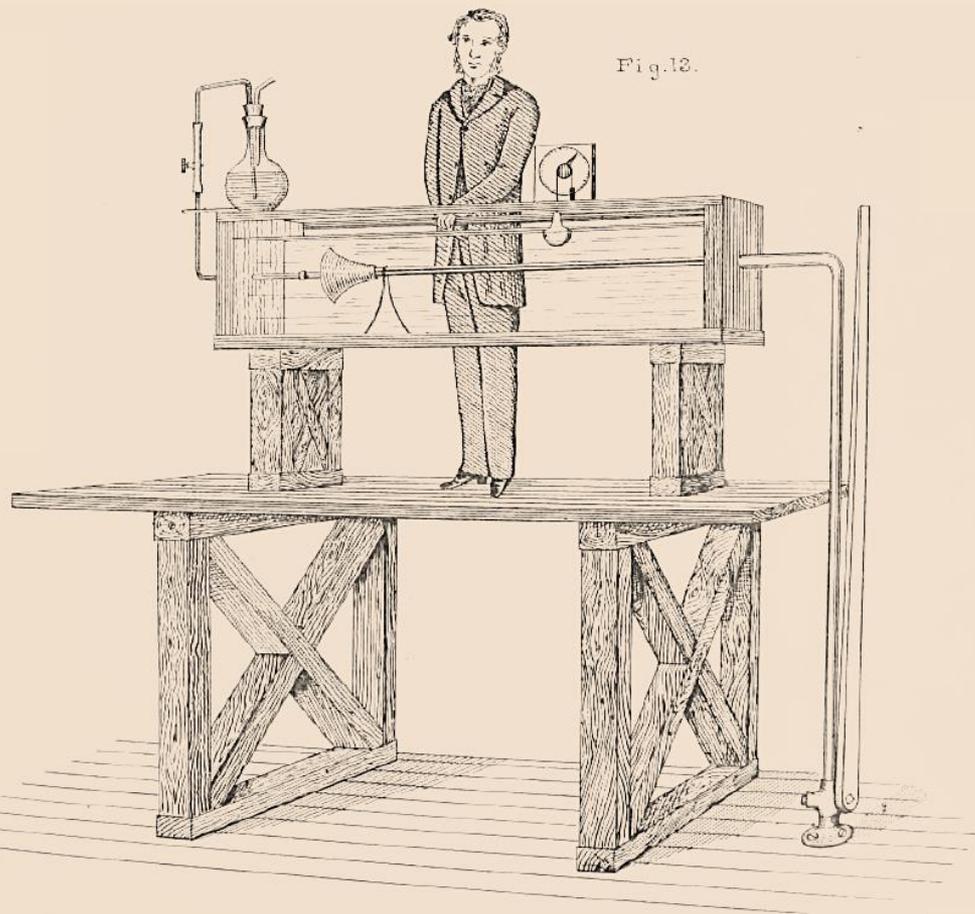


Fig. 12.

In his 1883 paper, Reynolds also writes,

*“Again, the internal motion of water assumes one or other of two broadly distinguishable forms – either the elements of the fluid follow one another along lines of motion which lead in the most direct manner to their destination, or they eddy about in sinuous paths, the most indirect possible.”*

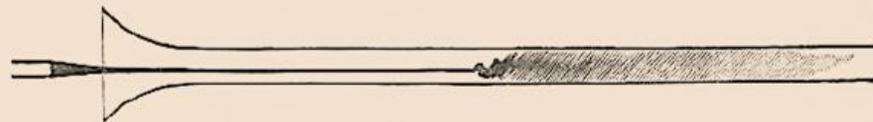
In present-day terminology the direct motion is called laminar. This is a state in which the behavior of a fluid is very regular.

The sinuous paths Reynolds refers to are not sinusoidal (periodic) motions. Instead, they are the ones having many curves and turns, being very irregular. We refer to these flows as turbulent.

Fig. 3.



Fig. 4.



IV. *On the Dynamical Theory of Incompressible Viscous Fluids and the Determination of the Criterion.*

By OSBORNE REYNOLDS, M.A., LL.D., F.R.S., Professor of Engineering in Owens College, Manchester.

Received April 25—Read May 24, 1894.

SECTION I.

*Introduction.*

1. THE equations of motion of viscous fluid (obtained by grafting on certain terms to the abstract equations of the Eulerian form so as to adapt these equations to the case of fluids subject to stresses depending in some hypothetical manner on the rates of distortion, which equations NAVIER\* seems to have first introduced in 1822, and which were much studied by CAUCHY† and POISSON‡) were finally shown by St. VENANT§ and Sir GABRIEL STOKES|| in 1845, to involve no other assumption than that the stresses, other than that of pressure uniform in all directions, are linear functions of the rates of distortion, with a co-efficient depending on the physical state of the fluid.

By obtaining a singular solution of these equations as applied to the case of pendulums in steady periodic motion, Sir G. STOKES¶ was able to compare the theoretical results with the numerous experiments that had been recorded, with the result that the theoretical calculations agreed so closely with the experimental determinations as seemingly to prove the truth of the assumption involved. This was also the result of comparing the flow of water through uniform tubes with the flow calculated from a singular solution of the equations so long as the tubes were small and the velocities slow. On the other hand, these results, both theoretical and practical, were directly at variance with common experience as to the resistance

\* 'Mém. de l'Académie,' vol. 6, p. 389.

† 'Mém. des Savants Étrangers,' vol. 1, p. 40.

‡ 'Mém. de l'Académie,' vol. 10, p. 345.

§ 'B.A. Report,' 1846.

|| 'Cambridge Phil. Trans.,' 1845.

¶ 'Cambridge Phil. Trans.,' vol. 9, 1857.

In a follow up paper published 1895 and titled,

***“On the Dynamical Theory of Incompressible Viscous Fluids and the Determination of the Criterion.”***

Reynolds proposed to take the Navier-Stokes equations as a starting point to derive equations for the evolution of the mean (or average) velocity field. Furthermore, he obtained equations for the evolution of the kinetic energy contained in the mean velocity field, and for the energy contained in the small fluctuation motions.

Without a doubt, the most important result of that paper is the procedure in which the velocity field is decomposed into a mean and a fluctuating part.

This procedure is now referred to as Reynolds averaging and it constitutes the basis for modern simulation techniques like RANS and LES models.

Lensfield Cottage, Cambridge, 31 Oct. 1894.

Dear Lord Rayleigh,

I must plead guilty to not having digested Professor Osborne Reynolds's paper, though much time has passed since it was referred to me.

I find it very difficult to make out what the author's notions are. As far as I can conjecture his meaning, I must say I do not think he has made out his point. He is however an able man, and in his former paper did very good work in showing that the conditions of dynamical similarity which follow from the dimensions of the hydrodynamical equations when viscosity is taken into account are not confined to what I may call regular motions, but continue to apply (in relation to mean effects) even when the motion is of that irregular kind which constituted eddies, and which at first sight appears to defy mathematical treatment. The fact that the author has gone to the expense of printing the paper shows that he himself considers it as of much importance. I confess I am not prepared to endorse that opinion myself, but neither can I say that it may not be true.

I do not know whether these remarks will be of any use in assisting the Council to come to a decision.

Yours very truly,



It is interesting to mention that Reynolds 1895 paper received a hard review from Sir George Gabriel Stokes, one of scientist reviewing the paper.

*“I must plead guilty to not having digested Professor Osborne Reynolds’s paper, though much time has passed since it was referred to me.”*

*“I find it very difficult to make out what the author’s notions are. As far as I can conjecture his meaning, I must say I do not think he has made out his point.”*

Despite this review, Reynolds' paper was published, and it is now seen as a landmark contribution to the field of fluid mechanics, and particularly to the research relating to the behavior of turbulent flows.

# MÉMOIRES

PRÉSENTÉS PAR DIVERS SAVANTS

## A L'ACADÉMIE DES SCIENCES

DE L'INSTITUT NATIONAL DE FRANCE.

TOME XXIII. — N° 1.

### RAPPORT

SUR UN MÉMOIRE DE M. BOUSSINESQ,

PRÉSENTÉ LE 28 OCTOBRE 1872

ET INTITULÉ

ESSAI SUR LA THÉORIE DES EAUX COURANTES.

Commissaires :

MM. Bonnet, Phillips, de Saint-Venant, rapporteur<sup>(1)</sup>.

1. Une première rédaction de ce grand travail a été l'objet d'une lecture faite à l'Académie le 15 avril 1872. Son titre était : *De l'influence des forces centrifuges sur l'écoulement de l'eau dans les canaux prismatiques de grande largeur*<sup>(2)</sup>. On y trouvait l'établissement, sur les bases rationnelles posées dans des notes récentes<sup>(3)</sup>, des équations du mouvement

<sup>(1)</sup> Ce rapport est du 14 avril 1873 (*Comptes rendus des séances de l'Académie des sciences*, t. LXXVI, p. 924).

<sup>(2)</sup> L'extrait est à la page 1026 du tome LXXIV des *Comptes rendus*. Celui de la rédaction nouvelle, du 28 octobre 1872, est à la page 1011 du tome LXXV.

<sup>(3)</sup> Notes des 29 août 1870, 3 et 10 juillet 1871, aux *Comptes rendus*, t. LXXI, p. 389; t. LXXIII, p. 34 et 101.

More than 20 years before Reynolds work, and without formally introducing the stresses resulting from the averaging of the N-S equations, Boussinesq (1872 report and 1877 publication) proposed to account for the effect of turbulence by replacing in the Navier-Stokes equations the molecular viscosity with a larger, artificially introduced viscosity—the turbulent or eddy viscosity.

Boussinesq approach (or hypothesis) is the most used closure technique for the apparent stresses arising from the averaging technique introduced by Reynolds in 1895.

Boussinesq hypothesis corresponds to a linear relation between stress and strain tensors, and is analogous to the linear constitutive equation for Newtonian flows.

Molecular viscosity

$$\tau = \nu \left( \frac{\partial U_j}{\partial x_i} + \frac{\partial U_i}{\partial x_j} \right)$$

Viscous stress

Turbulent viscosity – Eddy viscosity

$$\tau_T = \nu_T \left( \frac{\partial U_j}{\partial x_i} + \frac{\partial U_i}{\partial x_j} \right)$$

Turbulent stress – Reynolds stress

## TECHNICAL MEMORANDUM NO. 1231

## REPORT ON INVESTIGATION OF DEVELOPED TURBULENCE\*

By L. Prandtl

The recent experiments by Jakob and Erk (reference 1) on the resistance of flowing water in smooth pipes, which are in good agreement with earlier measurements by Stanton and Pannell (reference 2), have caused me to change my opinion that the empirical Blasius law (resistance proportional to the  $7/4$  power of the mean velocity) was applicable up to arbitrarily high Reynolds numbers. According to the new tests the exponent approaches 2 with increasing Reynolds number, where it remains an open question whether or not a specific finite limiting value of the resistance factor  $\lambda$  is obtained at  $R = \infty$ .

With the collapse of Blasius' law the requirements which produced the relation that the velocity in the proximity of the wall varied in proportion to the 7th root of the wall distance must also become void (reference 3). However, it is found that the fundamental assumption that led to this relationship can be generalized so as to furnish a velocity distribution for any empirical resistance law. These fundamental assumptions can be so expressed that for the law of velocity distribution in proximity of the wall as well as for that of friction at the wall, a form can be found in which the pipe diameter no longer occurs, or in other words, that the processes in proximity of a wall are not dependent upon the distance of the opposite wall.

For the velocity  $u$  (time average value) at  $y$  distance from the wall only one nondimensional can then be formed, namely,  $\frac{uy}{\nu}$  ( $\nu$  = kinematic viscosity), giving for  $u$  a formula of the form

$$u = C\varphi\left(\frac{uy}{\nu}\right) \quad (1)$$

where  $C$  is a velocity and  $\varphi$  an arbitrary function. The shearing stress at the wall then must be

$$\tau = \zeta \rho C^2 \quad (2)$$

where  $\zeta$  is a constant.

\*"Bericht über Untersuchungen zur ausgebildeten Turbulenz."  
Zeitschrift für angewandte Mathematik und Mechanik, vol. 5, no. 2,  
April 1925, pp. 136-139.

It is important to mention that neither Reynolds nor Boussinesq proposed a technique to solve turbulent flows. However, their observations constitute the basis for modern turbulent flows modeling.

It took more than 20 years to propose a model to relate the Reynolds stress tensor to the Boussinesq hypothesis.

The first model allowing this, and hence the first proper turbulence model, was proposed by Prandtl (1925) and is known as the mixing-length model.

This model relates the eddy viscosity to mean velocity gradients and an empirically prescribed length scale of turbulence, the mixing length.

XLV. *On the Propagation of Laminar Motion through a turbulently moving Inviscid Liquid.* By Sir WILLIAM THOMSON, LL.D., F.R.S.\*

1. **I**N endeavouring to investigate turbulent motion of water between two fixed planes, for a promised communication to Section A of the British Association at its coming Meeting in Manchester, I have found something seemingly towards a solution (many times tried for within the last twenty years) of the problem to construct, by giving vortex motion to an incompressible inviscid fluid, a medium which shall transmit waves of laminar motion as the luminiferous æther transmits waves of light.

2. Let the fluid be unbounded on all sides, and let  $u, v, w$  be the velocity-components, and  $p$  the pressure at  $(x, y, z, t)$ . We have

$$\frac{du}{dx} + \frac{dv}{dy} + \frac{dw}{dz} = 0 \quad . \quad . \quad . \quad (1),$$

\* Communicated by the Author, having been read before Section A of the British Association at its recent Meeting in Manchester.

[ 272 ]

XXXIV. *Stability of Motion (continued from the May, June, and August Numbers).*—*Broad River flowing down an Inclined Plane Bed.* By Sir WILLIAM THOMSON, F.R.S.\*

41. **C**ONSIDER now the second of the two cases referred to in § 27—that is to say, the case of water on an inclined plane bottom, under a fixed parallel plane cover (ice, for example), both planes infinite in all directions and gravity everywhere uniform. We shall include, as a sub-case, the icy cover moving with the water in contact with it, which is particularly interesting, because, as it annuls tangential force at the upper surface, it is, for the steady motion, the same case as that of a broad open river flowing uniformly over a perfectly smooth inclined plane bed. It is not the same, except when the motion is steadily laminar, the difference being that the surface is kept rigorously plane, but not free from tangential force, by a rigid cover, while the open surface is kept almost but not quite rigorously plane by gravity, and rigorously free from tangential force. But, provided the bottom is smooth, the smallness of the dimples and little round hollows which we see on the surface, produced by turbulence (when the motion is turbulent), seems to prove that the motion must be very nearly the same as it would be if the upper surface were kept rigorously plane, and free from tangential force.

It is also interesting to mention that neither Boussinesq nor Reynolds seem to have used the word turbulence in their publications.

Boussinesq used the words *tumultuous movements, eddy agitations, movements theory, liquid eddy theory* (in French, *mouvements tumultueux, agitation tourbillonnaire, théorie des remous, théorie des tourbillons liquides, force vive*).

Whereas Reynolds used the words *sinuous paths, sinuous motion, irregular eddies, sinuous disturbance, relative disturbance*.

The word turbulence seems to have been introduced in the field of fluid mechanics for the first time by William Thomson (later Lord Kelvin) in 1887.

The word turbulence was adopted in the field only later, in the beginning of the 20th century, in particular through the works of Prandtl.

# The turbulent world around us

## What is turbulence?

- According to the Merriam-Webster dictionary, turbulence is defined as,

### turbulence noun



tur·bu·lence | \ 'tər-byə-lən(t)s \

#### Definition of *turbulence*

: the quality or state of being turbulent: such as

**a** : great commotion or agitation

// emotional *turbulence*

**b** : irregular atmospheric motion especially when characterized by up-and-down currents

**c** : departure in a fluid from a smooth flow

- Similar definitions follow in different languages.

- Note that this turbulence definition is too general.

- Moving to technical grounds, namely, fluid dynamics, the use of the word **turbulent** to characterize a certain type of flow, namely, the counterpart of a streamline motion, smooth flow, or a laminar flow, is comparatively recent.

# The turbulent world around us

## What is turbulence?

- Not even Osborne Reynolds used the word turbulent in his two principal papers on turbulent flows,
  - O. Reynolds (1883). “An experimental investigation of the circumstances which determine whether the motion of water shall be direct or sinuous, and of the law of resistance in parallel channels.”
  - O. Reynolds (1895). “On the dynamical theory of incompressible viscous fluids and the determination of the criterion.”
- On these two papers, Osborne Reynolds, defined turbulence (or turbulent flows) as eddying or sinuous motion (more on this later).
- Both papers were published in the Philosophical Transactions of the Royal Society, and essentially provided a marker for the direction of research in Engineering Fluid Mechanics for the next century.
- In fluid dynamics we prefer to use the terminology **turbulent flows** instead of **turbulence**.
- However, both terms are valid when dealing at a technical level.
- Hereafter, we will use both terminologies interchangeably.

## What is turbulence?

- Due to the extremely complex nature of turbulence and its incomplete understanding, there is not a single accepted definition of turbulence.
  - Leonardo da Vinci was so intrigued by turbulence that he depicted it in many of his sketches (see previous slides).
  - While observing the flow of water, he gave one of the very first definitions of turbulence (if not the first one), this was more than 500 years ago.

*“...the smallest eddies are almost numberless, and large things are rotated only by large eddies and not by small ones and small things are turned by small eddies and large”*

# The turbulent world around us

## What is turbulence?

- Due to the extremely complex nature of turbulence and its incomplete understanding, there is not a single accepted definition of turbulence.
  - Osborne Reynolds, one of the pioneers in the study of turbulent flows, in 1883, defined turbulent flows as eddying or sinuous motion [1].

*“Again, the internal motion of water assumes one or other of two broadly distinguishable forms – either the elements of the fluid follow one another along lines of motion which lead in the most direct manner to their destination, or they eddy about in sinuous paths, the most indirect possible.”*

*“The small evidence which clear water shows as to the existences of internal eddies, not less than the difficulty of estimating the viscous nature of the fluid, appears to have hitherto obscured the very important circumstance that the more viscous a fluid is, the less prone is it to eddying or sinuous motion.*

## What is turbulence?

- Due to the extremely complex nature of turbulence and its incomplete understanding, there is not a single accepted definition of turbulence.
  - Richardson, in 1922, introduces the idea of an energy cascade in turbulent flows [1],

*“Big whorls have little whorls,  
which feed on their velocity,  
and little whorls have lesser whorls,  
and so on to viscosity”*

## What is turbulence?

- Due to the extremely complex nature of turbulence and its incomplete understanding, there is not a single accepted definition of turbulence.
  - T. von Karman who is known for his studies about Fluid Dynamics, quotes G. I. Taylor with the following definition of turbulence in 1937 [1],

*“Turbulence is an irregular motion which in general makes its appearance in fluids, gaseous or liquid, when they flow past solid surfaces or even when neighboring streams same fluid past or over one another.”*

## What is turbulence?

- Due to the extremely complex nature of turbulence and its incomplete understanding, there is not a single accepted definition of turbulence.
  - J.O. Hinze offers yet another definition for turbulence in 1959 [1],

*“Turbulent fluid motion is an irregular condition of the flow in which quantities show a random variation with time and space coordinates, so that statistically distinct average values can be discerned.”*

## What is turbulence?

- Due to the extremely complex nature of turbulence and its incomplete understanding, there is not a single accepted definition of turbulence.
  - Monin and Yaglom [1], in 1971, gave another definition of laminar and turbulent flows.
  - Notice that at this point, random variations in space and time are becoming a common in all definitions.

*“It is known that all flows of liquids and gases may be divided into two sharply different types; the quiet smooth flows known as “laminar” flows, and their opposite, “turbulent” flows in which the velocity, pressure, temperature and other fluid mechanical quantities fluctuate in a disordered manner with extremely sharp and irregular space- and time-variations.”*

## What is turbulence?

- Due to the extremely complex nature of turbulence and its incomplete understanding, there is not a single accepted definition of turbulence.
  - A more modern (in 1985), and highly specific definition of turbulence is given by G. T. Chapman and M. Tobak [1],

*“Turbulence is any chaotic solution to the 3D Navier–Stokes equations that is sensitive to initial data and which occurs as a result of successive instabilities of laminar flows as a bifurcation parameter is increased through a succession of  $\nu$  values.”*

# The turbulent world around us

## What is turbulence?

- Due to the extremely complex nature of turbulence and its incomplete understanding, there is not a single accepted definition of turbulence.

- A more recent definition is given by Rodi [1] in 2017,

*“Turbulence is a very complex phenomenon as the turbulent motions are highly irregular, fluctuating and always three-dimensional (3D). The turbulent fluctuations cause strong mixing of all flow quantities and hence momentum, heat, and mass transfer that is usually much larger than the transfer resulting from Brownian motion in a laminar flow, which in contrast to turbulence is smooth and regular.”*

- And Schmitt [2], also in 2017,

*Turbulence is found for high Reynolds number flows, and is characterized by erratic motion, intermittency, 3-D vortices and filaments, irreversibility, chaos, unpredictability . Turbulence is ubiquitous in nature and is found, e.g., in the ocean, the atmosphere, geosciences, and also in climate models.*

[1] W. Rodi. Turbulence Modeling and Simulation in Hydraulics: A Historical Review Journal of Hydraulic Engineering. Vol. 143, Issue 5 (May 2017)

[2] F. G. Schmitt. Turbulence from 1870 to 1920: The birth of a noun and of a concept. Comptes Rendus Mécanique Volume 345, Issue 9, September 2017, Pages 620-626

## What is turbulence?

- Due to the extremely complex nature of turbulence and its incomplete understanding, there is not a single accepted definition of turbulence.
  - S. Rodriguez, in 2019, gives an even more modern definition linked to the use of numerical approximations (and therefore computers), to deliver approximated solutions [1],

*“Turbulent flows is the dynamic superposition of an extremely large number of eddies with random (irregular) but continuous spectrum of sizes and velocities that are interspersed with small, discrete pockets of laminar flow (as a result of the Kolmogorov eddies that decayed, as well as in the viscous laminar sublayer and in the intermittent boundary). In this sense, turbulent flows are intractable in its fullest manifestation; this is where good, engineering common sense and approximations can deliver reasonable solutions, albeit approximate.”*

## What is turbulence?

- Due to its complexity, a definition does not work properly for turbulence, instead of it, it's better to explain its characteristics.
- Tennekes and Lumley [1] in their book called "*A First Course in Turbulence*", list the characteristics of turbulence:
  - Irregularity.
  - Diffusivity.
  - Large Reynolds numbers.
  - Three-Dimensional vorticity fluctuations.
  - Dissipation.
  - Continuum.
  - Feature of a flow, not fluid.
- These characteristics represent the fingerprint of turbulent motion

# The turbulent world around us

## Turbulent flows have the following characteristics

- **Irregularity.** One characteristic of turbulent flows is their irregularity (or randomness). A fully deterministic approach to characterize turbulent flows is very difficult, if not impossible. Turbulent flows are usually described statistically.



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# The turbulent world around us

## Turbulent flows have the following characteristics

- **Diffusivity.** The diffusivity of turbulence causes rapid mixing and increased rates of momentum, heat, and mass transfer. A flow that looks random but does not exhibit the spreading of velocity fluctuations through the surrounding fluid is not turbulent.



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# The turbulent world around us

## Turbulent flows have the following characteristics

- **Large Reynolds number.** Turbulent flows always occur at high Reynolds numbers. They are caused by a complex interaction between the viscous terms and nonlinear terms in the equations of motion. Randomness and nonlinearity combine to make the equations of turbulence nearly intractable.



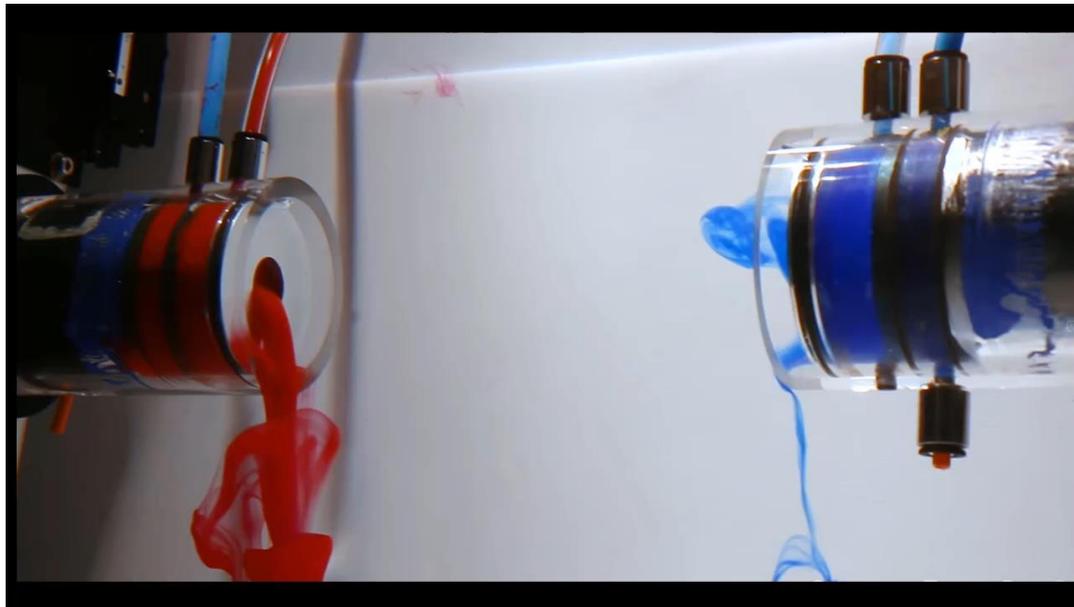
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# The turbulent world around us

## Turbulent flows have the following characteristics

- **Three-Dimensional vorticity fluctuations.** Turbulence is rotational and three dimensional. Turbulence always exhibit high levels of fluctuating vorticity. The random vorticity fluctuations that characterize turbulence could not maintain themselves if the velocity fluctuations were two dimensional. Mechanisms such as the stretching of three-dimensional vortices play a key role in turbulence.



Video credit: <https://www.youtube.com/watch?v=EVbdbVhzcM4&t>. This video has been edited to fit this presentation. Copyright on the images is held by the contributors. Apart from Fair Use, permission must be sought for any other purpose.

# The turbulent world around us

## Turbulent flows have the following characteristics

- **Dissipation.** Turbulent flows are dissipative. Kinetic energy gets converted into heat due to viscous shear stresses. Turbulent flows die out quickly when no energy is supplied.



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# The turbulent world around us

## Turbulent flows have the following characteristics

- **Continuum.** Turbulence is a continuum phenomenon. Even the smallest eddies are significantly larger than the molecular scales.



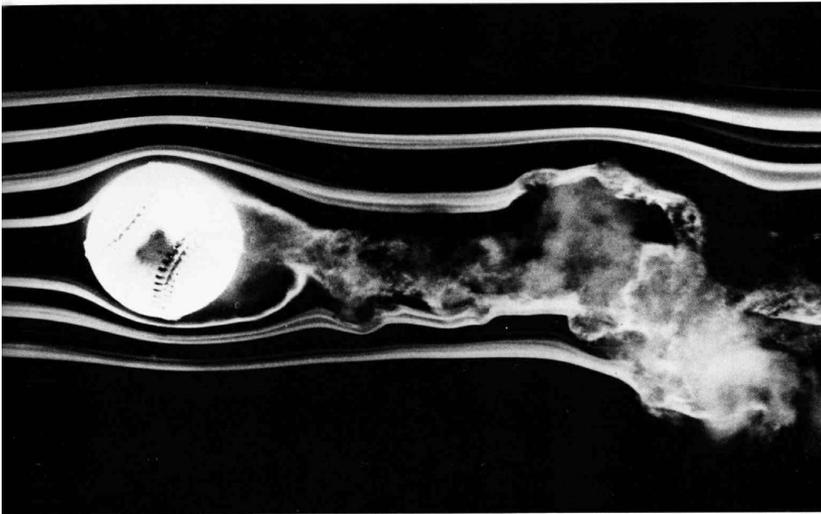
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# The turbulent world around us

## Turbulent flows have the following characteristics

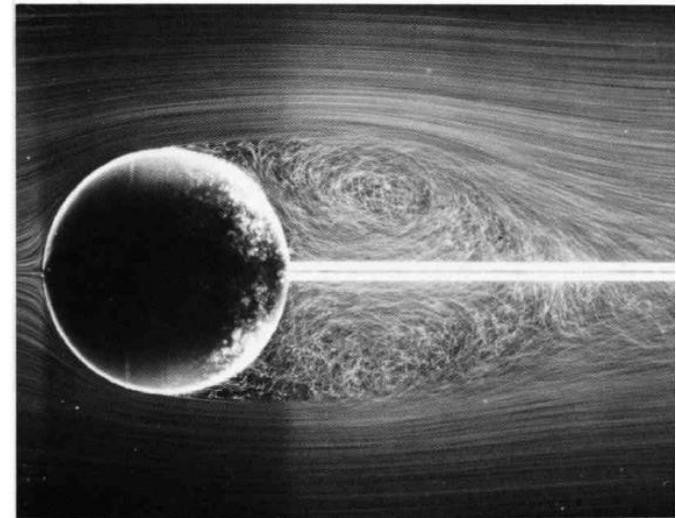
- **Feature of a flow, not fluid.** Turbulence is a feature of fluid flow and is not a property of the flow. A liquid or a gas at high Reynolds number will exhibit the same dynamics.



**Air flow over a spinning baseball.**

M. Van Dyke. An album of fluid motion.

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**Water flow over a sphere.**

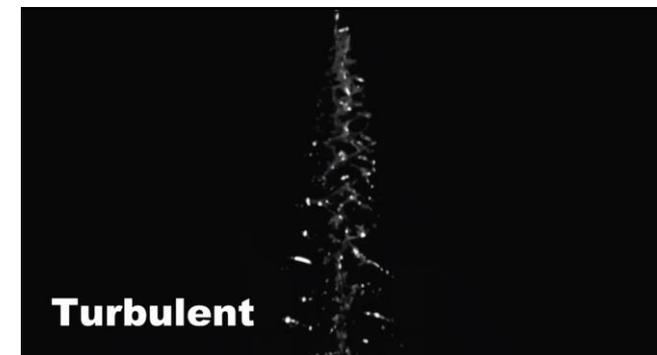
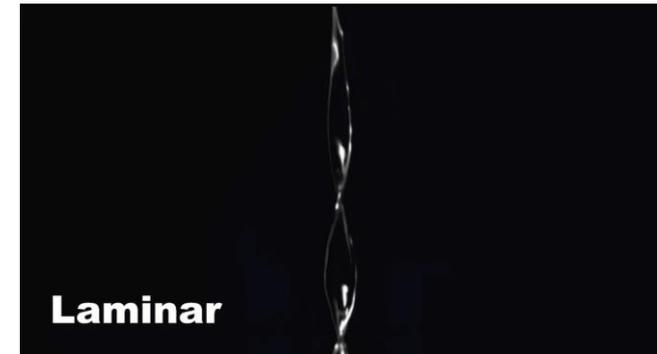
M. Van Dyke. An album of fluid motion.

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# The turbulent world around us

## Turbulent flows have the following characteristics

- In summary:
  - One characteristic of turbulent flows is their **irregularity** (or randomness). A fully deterministic approach to characterize turbulent flows is very difficult. Turbulent flows are usually described statistically. Turbulent flows are always chaotic. But not all chaotic flows are turbulent. Magma flowing can be chaotic but not necessarily turbulent.
  - The **diffusivity** of turbulence causes rapid mixing and increased rates of momentum, heat, and mass transfer. A flow that looks random but does not exhibit the spreading of velocity fluctuations through the surrounding fluid is not turbulent.
  - Turbulent flows are **dissipative**. Kinetic energy gets converted into heat due to viscous shear stresses. Turbulent flows die out quickly when no energy is supplied.
  - Turbulent flows always occur at **high Reynolds numbers**. They are caused by a complex interaction between the viscous forces and convection.
  - Turbulent flows are **rotational**, that is, they have non-zero vorticity. Mechanisms such as the stretching of three-dimensional vortices play a key role in turbulence.
  - Turbulence is a **continuum** phenomenon. Even the smallest eddies are significantly larger than the molecular scales.
  - Turbulence is a **feature of fluid flow** and is not a property of the flow. A liquid or a gas at high Reynolds number will exhibit the same dynamics.

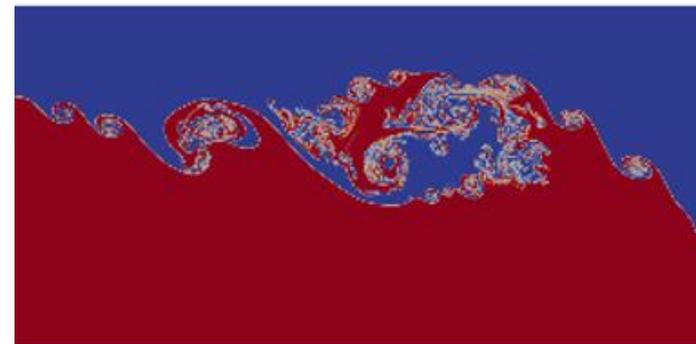
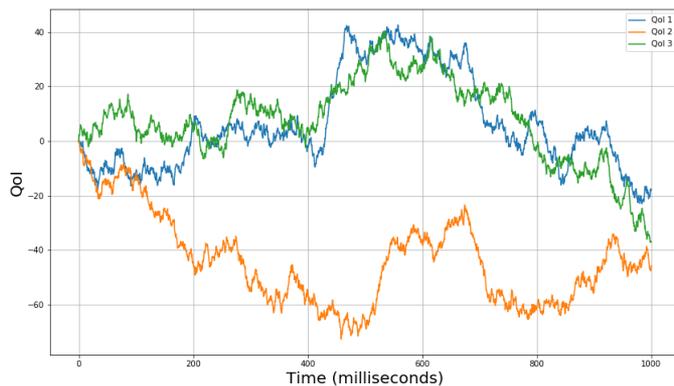


Video credit: <https://www.youtube.com/watch?v=9dz7fUJBF0k>  
This video has been edited to fit this presentation.  
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# The turbulent world around us

## ... in the end, what is turbulence?

- Turbulent flows share all the previous characteristics. In addition, we can state the following,
  - Turbulence is an unsteady, aperiodic motion in which all three velocity components fluctuate in space and time.
  - Every transported quantity shows similar fluctuations (pressure, temperature, species, concentration, and so on)
  - Turbulent flows contains a wide range of eddy sizes (scales):
    - Large eddies derives their energy from the mean flow. The size and velocity of large eddies are on the order of the mean flow.
    - Large eddies are unstable and they break-up into smaller eddies.
    - The smallest eddies convert kinetic energy into thermal energy via viscous dissipation.
    - The behavior of small eddies is more universal in nature.



# The turbulent world around us

## Turbulence and computers

- In 1949 von Neumann predicted that the advent of digital computers would revolutionize the study of turbulence since it would become possible to simulate the Navier-Stokes equations in 3D in turbulent regimes.
- Von Neumann, convinced of the important role of computers for the study of turbulence made the following observations [1],

*“... a considerable mathematical effort towards a detailed understanding of the mechanism of turbulence is called for ...”*

- But that, given the analytic difficulties presented by the turbulence problem,

*“... there might be some hope to ‘break the deadlock’ by extensive, but well-planned, computational efforts.”*

- It took over 20 years until von Neumann’s vision came to reality with the first genuine 3D simulations of turbulence conducted by Orszag and Patterson [2].

[1] J. von Neumann. 1963. Recent Theories of Turbulence. In Collected Works (1949–1963), Vol. 6, p. 437. Edited by A. H. Taub. Oxford, UK: Pergamon Press.

[2] S. A. Orszag and G. S. Patterson, Jr. Numerical Simulation of Three-Dimensional Homogeneous Isotropic Turbulence. Phys. Rev. Lett. 28, 76 – Published 10 January 1972.

# The turbulent world around us

## Turbulence and computers

- Numerical simulations and the ability to analyze large ensemble of experimental data using computers have revolutionized our understanding of turbulent flows [1].

*“From a fundamental perspective, the direct numerical simulation of idealized isotropic, homogeneous turbulence has been revolutionary in its impact on turbulence research because of the ability to simulate and display the full 3-D velocity field at increasingly large Reynolds number.”*

*“Similarly, experimentation on turbulence has advanced tremendously by using computer data acquisition; 20 years ago it was possible to measure and analyze time series data from single-point probes that totaled no more than 10 megabytes of information, whereas today statistical ensembles of thousands of spatially and temporally resolved velocity fields, taking 10 terabytes of storage space can be obtained and processed.”*

## Turbulence and computers

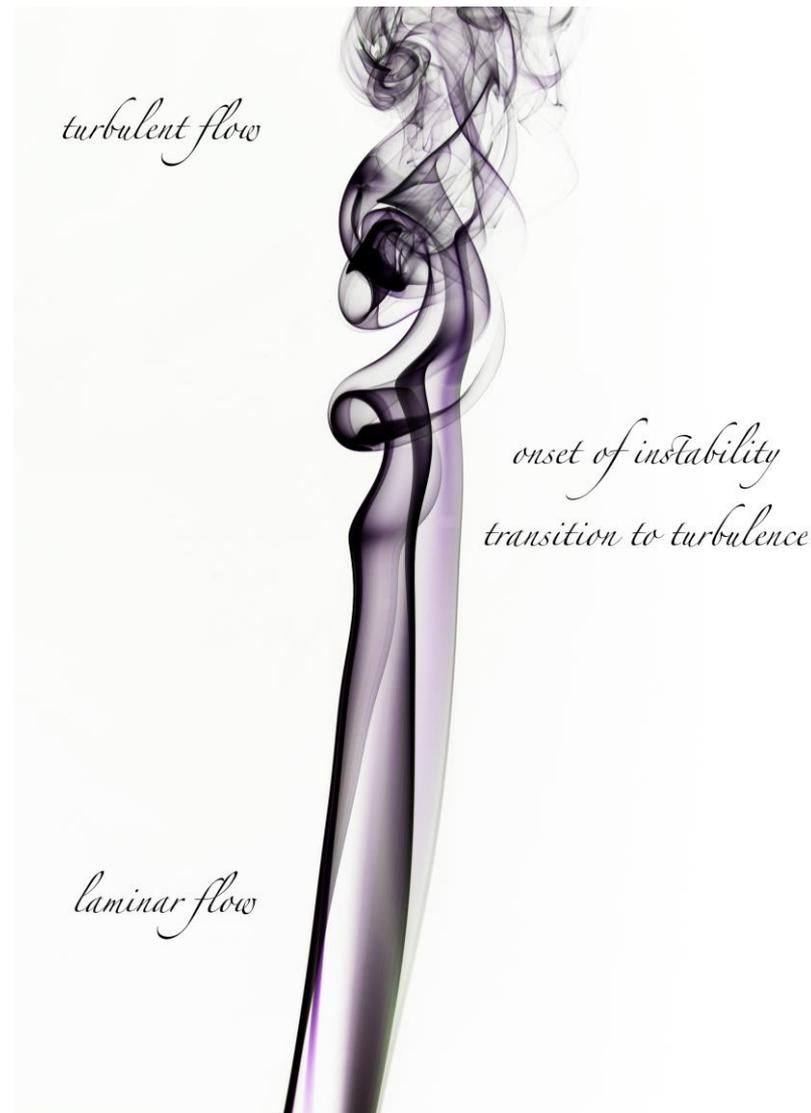
- The numerical and experimental possibilities in turbulence research can only be enhanced even further by expected future increases in computational power.
- From an academic and research point of view, computers are used to improve the theoretical understanding of turbulent flows, developed new models, validate existent models, and analyze numerical and experimental data.
- From the industrial point of view, computers (and CFD models) have made accessible complex physics and large-scale simulations in relatively affordable times.
- Computers are an invaluable tool in the turbulence research field.
- But, before conducting numerical simulations, we must understand the basis and apply this knowledge to reduce the uncertainties associated with turbulence models.
- And this is the goal of this course.
  - Guide you, engineers, in computing turbulent flows.

# The turbulent world around us

Before continuing, let me share a few more amazing images that show the beauty and complexity of turbulence in nature and engineering applications.



# The turbulent world around us

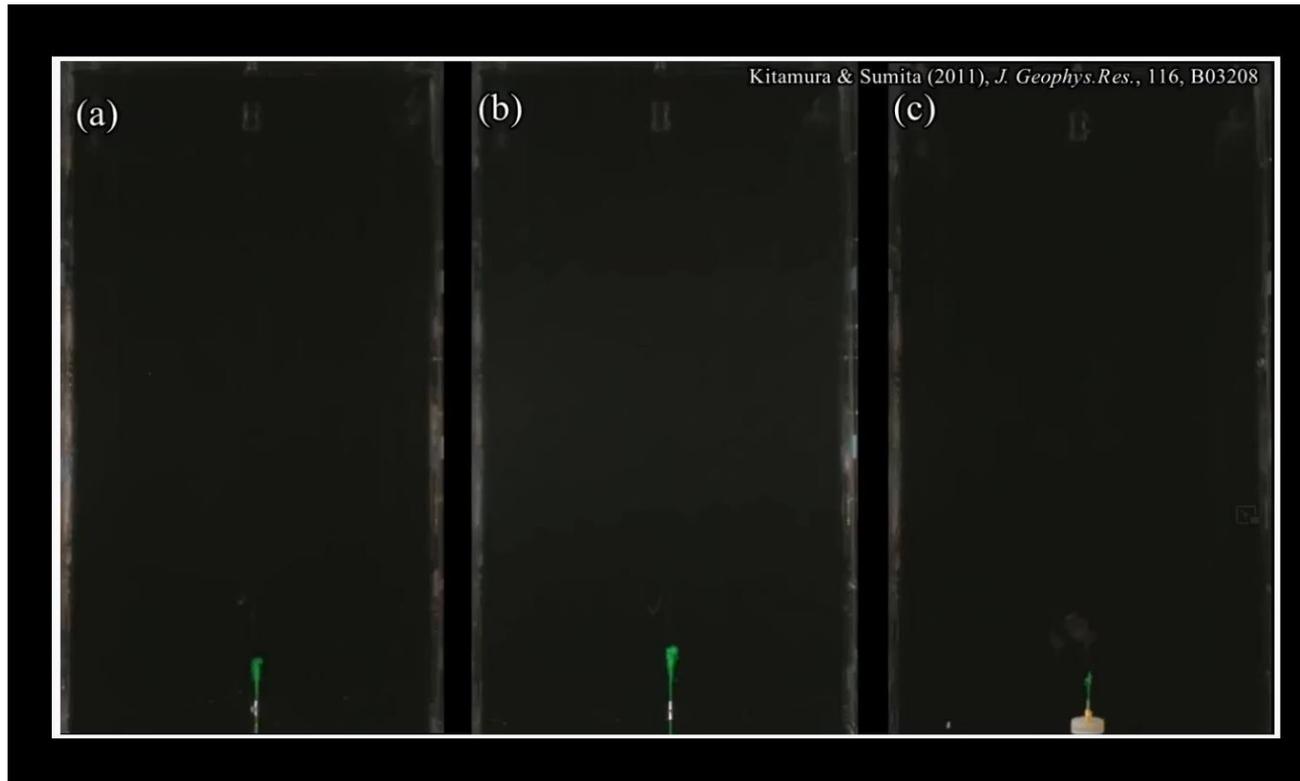


**Buoyant plume of smoke rising from a stick of incense**

Photo credit: <https://www.flickr.com/photos/jlhopgood/>

This work is licensed under a Creative Commons License (CC BY-NC-ND 2.0)

# The turbulent world around us



Movies are played at real time. Images are upside down (experiments are conducted by injecting negatively or neutrally buoyant fluid from the top). Size of the images are 0.35 m x 0.20 m.

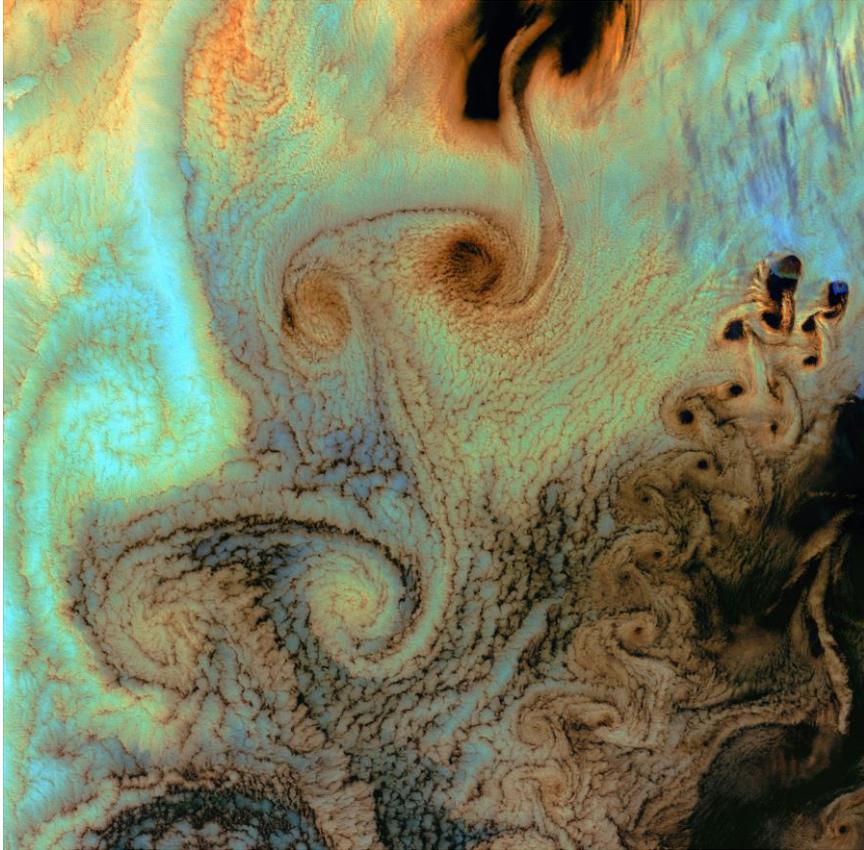
- (a) Reynolds number  $Re = 1157$  and density difference  $\Delta \rho = 8.00 \times 10^2 \text{ kg/m}^3$  (large inertia and buoyancy). Plumes keeps on rising after the inertia is lost.
- (b)  $Re = 1380$ ,  $\Delta \rho = 0 \text{ kg/m}^3$  (large inertia but no buoyancy). Plume decelerates as inertia is lost.
- (c)  $Re = 300$ ,  $\Delta \rho = 0 \text{ kg/m}^3$  (small inertia but no buoyancy).

## Turbulent plume shapes : effects of buoyancy and inertia

Movie credit: [https://www.youtube.com/watch?v=l\\_Yimq6gWfU](https://www.youtube.com/watch?v=l_Yimq6gWfU)

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# The turbulent world around us



**Von Karman vortices created when prevailing winds sweeping east across the northern Pacific Ocean encountered Alaska's Aleutian Islands**

Photo credit: USGS EROS Data Center Satellite Systems Branch.  
Copyright on the images is held by the contributors. Apart from Fair Use, permission must be sought for any other purpose.



**Von Karman Vortex Streets in the northern Pacific Photographed from the International Space Station**

Photo credit: NASA

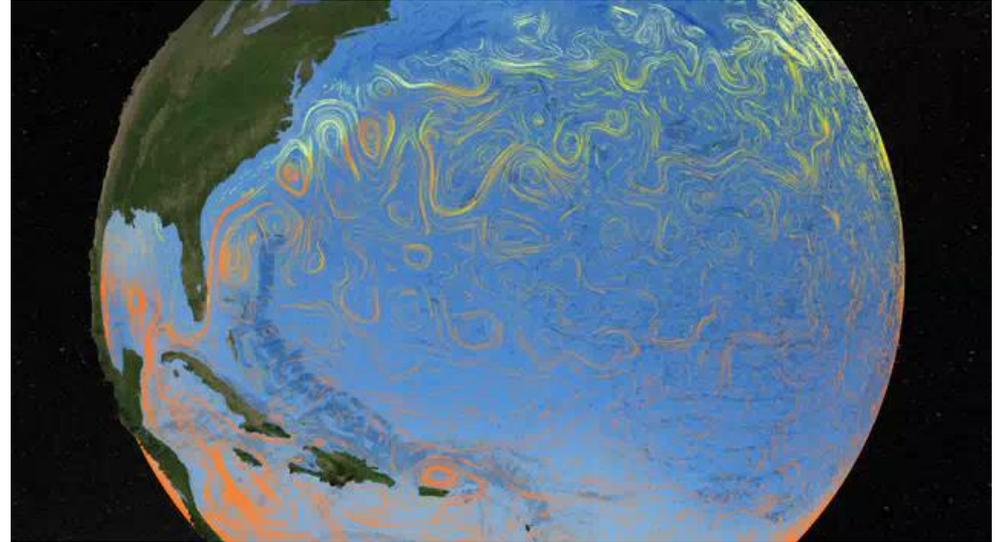
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# The turbulent world around us



## **Cirrus clouds - Kelvin-Helmholtz instability**

Photo credit: <https://www.pinterest.it/pin/8514686771867411/>  
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## **NASA Aquarius mission - Studies of ocean and wind flows**

The Aquarius mission measured the salinity in the ocean, giving scientists the tools needed to improve predictions of future climate trends and events. Aquarius salinity data, combined with data from other sensors that measure sea level, rainfall, temperature, ocean color, and winds, gave us a much clearer picture of how the ocean works. Will higher temperatures intensify evaporation and alter sea surface salinity patterns? Will changes in salinity affect ocean circulation and how heat is distributed over the globe? Aquarius measurements provide a new perspective on the ocean, how it is linked to climate, and how it will respond to climate change

Video credit: <https://svs.gsfc.nasa.gov/cgi-bin/details.cgi?aid=3829>  
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# The turbulent world around us



## **Turbulent waters**

Photo credit: <https://www.flickr.com/photos/thepaegan>

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## **Confluence of the Rio Negro and the Rio Solimoes near Manaus, Brazil**

Photo credit:

[https://en.wikipedia.org/wiki/File:Meeting\\_of\\_waters\\_from\\_the\\_air\\_manaus\\_brazil.JPG](https://en.wikipedia.org/wiki/File:Meeting_of_waters_from_the_air_manaus_brazil.JPG)

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# The turbulent world around us



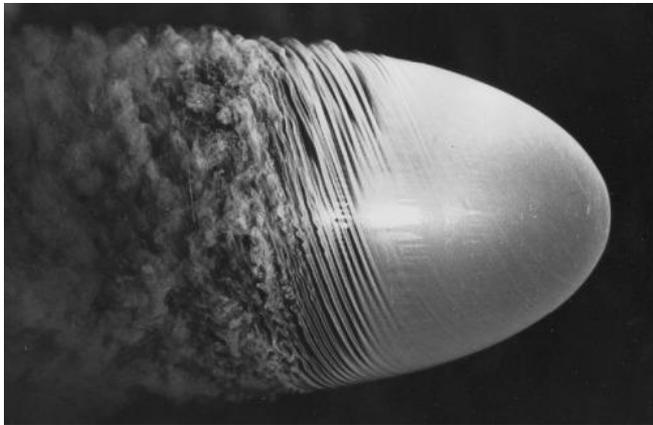
**Tugboat riding on the turbulent wake of a ship**

Photo credit: <https://www.flickr.com/photos/oneeighteen/>  
This work is licensed under a Creative Commons License (CC BY-NC 2.0)



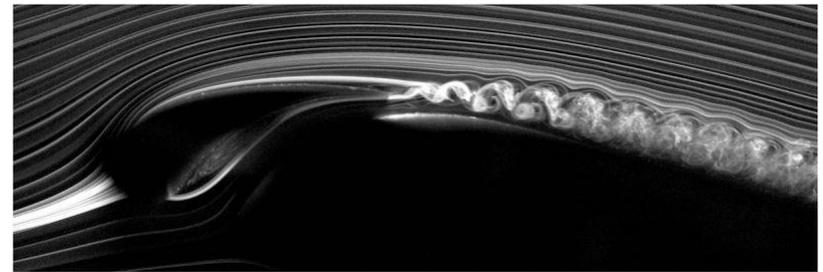
**Trailing vortices**

Photo credit: Steve Morris. AirTeamImages.  
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**Flow visualization over a spinning spheroid**

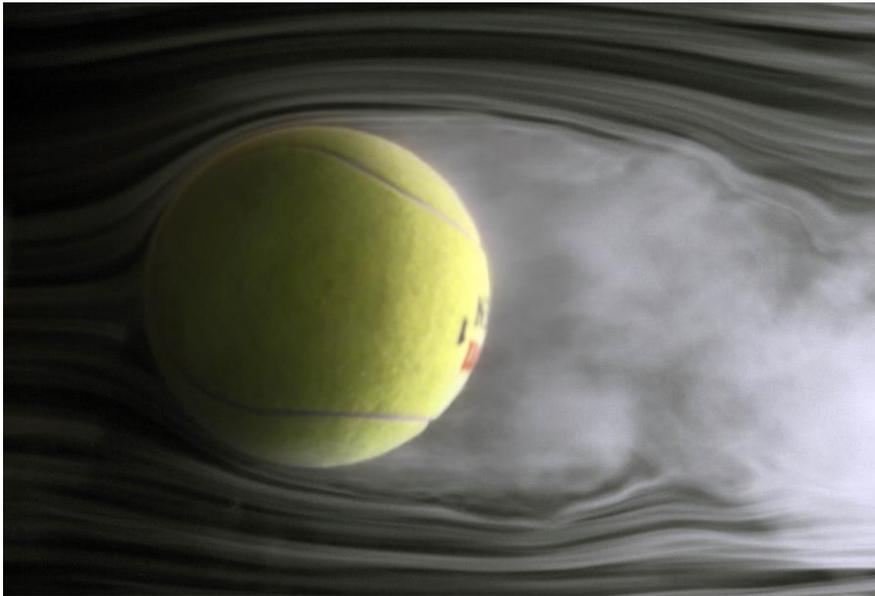
Photo credit: Y. Kohama.  
Copyright on the images is held by the contributors. Apart from Fair Use, permission must be sought for any other purpose.



**Flow around an airfoil with a leading-edge slat**

Photo credit: S. Makiya et al.  
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# The turbulent world around us



## Wind Tunnel Test of New Tennis Ball

Photo credit: NASA

<http://tennisclub.gsfc.nasa.gov/tennis.windtunnelballs.html>

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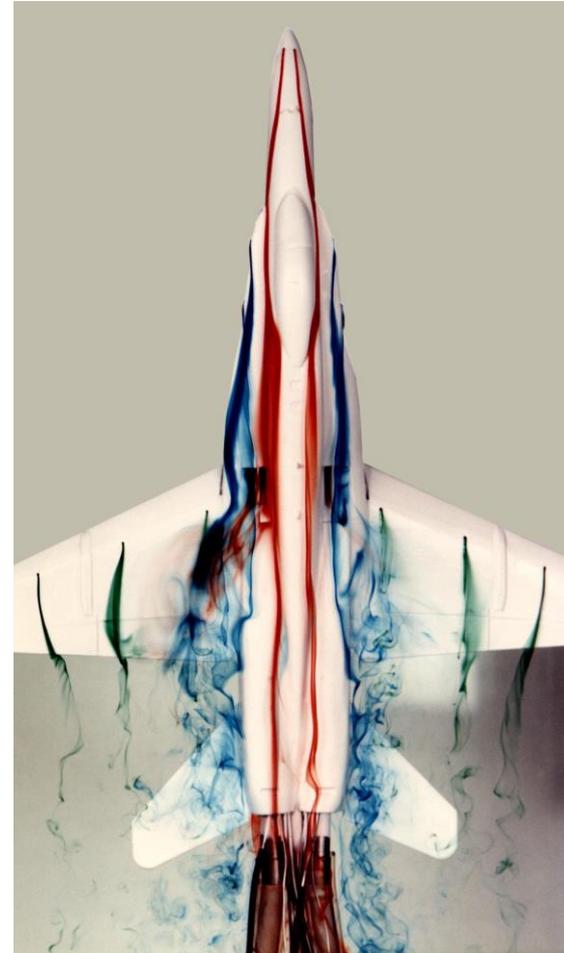
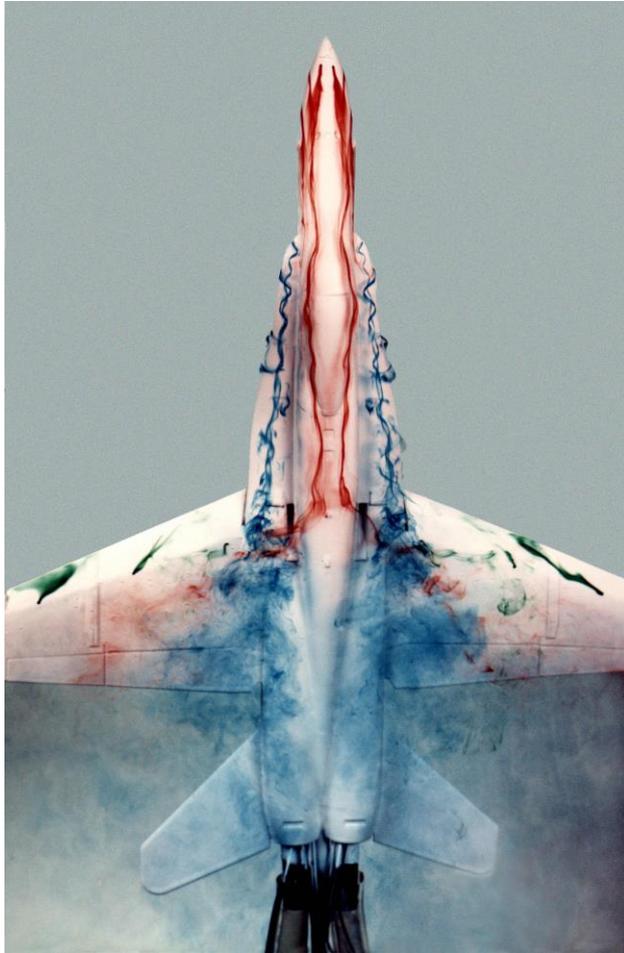


## Wake turbulence behind individual wind turbines

Photo credit: NREL's wind energy research group.

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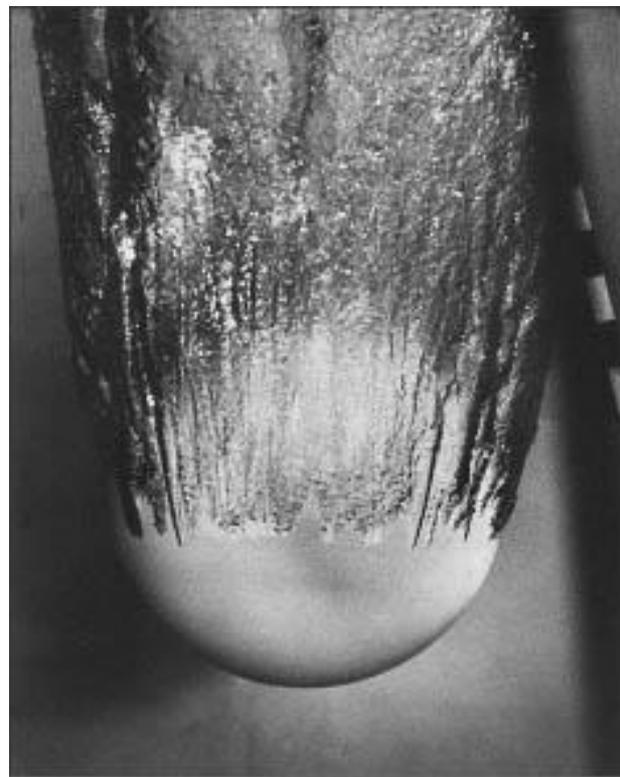
# The turbulent world around us



**Vortices on a 1/48-scale model of an F/A-18 aircraft inside a Water Tunnel**

Photo credit: NASA Dryden Flow Visualization Facility. <http://www.nasa.gov/centers/armstrong/multimedia/imagegallery/FVF>  
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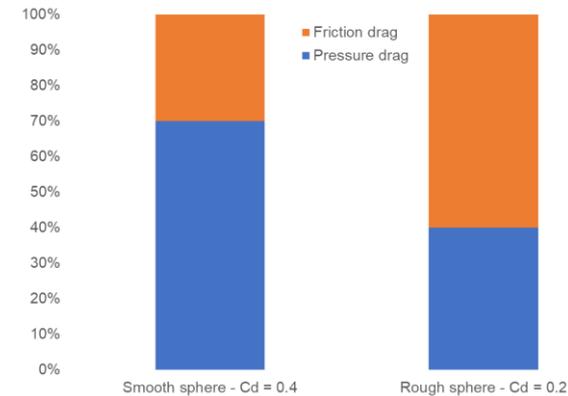
# The turbulent world around us



(a)  $C_D \approx 0.4$



(b)  $C_D \approx 0.2$



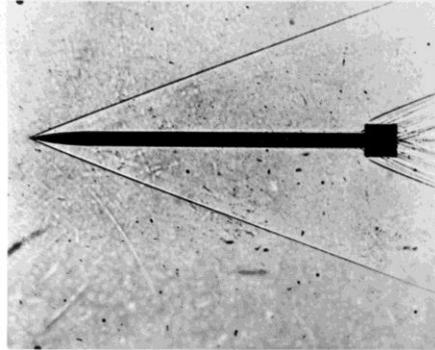
**Abstract representation of the drag decomposition**

- Turbulent flows are not always detrimental to the overall performance of a system.
- In the left image the boundary layer is laminar and in the right image the boundary layer is turbulent.
- Note that in the case with the turbulent boundary layer, the drag coefficient is lower.

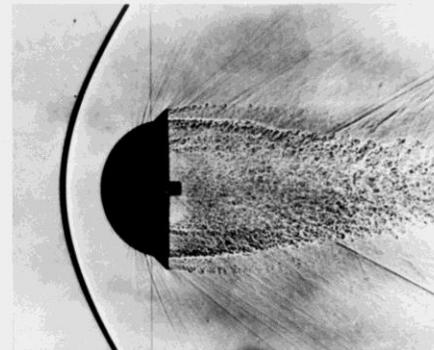
**Flow around two spheres. Left image: smooth sphere. Right image: sphere with rough surface at the nose**  
Photo credit: <http://www.mhhe.com/engcs/civil/finnmore/graphics/photos/AuthorRecommendedImages/index.html>  
Copyright on the images is held by the contributors. Apart from Fair Use, permission must be sought for any other purpose

# The turbulent world around us

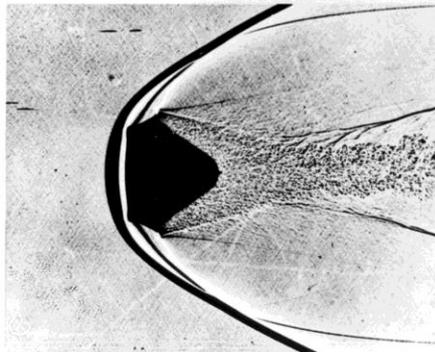
## RESEARCH CONTRIBUTING TO PROJECT MERCURY



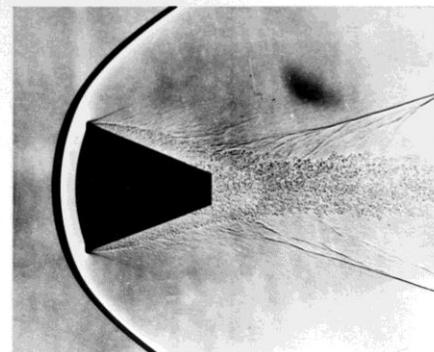
INITIAL CONCEPT



BLUNT BODY CONCEPT 1953



MISSILE NOSE CONES 1953-1957



MANNED CAPSULE CONCEPT 1957

### Shadowgraph Images of Re-entry Vehicles

Photo credit: NASA on the Commons. <https://www.flickr.com/photos/nasacommons/>

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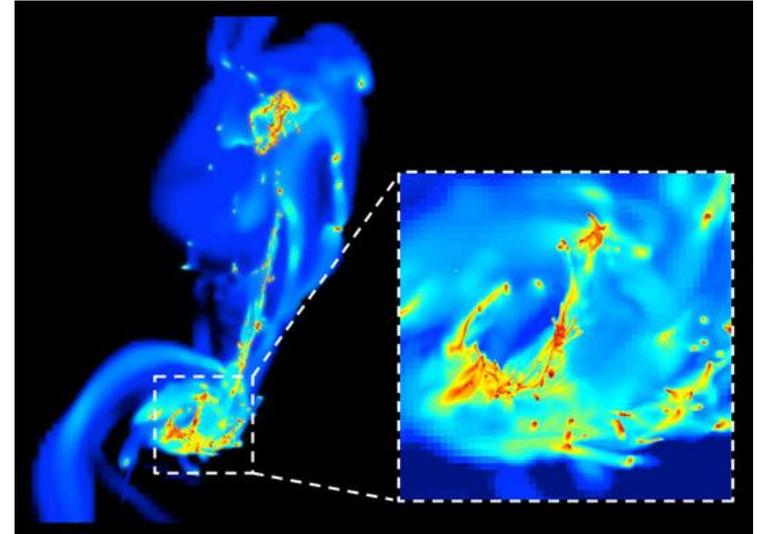
# The turbulent world around us

## Astrophysical, plasma, planetary and quantum turbulence



**M8: The Lagoon Nebula**

Photo credit: Steve Mazlin, Jack Harvey, Rick Gilbert, and Daniel Verschate.  
Star Shadows Remote Observatory, PROMPT, CTIO  
Copyright on the images is held by the contributors. Apart from Fair Use,  
permission must be sought for any other purpose



**A frame from the simulation of the two colliding Antennae galaxies.**

Photo credit: F. Renaud / CEA-Sap.  
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permission must be sought for any other purpose



**Jupiter photo taken by Juno's cam.**

Photo credit: NASA / JPL / SwRI / MSSS / David Marriott  
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# Roadmap to Lecture 2

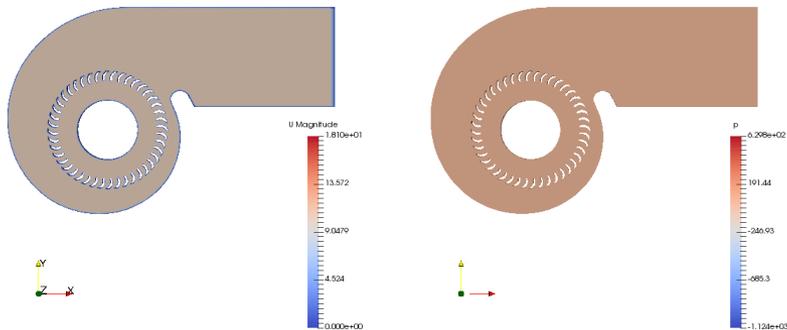
- ~~1. The turbulent world around us~~
- 2. Turbulence, does it matter?**
3. Introduction to turbulence modeling – Basic concepts
4. Wall bounded flows and shear flows
5. A peek to the turbulence closure problem, some correlations in turbulence modeling, and the energy cascade

# Turbulence, does it matter?

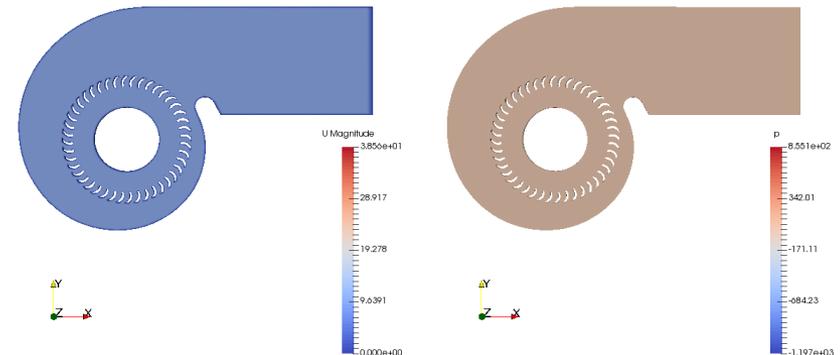
## Blower simulation using sliding grids



Time: 0.000000



Time: 0.000000



**No turbulence model used (laminar, no turbulence modeling, DNS, unresolved DNS, exact Navier-Stokes, physics resolving simulation, name it as you want)**

<http://www.wolfdynamics.com/training/turbulence/image1.gif>

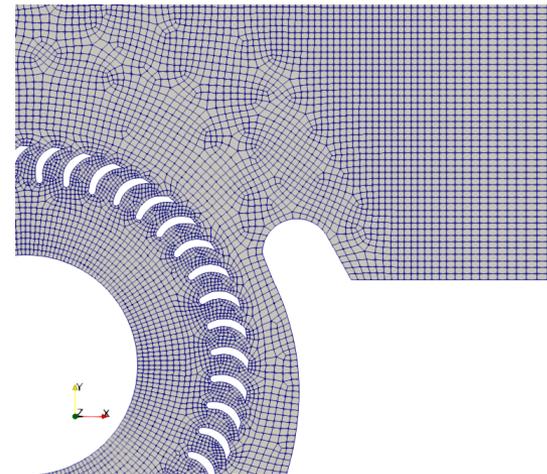
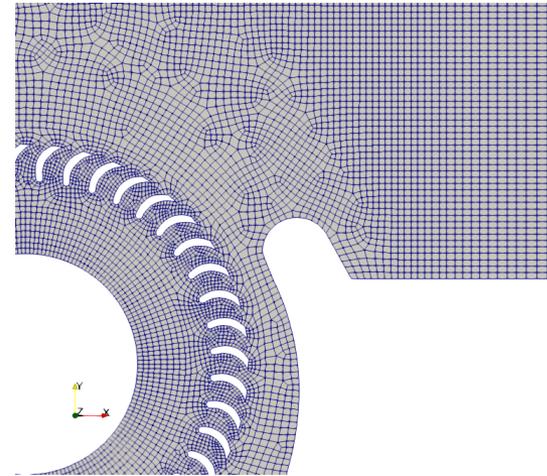
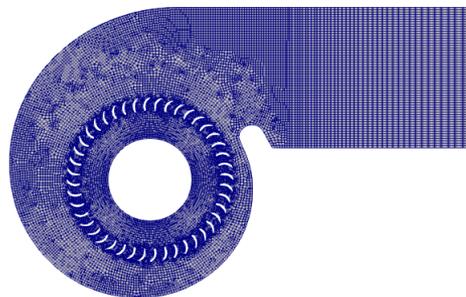
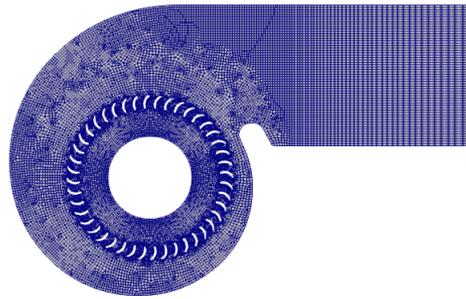
**K-epsilon turbulence model**

<http://www.wolfdynamics.com/training/turbulence/image2.gif>

# Turbulence, does it matter?

## Blower simulation using sliding grids

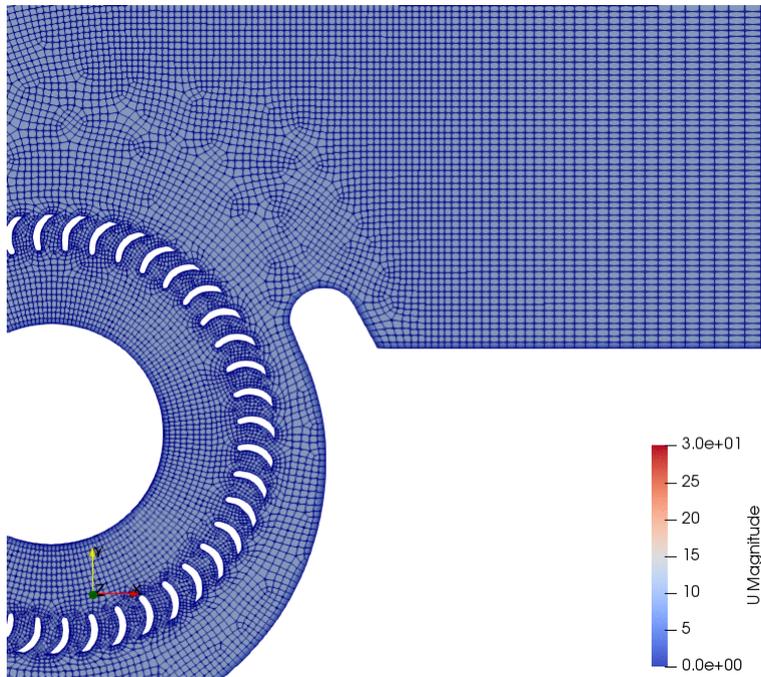
- Even if the mesh is coarse, thanks to the help of the turbulence model, we managed to capture the right physics.



# Turbulence, does it matter?

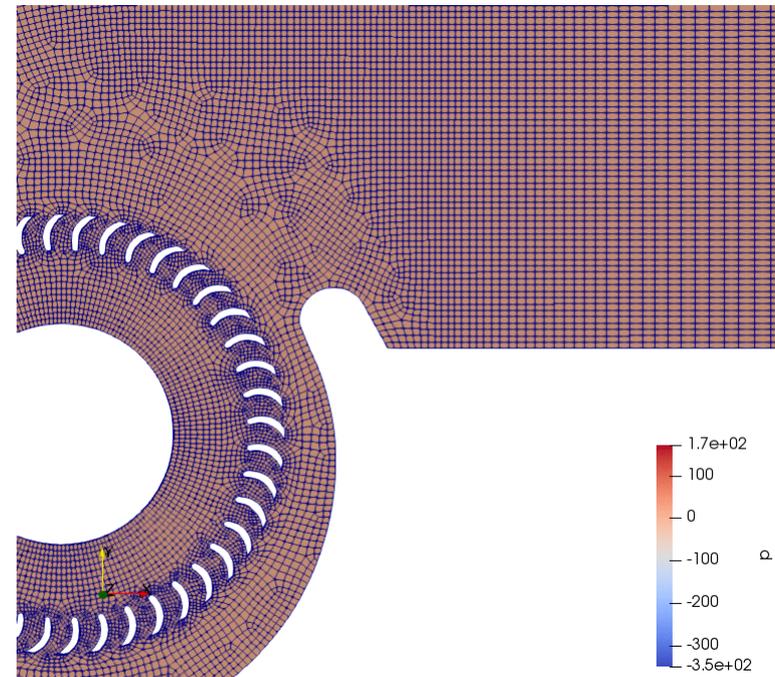
## Blower simulation using sliding grids

- Even if the mesh is coarse, thanks to the help of the turbulence model, we managed to capture the right physics.



**K-epsilon turbulence model – Velocity magnitude field (m/s)**

<http://www.wolfdynamics.com/training/turbulence/blower3.gif>

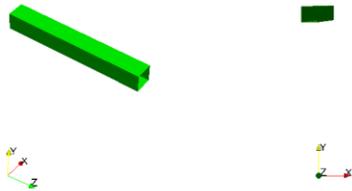


**K-epsilon turbulence model – Relative pressure field (Pa)**

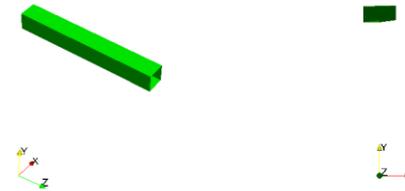
<http://www.wolfdynamics.com/training/turbulence/blower4.gif>

# Turbulence, does it matter?

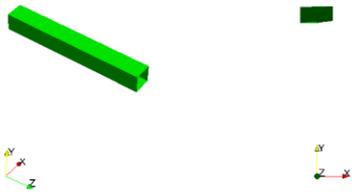
## Vortex shedding past square cylinder



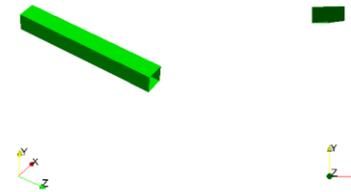
**URANS (K-Omega SST with no wall functions) – Vortices visualized by Q-criterion**  
[www.wolfdynamics.com/wiki/squarecil/urans2.gif](http://www.wolfdynamics.com/wiki/squarecil/urans2.gif)



**LES (Smagorinsky) – Vortices visualized by Q-criterion**  
[www.wolfdynamics.com/wiki/squarecil/les.gif](http://www.wolfdynamics.com/wiki/squarecil/les.gif)



**Laminar (no turbulence model) – Vortices visualized by Q-criterion**  
[www.wolfdynamics.com/wiki/squarecil/laminar.gif](http://www.wolfdynamics.com/wiki/squarecil/laminar.gif)



**DES (SpalartAllmarasDDES) – Vortices visualized by Q-criterion**  
[www.wolfdynamics.com/wiki/squarecil/des.gif](http://www.wolfdynamics.com/wiki/squarecil/des.gif)

# Turbulence, does it matter?

## Vortex shedding past square cylinder

Turbulence model	Drag coefficient	Strouhal number	Computing time (s)
Laminar	2.81	0.179	93489
LES	2.32	0.124	77465
DES	2.08	0.124	70754
SAS	2.40	0.164	57690
URANS (WF)	2.31	0.130	67830
URANS (No WF)	2.28	0.135	64492
RANS	2.20	-	28246 (10000 iter)
Experimental values	2.05-2.25	0.132	-

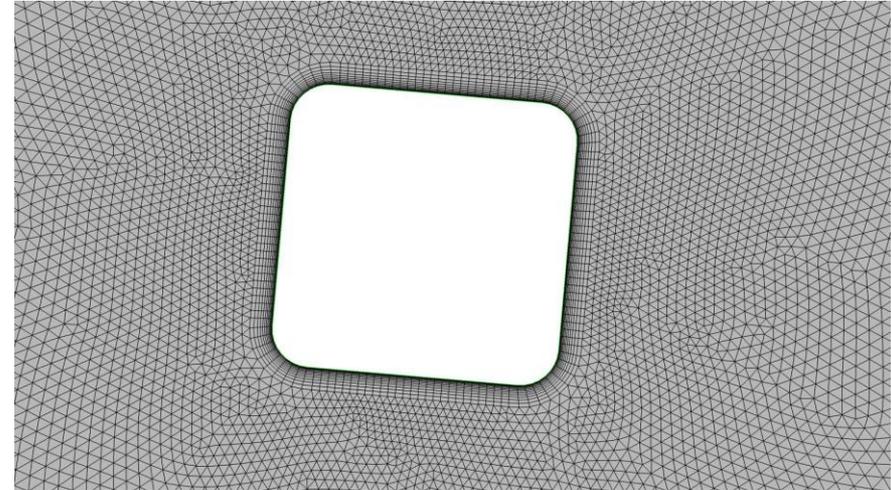
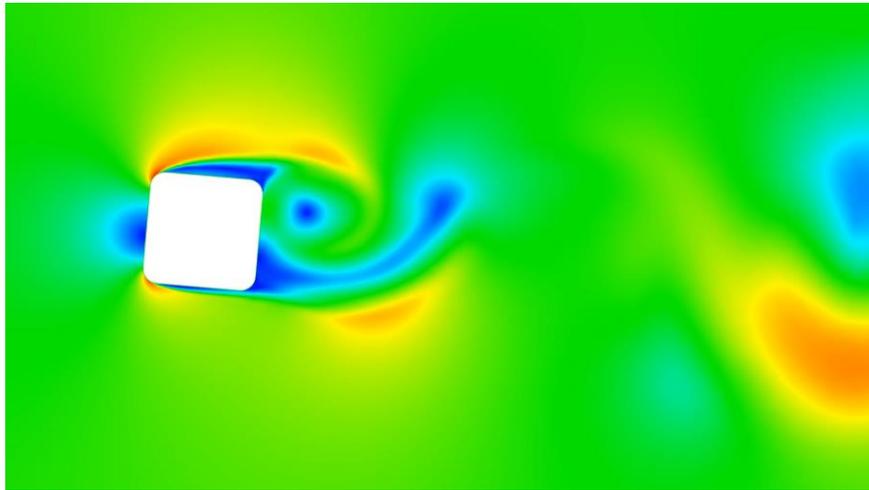
**Note:** all simulations were run using 4 cores.

### References:

- D. A. Lyn and W. Rodi. "The flapping shear layer formed by flow separation from the forward corner of a square cylinder". *J. Fluid Mech.*, 267, 353, 1994.  
D. A. Lyn, S. Einav, W. Rodi and J. H. Park. "A laser-Doppler velocimetry study of ensemble-averaged characteristics of the turbulent near wake of a square cylinder". *Report. SFB 210/E/100.*

# Turbulence, does it matter?

## Transitional flow past square cylinder with rounded corners – $Re = 54000$



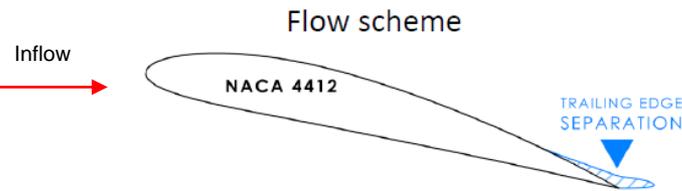
Velocity magnitude

[www.wolfdynamics.com/wiki/turb/media1.mp4](http://www.wolfdynamics.com/wiki/turb/media1.mp4)

Turbulence model	Drag coefficient	Lift coefficient
DNS	0.06295	0.07524
LES	0.1146	0.03269
SAS	0.1058	0.0258
URANS (No WF)	0.1107	0.00725
Transition K-KL-Omega	0.059	-0.0104
Transition K-Omega SST	0.0987	-0.0143
Experimental values	0.045 to 0.075	-0.011 to -0.015

# Turbulence, does it matter?

## Separated flow around a NACA-4412 airfoil



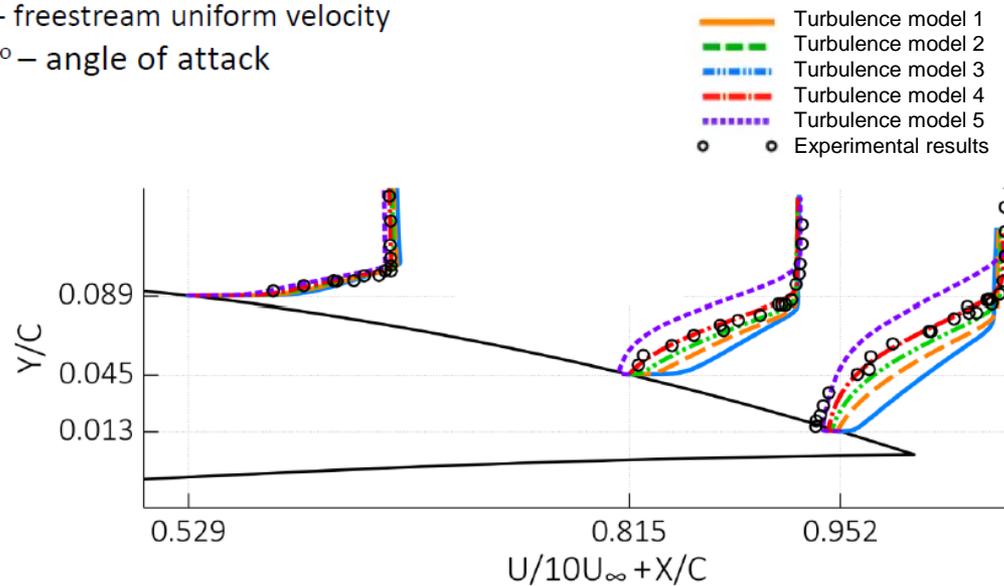
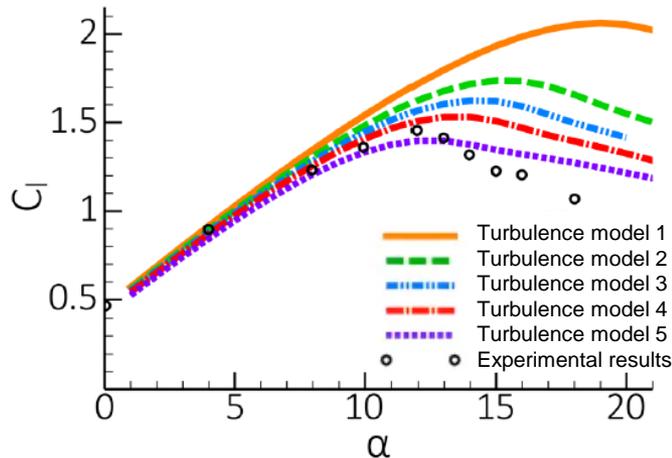
Incompressible flow

$$Re = U_{\infty} \cdot C / \nu = 1.64 \cdot 10^6$$

C - airfoil chord

$U_{\infty}$  - freestream uniform velocity

$\alpha = 12^{\circ}$  - angle of attack



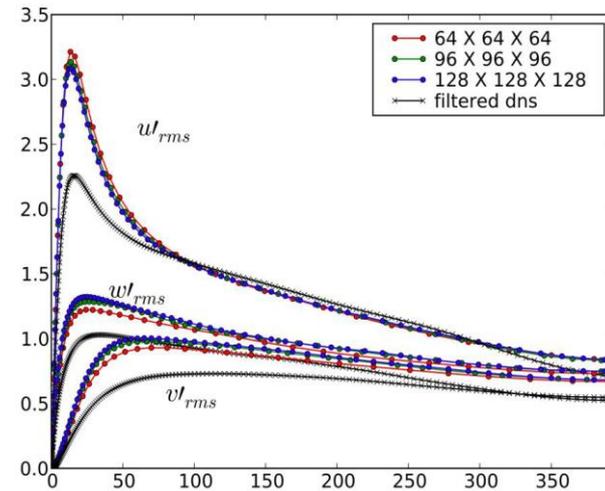
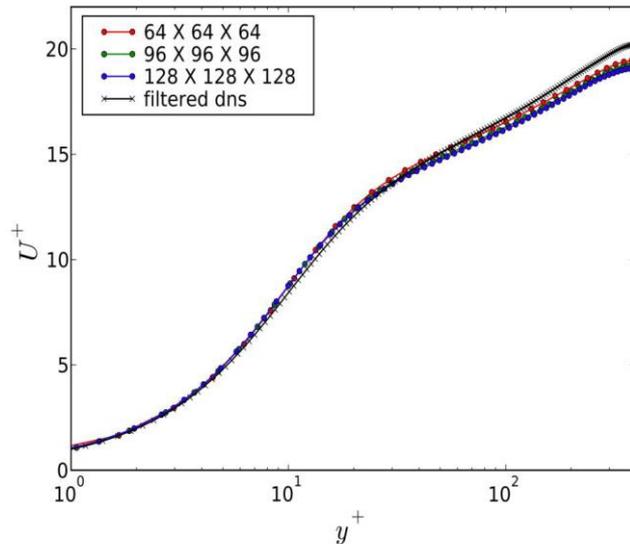
- CFD has been around since the late 1970s, and after all these years is not that easy to compute the flow around 2D airfoils.
- In particular, predicting the maximum lift and stall characteristics is not trivial.

### References:

- F. Menter. "A New Generalized k-omega model. Putting flexibility into Turbulence models (GEKO)", Ansys Germany
- A. J. Wadcock. "Investigation of Low-Speed Turbulent Separated Flow Around Airfoils", NASA Contractor Report 177450

# Turbulence, does it matter?

## Grid independent solutions and modeling errors



- CFD has been around since the late 1970s. Since then, a lot of progress has been done in hardware, software, algorithms and turbulence models.
- But many times, even if we get converged, grid-independent solutions we fail to get a good match with the experiments (the experiments are not always right) or a reference solution due to modeling errors.

*“The multiscale nature of turbulence creates unique challenges for numerical simulations. Discretization methods must preserve the physical processes, reducing or eliminating artificial dissipation and dispersion ...*

*... How do you establish confidence in the numerical simulations of turbulent flows?”*

### References:

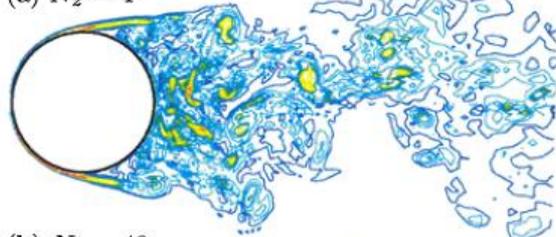
P. Moin. “Turbulence: V&V and UQ Analysis of a Multi-scale Complex System”. Center for Turbulence Research Stanford University

# Turbulence, does it matter?

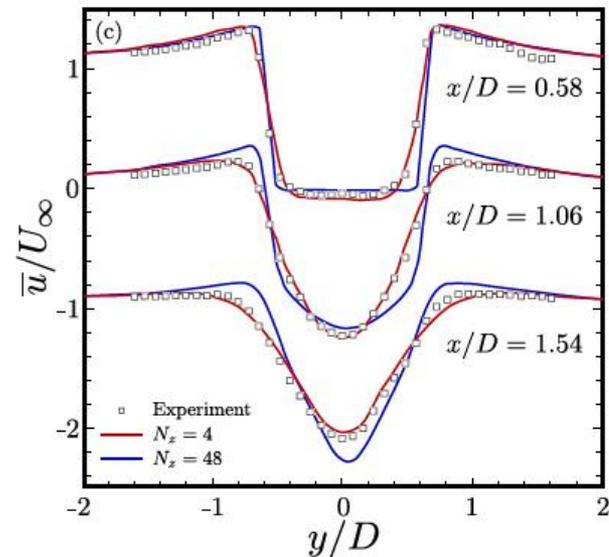
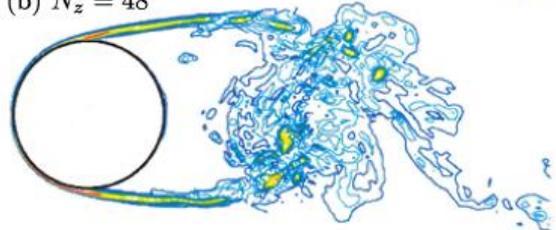
## Grid independent solutions and modeling errors

LES of Cylinder  $Re_D = 3900$

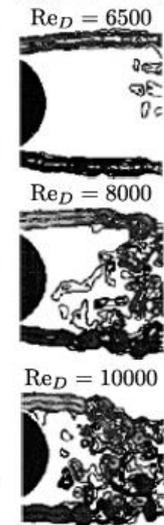
(a)  $N_z = 4$



(b)  $N_z = 48$



(d) PIV Data



- On the very last lecture, we are going to revisit again this image.
- Both cases are turbulent (**a** and **b** in the figure).
- I am going to ask you which solution do you think is right (**a** or **b** in the figure)?
- It is very difficult to answer this question only based on the image and the limited information available.
- But at that point in time, we will be able to do very educated guesses.

# Turbulence, does it matter?

## Turbulence is not a trivial problem

*“Turbulence is the most important unresolved problem of classical physics”*

Richard Feynman

*“Turbulence was probably invented by the devil on the seventh day of creation when the good lord was not looking”*

Peter Bradshaw

*“Turbulence is the graveyard of theories”*

Hans W. Liepmann

# Turbulence, does it matter?

## Turbulence is not a trivial problem

- This is probably my favorite quote, as it covers the largest elephants in CFD, mesh and turbulence.

*“Geometry modeling is to meshing what turbulence modeling is to computational fluid dynamics (CFD) – a mathematically complex model of something important that we try to treat as the proverbial black box.”*

John Chawner - Pointwise

# Roadmap to Lecture 2

- ~~1. The turbulent world around us~~
- ~~2. Turbulence, does it matter?~~
- 3. Introduction to turbulence modeling – Basic concepts**
- ~~4. Wall bounded flows and shear flows~~
- ~~5. A peek to the turbulence closure problem, some correlations in turbulence modeling, and the energy cascade~~

*“Essentially, all models are wrong,  
but some are useful”*

G. E. P. Box



## **George Edward Pelham Box**

18 October 1919 – 28 March 2013. Statistician, who worked in the areas of quality control, time-series analysis, design of experiments, and Bayesian inference. He has been called *“one of the great statistical minds of the 20th century”*.

Source: [https://en.wikipedia.org/wiki/George\\_E.\\_P.\\_Box](https://en.wikipedia.org/wiki/George_E._P._Box)

# Introduction to turbulence modeling – Basic concepts

## Turbulence modeling in engineering

- Most natural and engineering flows are turbulent, hence the necessity of modeling turbulence.
- The goal of turbulence modeling is to develop equations that predict the time averaged velocity, pressure, temperature fields without calculating the complete turbulent flow pattern as a function of time.
- Turbulence can be wall bounded or free shear, and depending on what you want to simulate, you will need to choose an appropriate turbulence model.
- There is no universal turbulence model, hence you need to know the capabilities and limitations of the turbulence models.
- Due to the multi-scale and unsteady nature of turbulence, modeling it is not an easy task.

# Introduction to turbulence modeling – Basic concepts

## Turbulence modeling in numerical simulations

- The objectives of turbulence models in numerical simulations is to discretize the modeled equations on a mesh or grid of adequate size, so that the processing time will not be too large.
- Thus, the idea is not to use a theory to provide an instantaneous turbulent solution of all scales, but to provide a mean numerical solution on a rough grid, using a model.
- The important point is the non-linearity of the Navier–Stokes equations. The averaged equations are not closed and are expressed using small-scale instantaneous fluctuations, through the Reynolds tensor.
- The introduction of a model is then necessary to close the equations, and provide, through an appropriate hypothesis, a closure expressing the Reynolds stress tensor using averaged quantities.
- Simulating turbulent flows in any general CFD solver (e.g., OpenFOAM, SU2, Fluent, CFX, Star-CCM+) requires selecting a turbulence model, providing initial conditions and boundary conditions for the closure equations of the turbulent model, selecting a near-wall modeling, generating an adequate mesh, and choosing runtime parameters and numerics.

### Reference:

F. G. Schmitt. About Boussinesq's turbulent viscosity hypothesis: historical remarks and a direct evaluation of its validity. C. R. Mecanique 335 (2007) 617–627

# Introduction to turbulence modeling – Basic concepts

## Why turbulent flows are challenging?

- Unsteady aperiodic motion.
- All fluid properties and transported quantities exhibit random spatial and temporal variations.
- They are intrinsically three-dimensional due to vortex stretching.
- Strong dependence from initial conditions.
- Contains a wide range of scales (eddies).
- Therefore, in order to accurately model/resolve turbulent flows, the simulations must be three-dimensional, time-accurate, and with fine enough meshes such that all spatial scales are properly captured.
- Additional physics that makes turbulence modeling even harder:
  - Buoyancy, compressibility effects, heat transfer, multiphase flows, transition to turbulence, surface finish, combustion, adverse pressure gradients, high speed flows, shock waves, chemical reactions, source terms, moving bodies and so on.

# Introduction to turbulence modeling – Basic concepts

## Reynolds number and Rayleigh number

- It is well known that the Reynolds number characterizes if the flow is laminar or turbulent.
- So before doing a simulation or experiment, check if the flow is turbulent.
- The Reynolds number is defined as follows,

$$\begin{array}{l} \text{Convective effects} \longrightarrow \\ \text{Viscous effects} \longrightarrow \end{array} Re_L = \frac{\rho U L}{\mu} = \frac{U L}{\nu}$$
$$\nu = \frac{\mu}{\rho}$$

- Where  $U$  is a characteristic velocity, e.g., free-stream velocity.
- And  $L$  is representative length scale, e.g., length, height, diameter, etc.

# Introduction to turbulence modeling – Basic concepts

## Reynolds number and Rayleigh number

- If you are dealing with natural convection, you can use the Rayleigh number (Ra), Grashof number (Gr), and Prandtl number (Pr) to characterize the flow.

Buoyancy effects  $\longrightarrow$

Viscous effects  $\longrightarrow$

$$Ra = \frac{g\beta L^3 \Delta T}{\nu\alpha} = \frac{\rho^2 c_p \beta g L^3 \Delta T}{\mu k} = Gr \times Pr$$

Specific heat  $\downarrow$

Thermal expansion coefficient  $\swarrow$

Thermal conductivity  $\swarrow$

Momentum diffusivity  $\longrightarrow$

$$Pr = \frac{\nu}{\alpha} = \frac{\mu c_p}{k}$$

Thermal diffusivity  $\longrightarrow$

$$Gr = \frac{g\beta(T_S - T_\infty)L^3}{\nu^2}$$

# Introduction to turbulence modeling – Basic concepts

## Reynolds number and Rayleigh number

- Turbulent flow occurs at large Reynolds number.

- For external flows,

$$Re_x \geq 500000 \quad \text{Around slender/streamlined bodies (surfaces)}$$

$$Re_d \geq 20000 \quad \text{Around an obstacle (bluff bodies)}$$

- For internal flows,

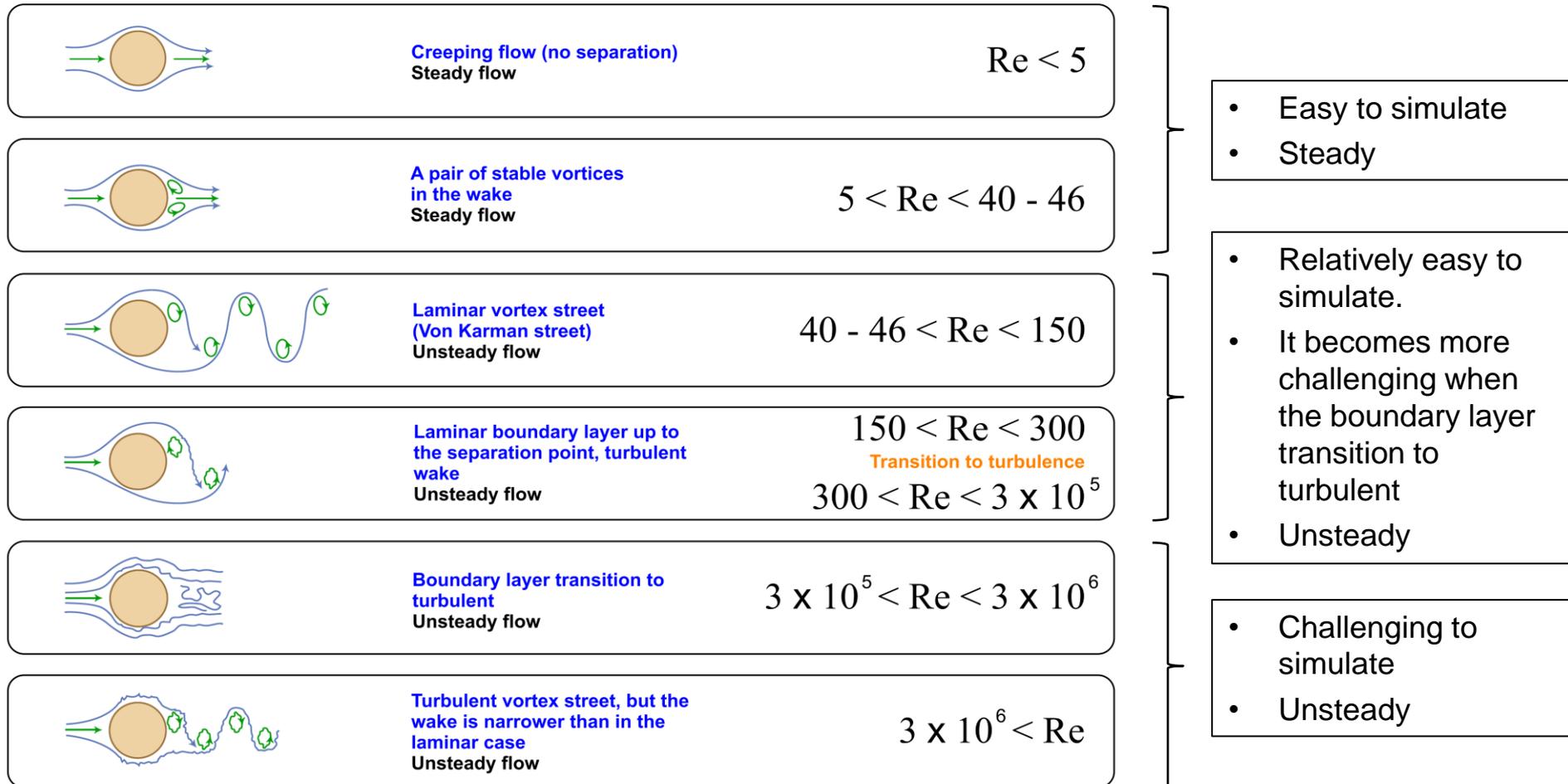
$$Re_{d_h} \geq 2300$$

- Notice that other factors such as free-stream turbulence, surface conditions, blowing, suction, roughness and other disturbances, may cause transition to turbulence at lower Reynolds number.
- If you are dealing with natural convection and buoyancy, turbulent flows occurs when

$$\frac{Ra}{Pr} \geq 10^9$$

# Introduction to turbulence modeling – Basic concepts

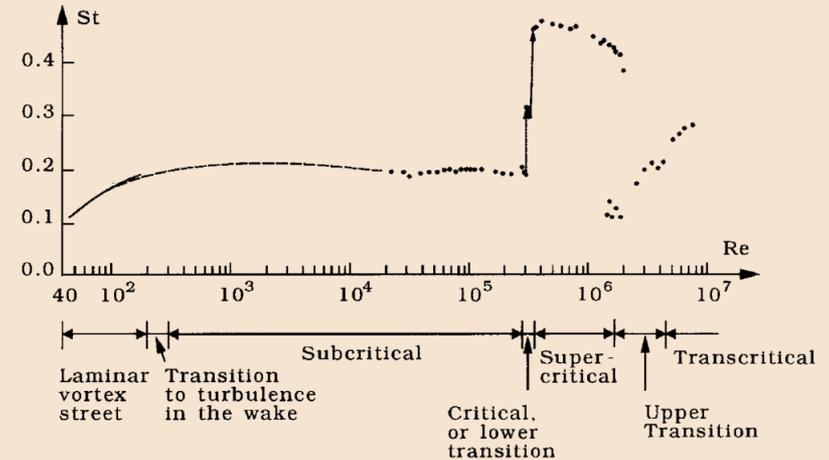
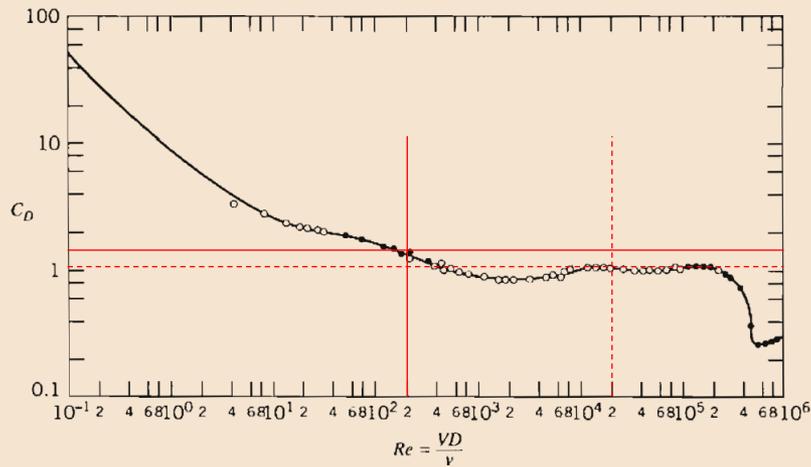
## What happens when we increase the Reynolds number?



Vortex shedding behind a cylinder and Reynolds number

# Introduction to turbulence modeling – Basic concepts

## What happens when we increase the Reynolds number?



Drag coefficient as a function of Reynolds number for a smooth cylinder [1]

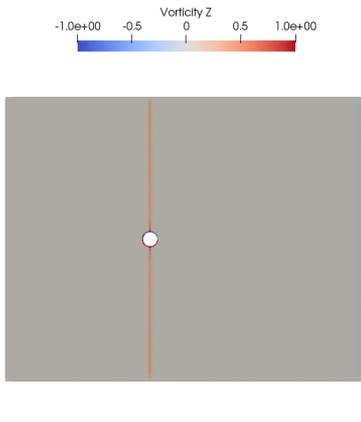
Strouhal number  $St = \frac{fL}{U}$  for a smooth cylinder [2]

### References:

1. Fox, Robert W., et al. Introduction to Fluid Mechanics. Hoboken, NJ, Wiley, 2010
2. Sumer, B. Mutlu, et al. Hydrodynamics Around Cylindrical Structures. Singapore, World Scientific, 2006

# Introduction to turbulence modeling – Basic concepts

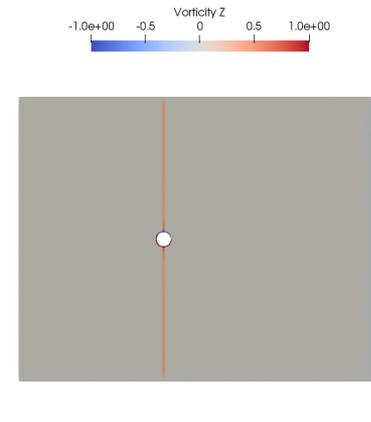
## What happens when we increase the Reynolds number?



Time: 0.000000

**Reynolds = 20 – Non-uniform initialization**  
**Laminar flow with separation**

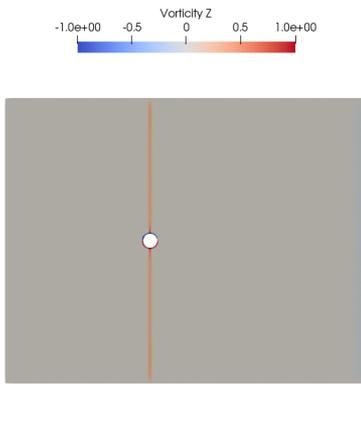
<http://www.wolfdynamics.com/training/turbulence/unscyl1.gif>



Time: 0.000000

**Reynolds = 200 – Non-uniform initialization**  
**Laminar flow with vortex shedding**

<http://www.wolfdynamics.com/training/turbulence/unscyl3.gif>

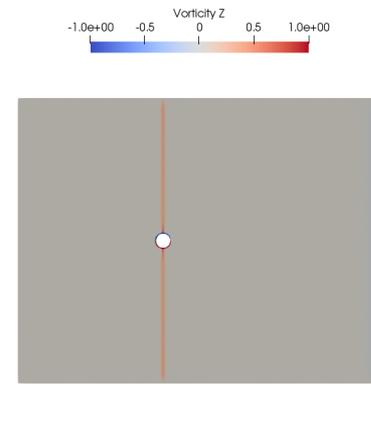


Time: 0.000000

**Reynolds = 50 – Non-uniform initialization**

**Laminar flow with vortex shedding (maybe on the limit of the onset of the Von Karman street.**

<http://www.wolfdynamics.com/training/turbulence/unscyl2.gif>



Time: 0.000000

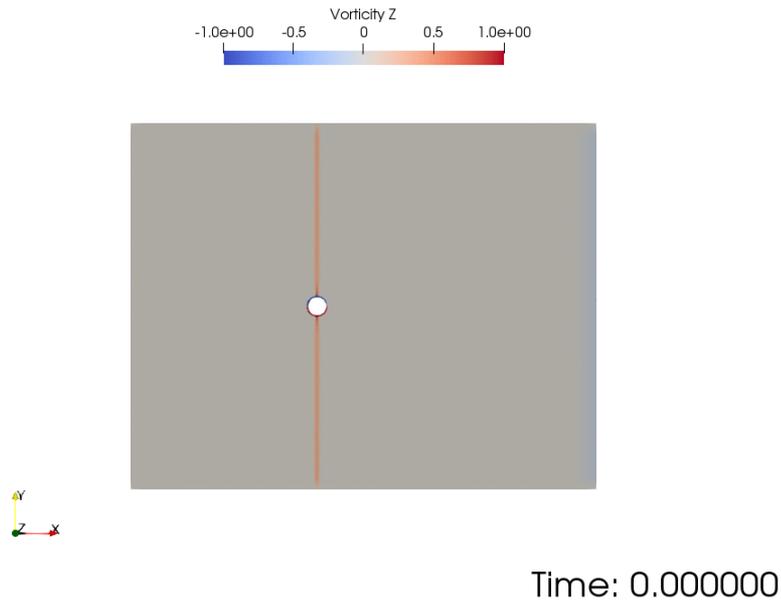
**Reynolds = 20000 – Non-uniform initialization**

**Turbulent flow with vortex shedding (turbulence model enable)**

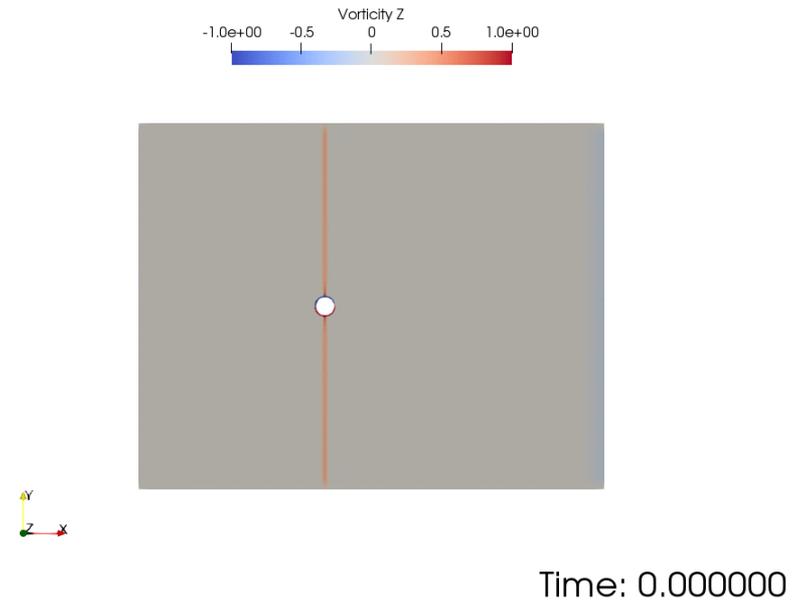
<http://www.wolfdynamics.com/training/turbulence/unscyl4.gif>

# Introduction to turbulence modeling – Basic concepts

## What happens when we increase the Reynolds number?



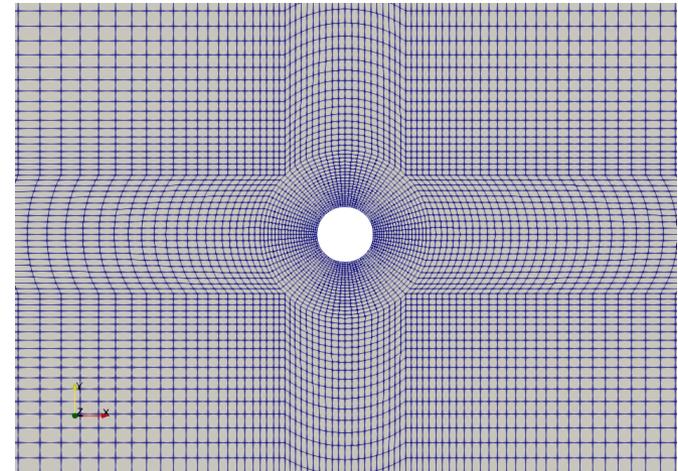
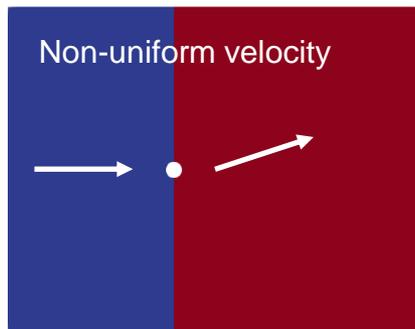
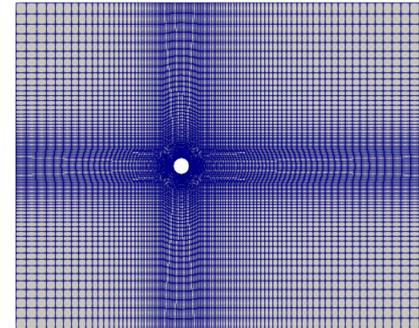
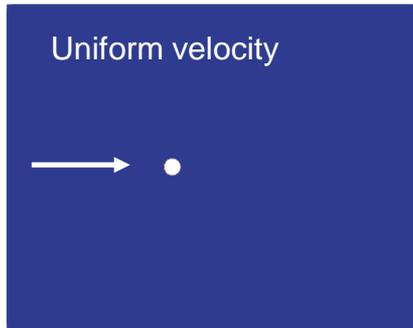
Reynolds = 20000 – Non-uniform initialization  
No turbulence model enable  
<http://www.wolfdynamics.com/training/turbulence/unscyl5.gif>



Reynolds = 20000 – Non-uniform initialization  
Turbulence model enable (k-omega SST)  
<http://www.wolfdynamics.com/training/turbulence/unscyl4.gif>

# Introduction to turbulence modeling – Basic concepts

What happens when we increase the Reynolds number?

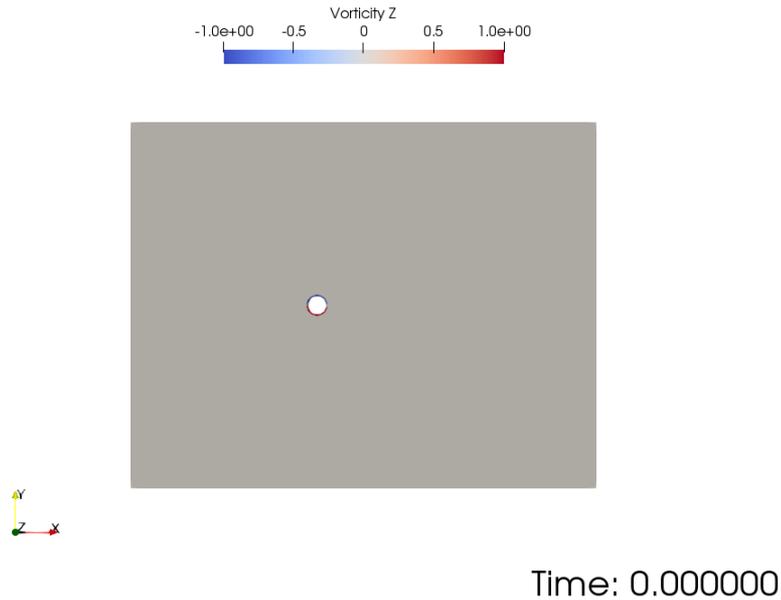


Field initialization - Velocity

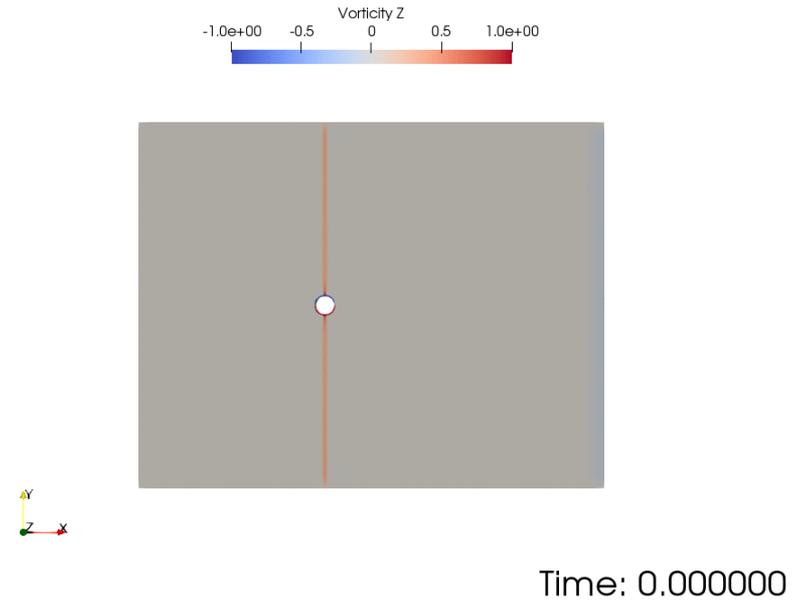
Mesh

# Introduction to turbulence modeling – Basic concepts

## What happens when we increase the Reynolds number?



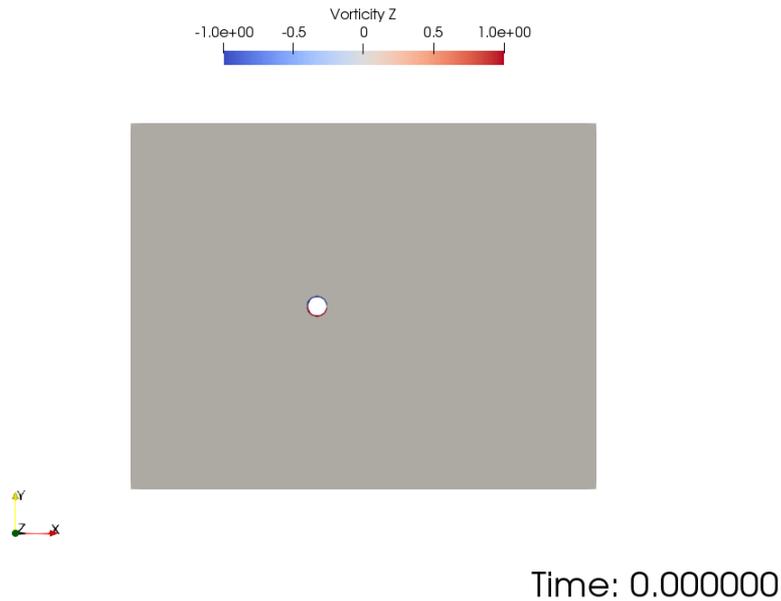
Reynolds = 20000 – Uniform initialization  
Turbulence model enable (k-omega SST)  
<http://www.wolfdynamics.com/training/turbulence/unscyl6.gif>



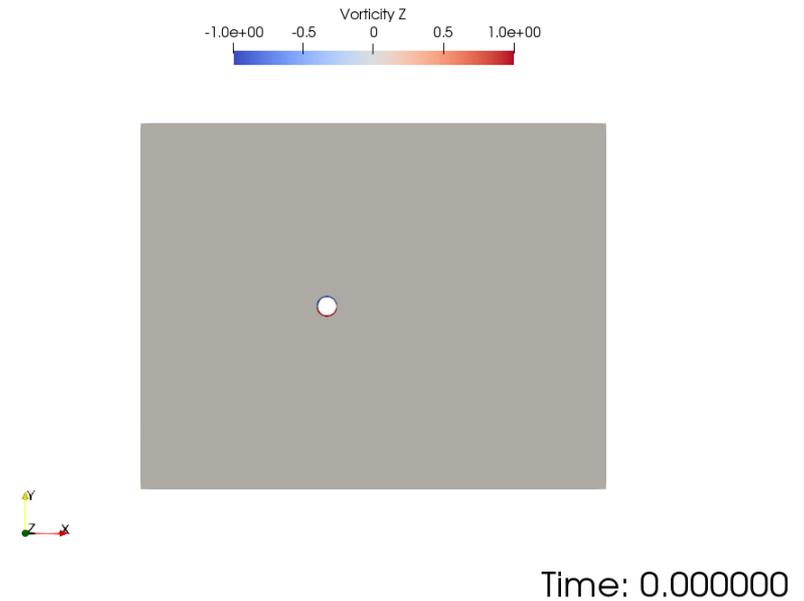
Reynolds = 20000 – Non-uniform initialization  
Turbulence model enable (k-omega SST)  
<http://www.wolfdynamics.com/training/turbulence/unscyl4.gif>

# Introduction to turbulence modeling – Basic concepts

## What happens when we increase the Reynolds number?



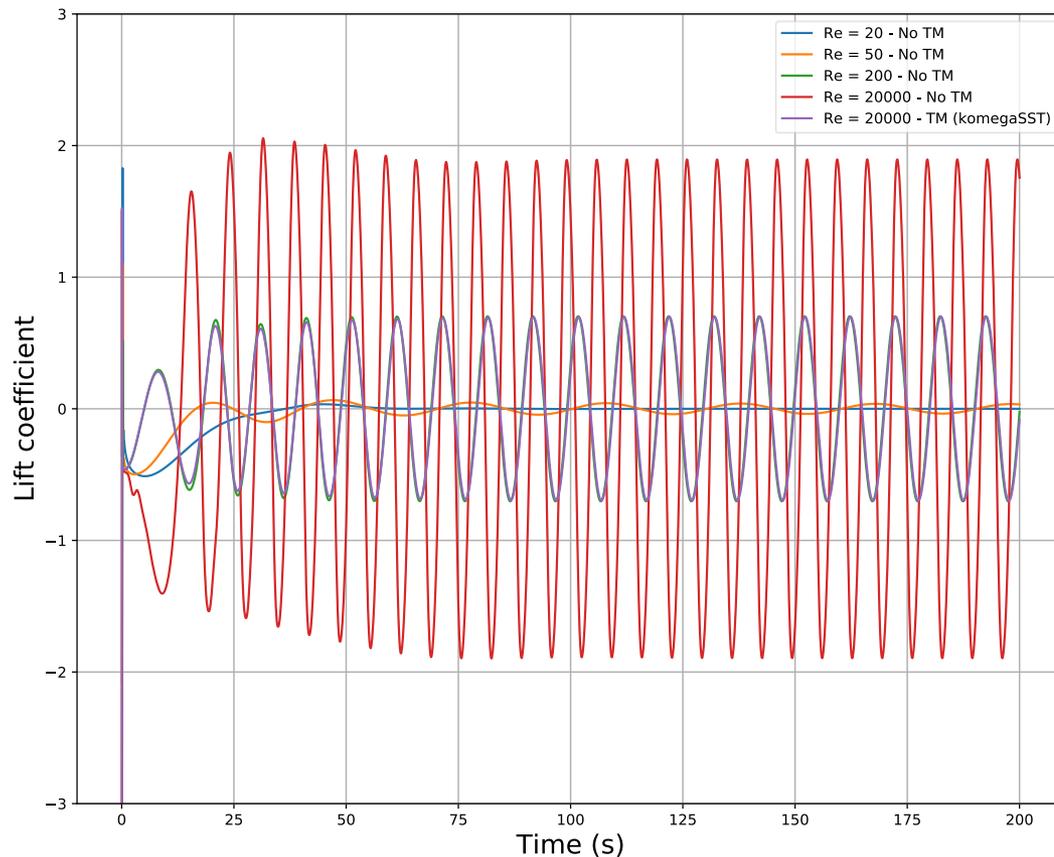
Reynolds = 20000 – Uniform initialization  
Turbulence model enable (k-omega SST)  
<http://www.wolfdynamics.com/training/turbulence/unscyl6.gif>



Reynolds = 20000 – Uniform initialization  
Turbulence model enable (LES Smagorinsky)  
<http://www.wolfdynamics.com/training/turbulence/unscyl7.gif>

# Introduction to turbulence modeling – Basic concepts

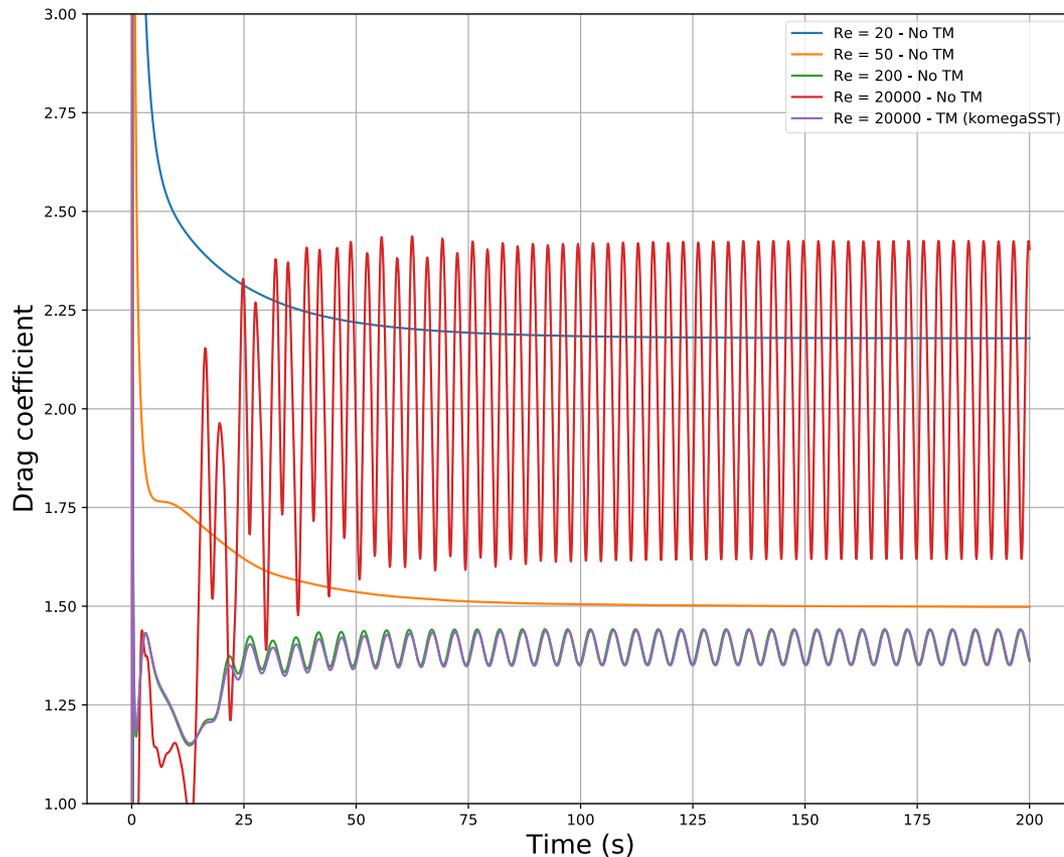
## What happens when we increase the Reynolds number?



Reynolds	Turbulence model	Mean $c_l$
20	No	-0.00012
50	No	0.00274
200	No	-0.00149
20000	No	0.02176
20000	K-Omega SST	-0.00214

# Introduction to turbulence modeling – Basic concepts

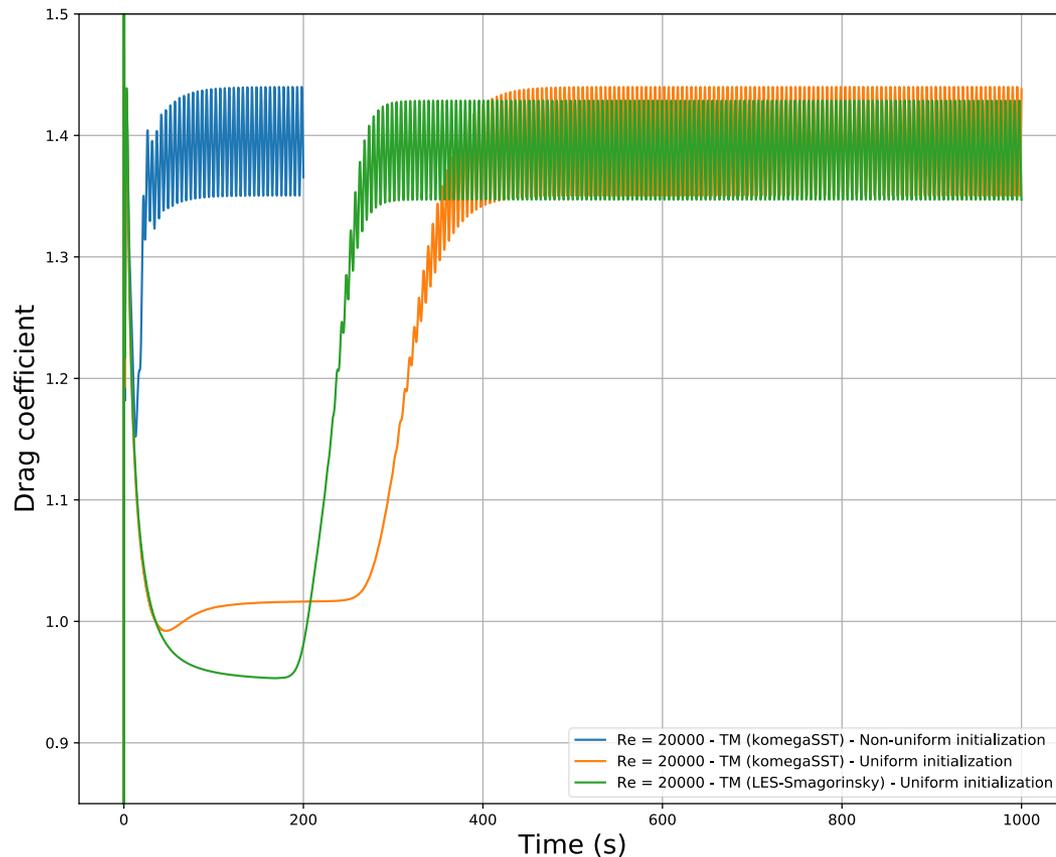
## What happens when we increase the Reynolds number?



Reynolds	Turbulence model	Mean $c_d$
20	No	2.17987
50	No	1.50056
200	No	1.39786
20000	No	2.05043
20000	K-Omega SST	1.39459

# Introduction to turbulence modeling – Basic concepts

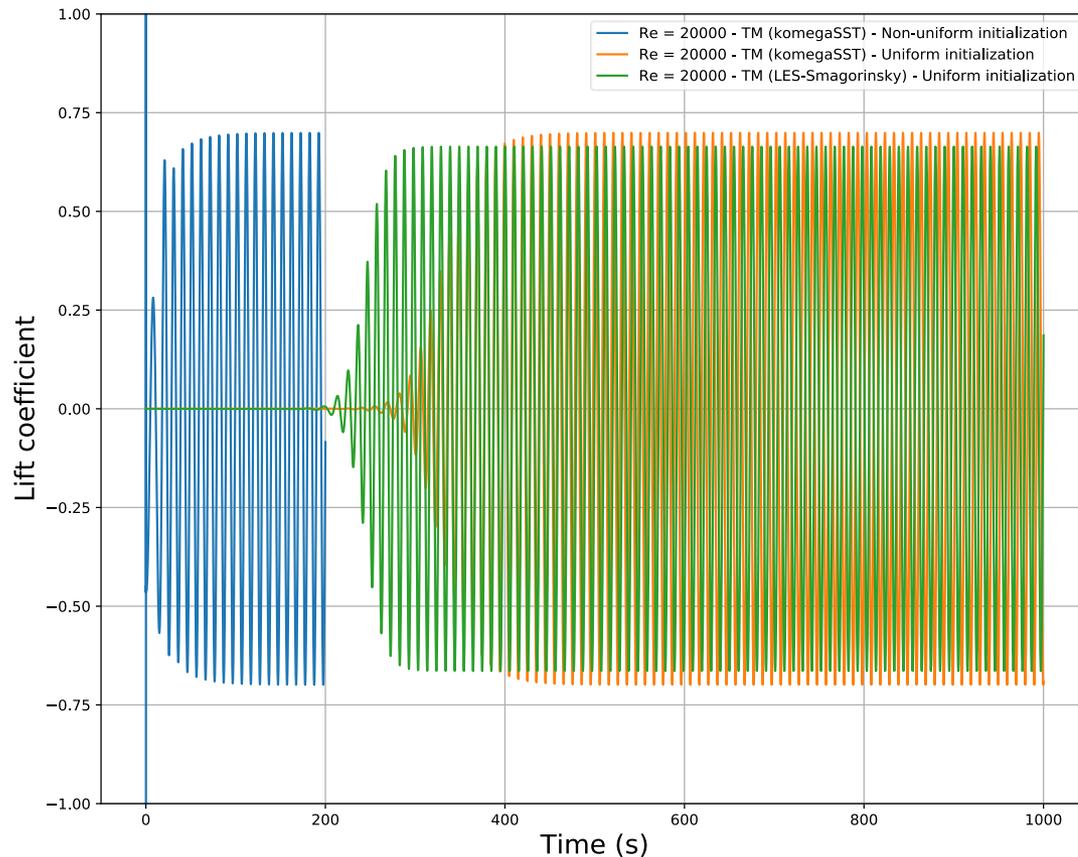
## What happens when we increase the Reynolds number?



Reynolds	Turbulence model	Mean $c_d$
20000	K-Omega SST (NUI)	1.39786
20000	K-Omega SST (UI)	1.39617
20000	LES-Smagorinsky (UI)	1.38865

# Introduction to turbulence modeling – Basic concepts

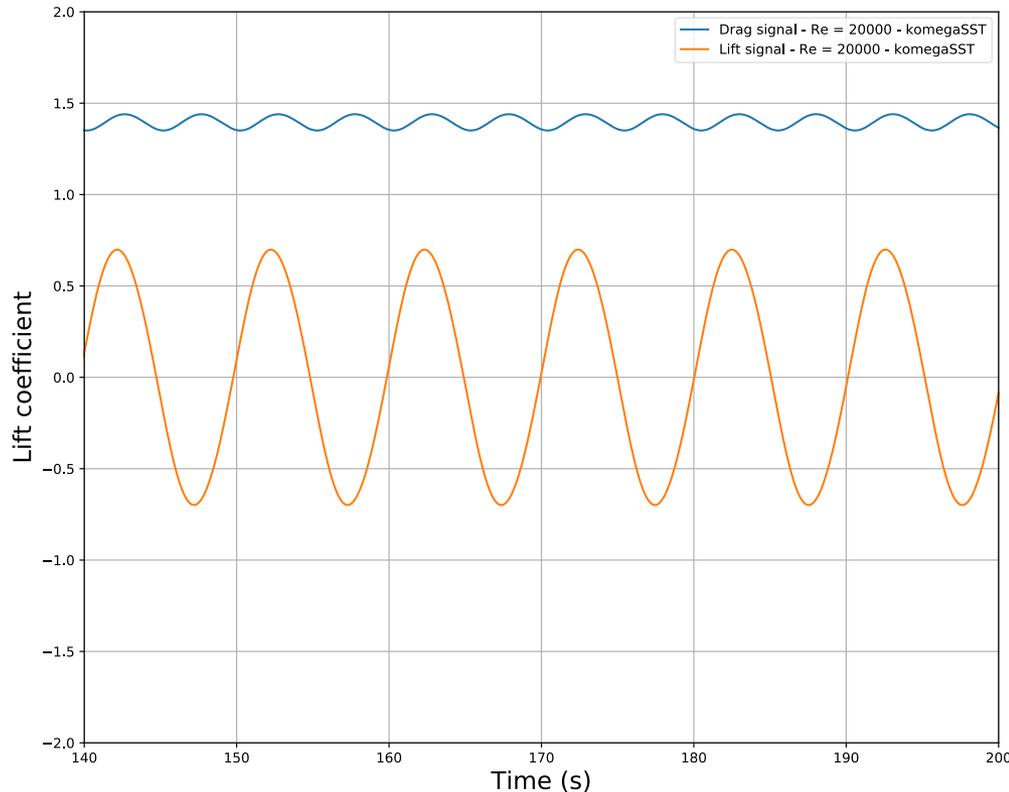
## What happens when we increase the Reynolds number?



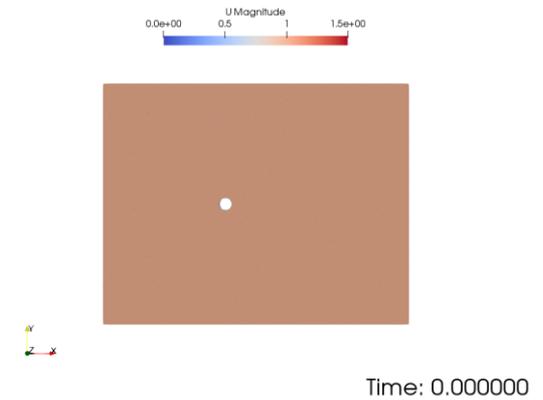
Reynolds	Turbulence model	Mean $c_l$
20000	K-Omega SST (NUI)	-0.00214
20000	K-Omega SST (UI)	0.00190
20000	LES-Smagorinsky (UI)	-0.00118

# Introduction to turbulence modeling – Basic concepts

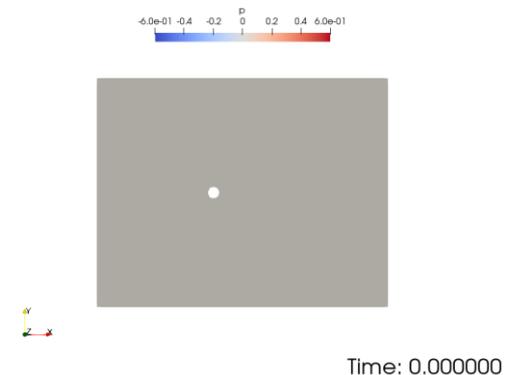
## What happens when we increase the Reynolds number?



<http://www.wolfdynamics.com/training/turbulence/unscyl8.gif>



<http://www.wolfdynamics.com/training/turbulence/unscyl9.gif>



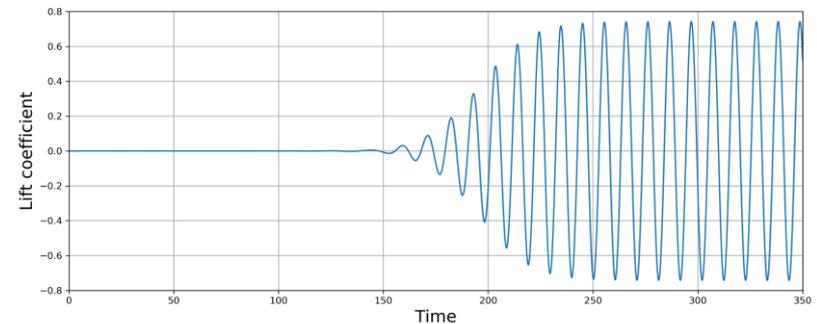
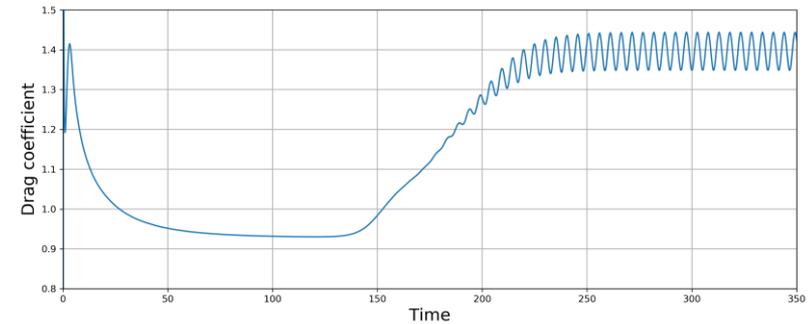
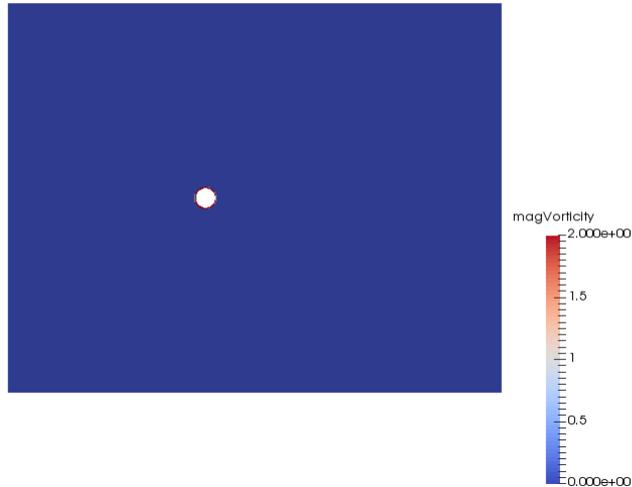
- Do you notice anything peculiar in the force coefficient signals?
- Look at the frequencies?
- Try different Reynolds number, do you see the same behavior?



# Introduction to turbulence modeling – Basic concepts

## Vorticity does not always mean turbulence

Time: 0.000000



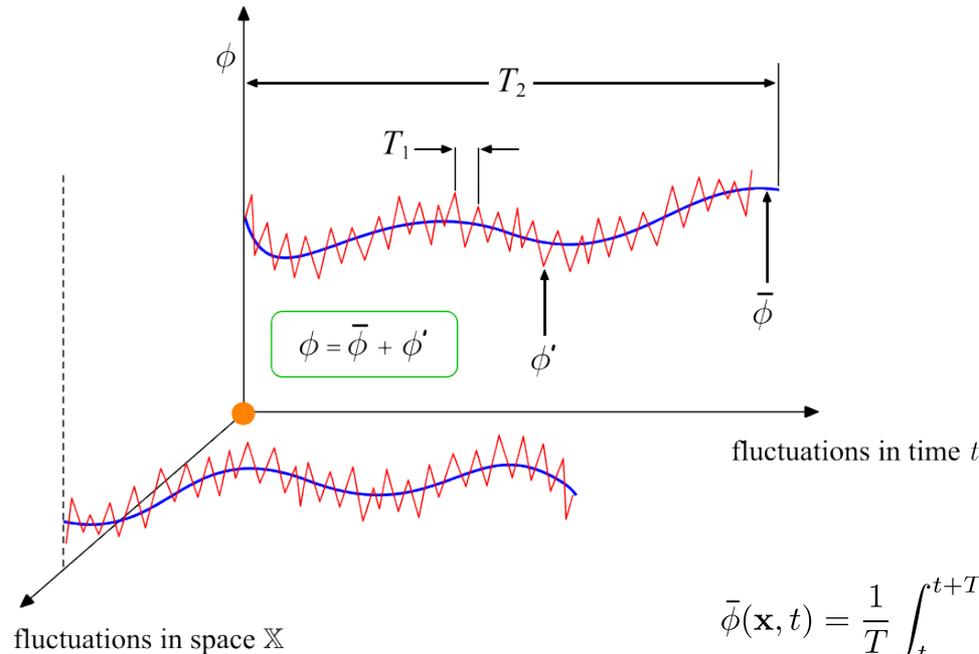
### Instantaneous vorticity magnitude field

<http://www.wolfdynamics.com/training/turbulence/image6.gif>

- The Reynolds number in this case is 200, for these conditions, the flow still is laminar.
- We are in the presence of the Von Karman vortex street, which is the periodic shedding of vortices caused by the unsteady separation of the fluid around blunt bodies.
- Vorticity is not a direct indication of turbulence.
- However, turbulent flows are rotational, they exhibit vortical structures.

# Introduction to turbulence modeling – Basic concepts

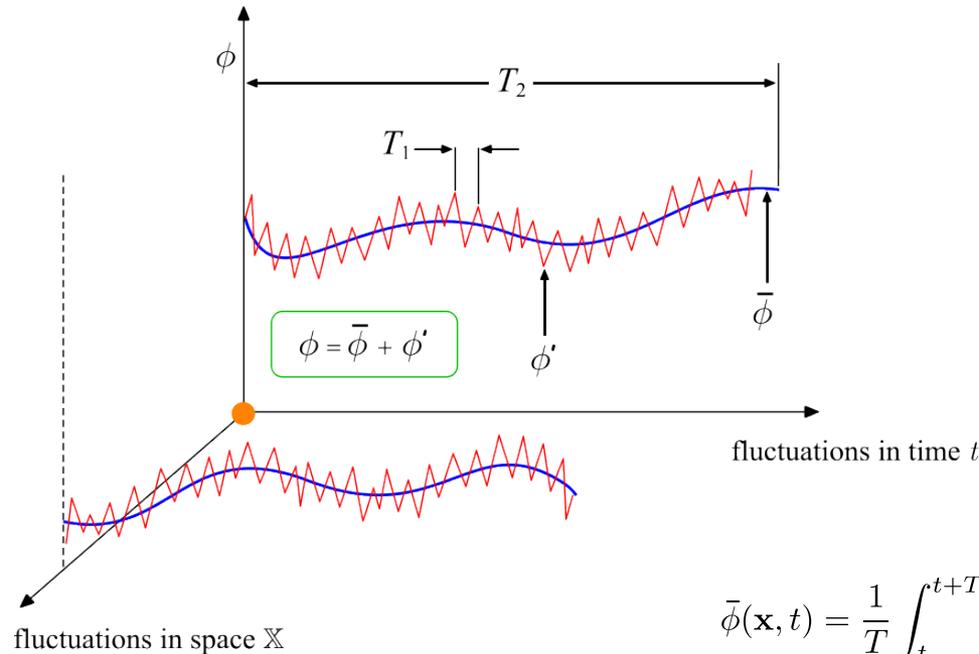
## Turbulence modeling – Fluctuations of transported quantities



- We have defined turbulence as an unsteady, aperiodic motion in which velocity components and every transported quantity fluctuate in space and time.
- For most engineering applications it is impractical to account for all these instantaneous fluctuations.
- Therefore, we need to somehow remove, avoid, or filter those small scales by using models.

# Introduction to turbulence modeling – Basic concepts

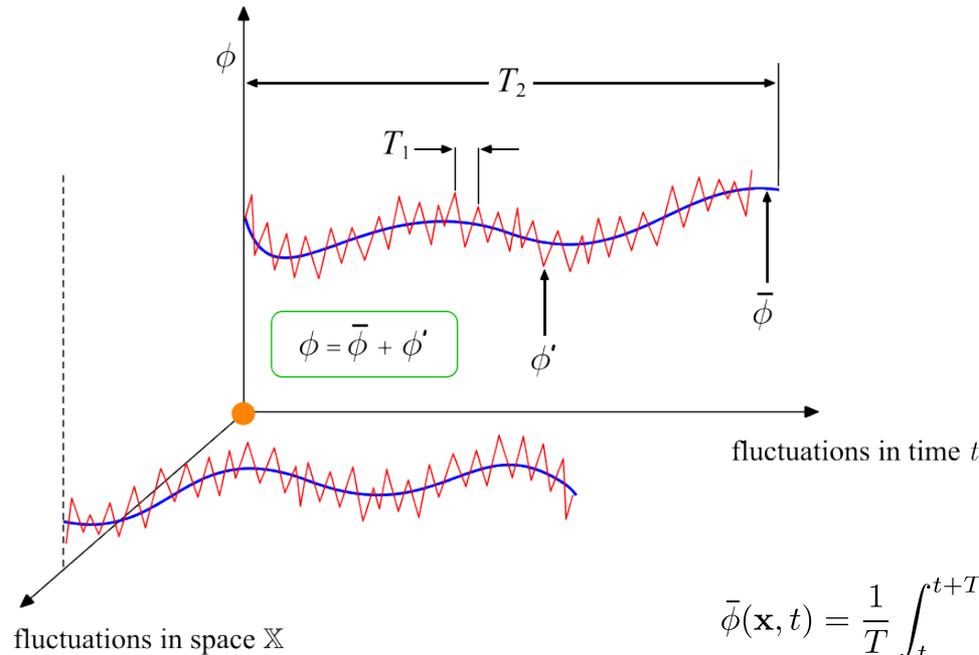
## Turbulence modeling – Fluctuations of transported quantities



- To remove, avoid, or filter the instantaneous fluctuations (or small scales), two methods can be used: Reynolds averaging and filtering the governing equations.
- Both methods introduce additional terms that must be modeled for closure, Turbulence Modeling.
- We are going to talk about closure methods later.

# Introduction to turbulence modeling – Basic concepts

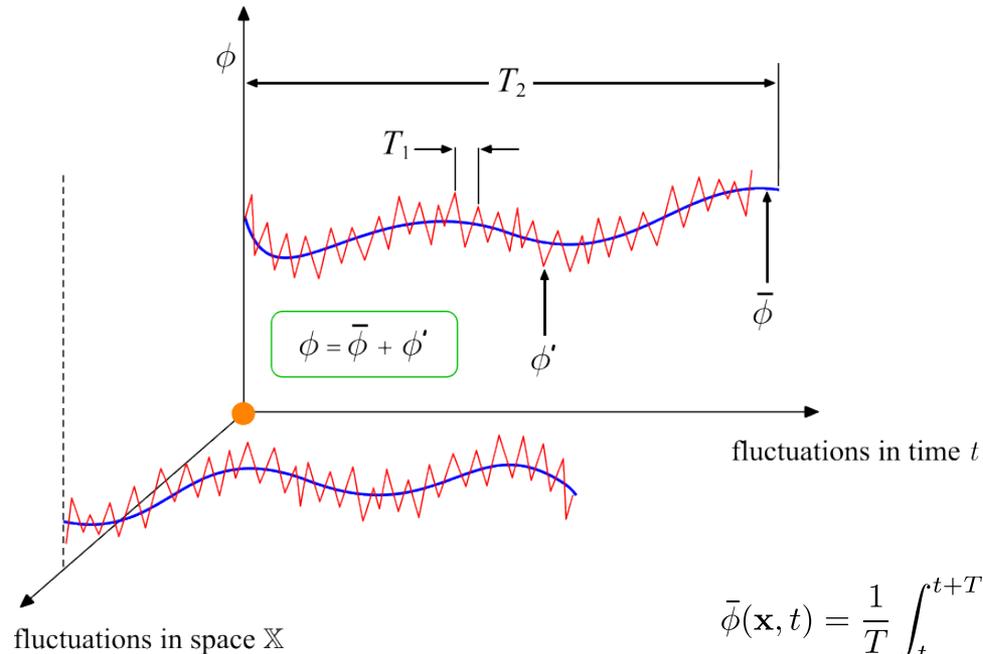
## Turbulence modeling – Fluctuations of transported quantities



- The objective of turbulence modeling is to develop equations that will predict the time averaged primitive fields (velocity, pressure, temperature, concentration, and so on), without calculating the complete turbulent flow pattern as a function of time.

# Introduction to turbulence modeling – Basic concepts

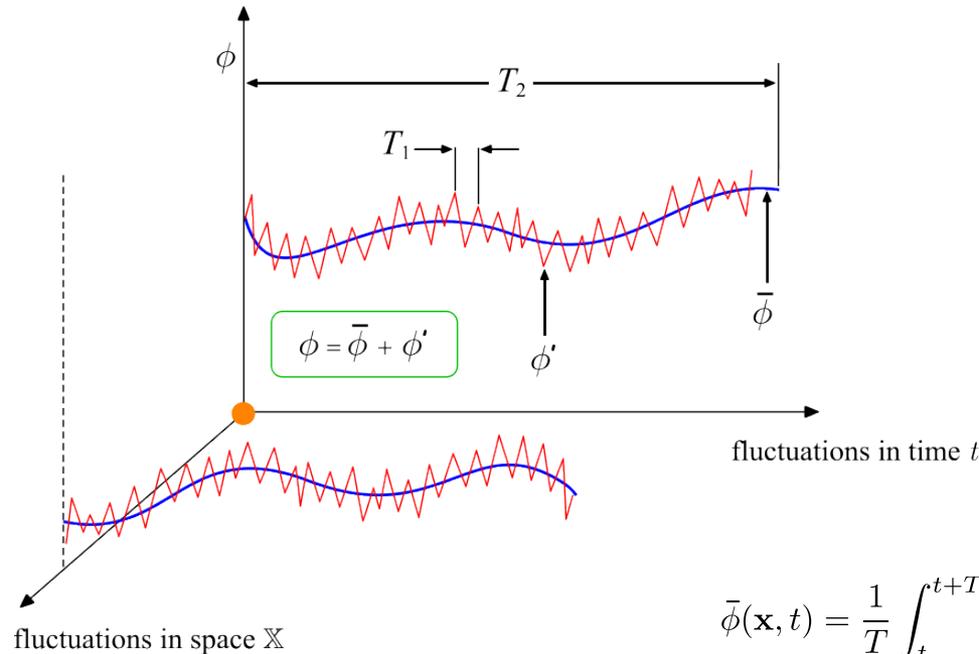
## Turbulence modeling – Fluctuations of transported quantities



- In other words, we do not want to resolve all the space and time scales.
  - This reduces the computational time and resources.
  - However, you can also compute instantaneous values and calculate other statistical properties (e.g., RMS, two point-correlations, PDF, and so on).
  - Turbulence modeling is very accurate, if you know what are you doing.

# Introduction to turbulence modeling – Basic concepts

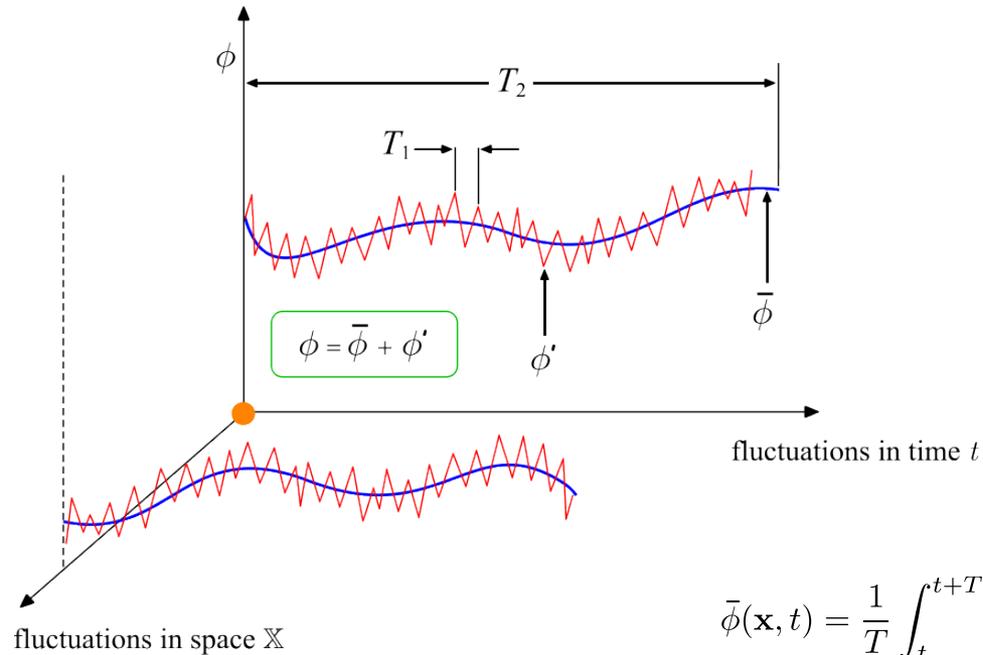
## Turbulence modeling – Fluctuations of transported quantities



- Important to understand:
  - The time averaged flow pattern is a statistical property of the flow.
  - It is not the actual flow pattern.
  - The flow pattern changes from instant to instant.
  - In engineering applications, most of the time it is enough to know the average value.

# Introduction to turbulence modeling – Basic concepts

## Turbulence modeling – Fluctuations of transported quantities

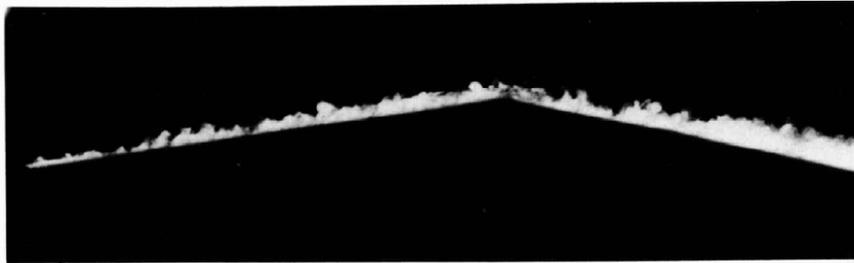


$$\bar{\phi}(\mathbf{x}, t) = \frac{1}{T} \int_t^{t+T} \phi(\mathbf{x}, t) dt, \quad T_1 \ll T \ll T_2$$

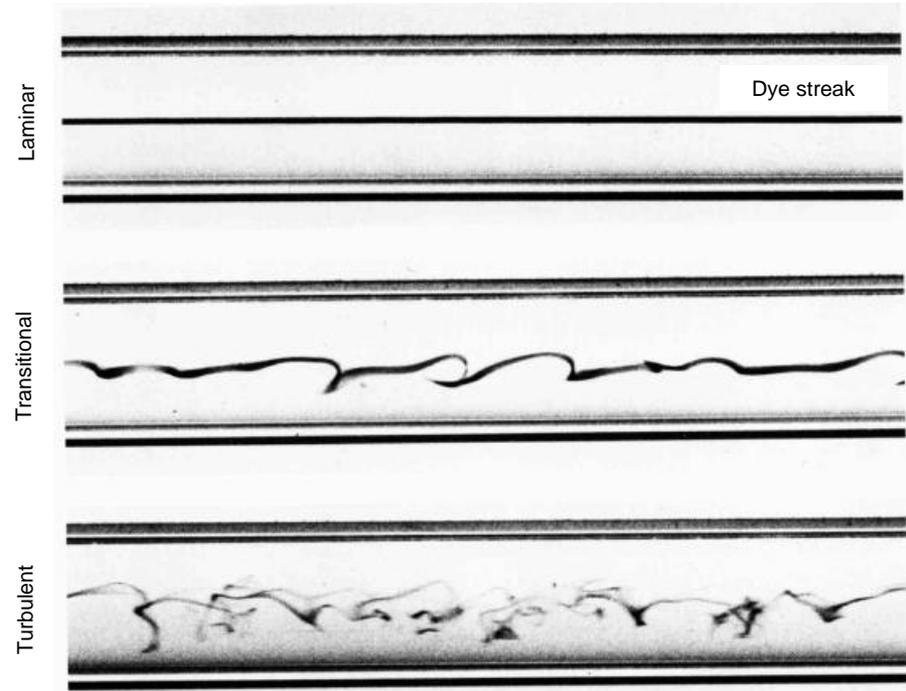
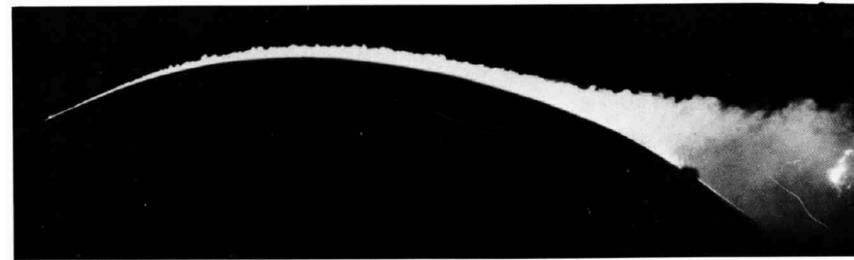
- Later we are going to make a distinction between averaging stationary turbulence, averaging nonstationary turbulence, and statistically steady turbulence.

# Introduction to turbulence modeling – Basic concepts

## Turbulence modeling – Wall bounded and shear free turbulence



Wall bounded turbulence

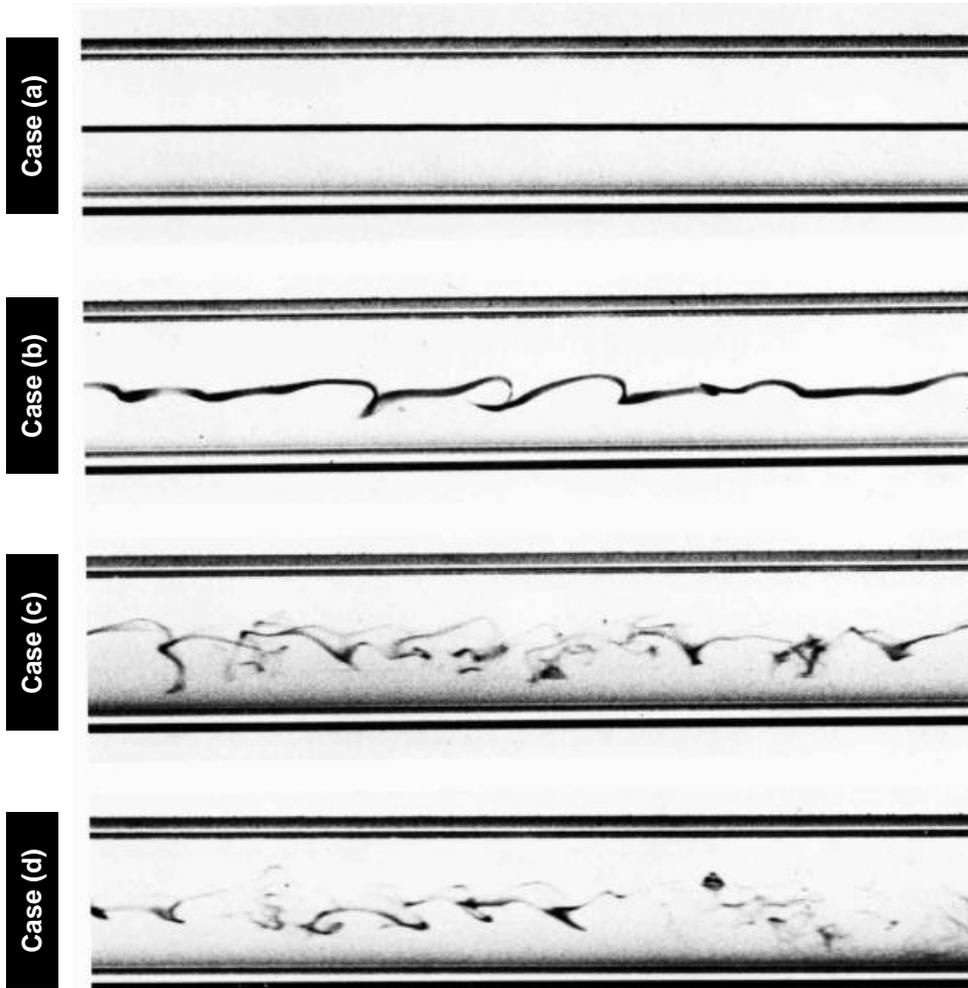


Shear free turbulence

- **Turbulent flows can originate at the walls.** When this is the case, we talk about wall bounded turbulence.
- **Turbulent flows can also originate in the absence of walls (or far from walls).** When this is the case, we talk about shear free turbulence (usually jets, mixing layers, heated walls, atmospheric flows).
- But indifferently of the type of turbulence, that is, wall bounded or shear free, turbulent motion has a direct effect on the velocity profiles, shear stresses, and mixing of transported quantities (heat transfer rate, species concentration, mass transfer, and so on).

# Introduction to turbulence modeling – Basic concepts

## Turbulence modeling – Wall bounded and shear free turbulence



- Turbulence has a direct effect on the velocity profiles and mixing of transported quantities.
  - **Case (a)** corresponds to a laminar flow, where the dye do not show any oscillation and can mix with the main flow only via molecular diffusion, this kind of mixing can take very long times.
  - **Case (b)** shows a transitional state where the dye streak becomes wavy, but the main flow still is laminar.
  - **Case (c) and case (d)** show the turbulent state, where the dye streak changes direction erratically, and the dye has mixed significantly with the main flow due to the velocity fluctuations.
- In the figure, a filament of colored water injected into pipe flow (left to right), and the flow velocity is increased from top to bottom.
- This image give us an idea of what happens at the core of the flow, but what about the walls?

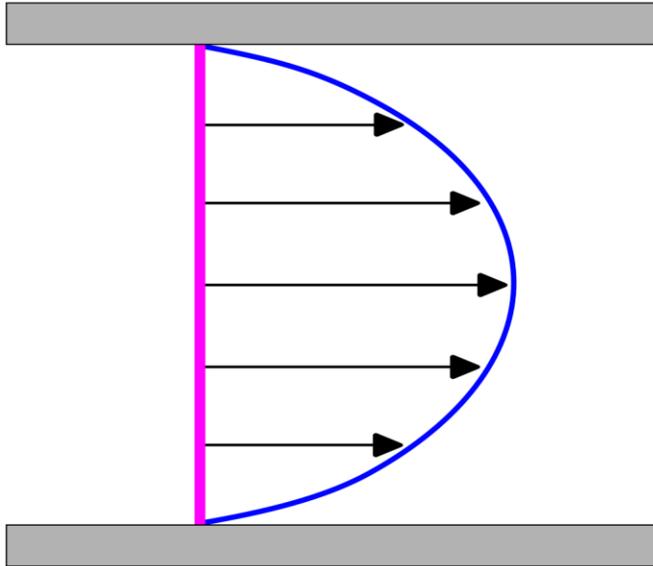
### Repetition of Reynolds' dye experiment.

Photo credit: M. Van Dyke. An Album of Fluid Motion. The Parabolic Press, Stanford, California, 1982.

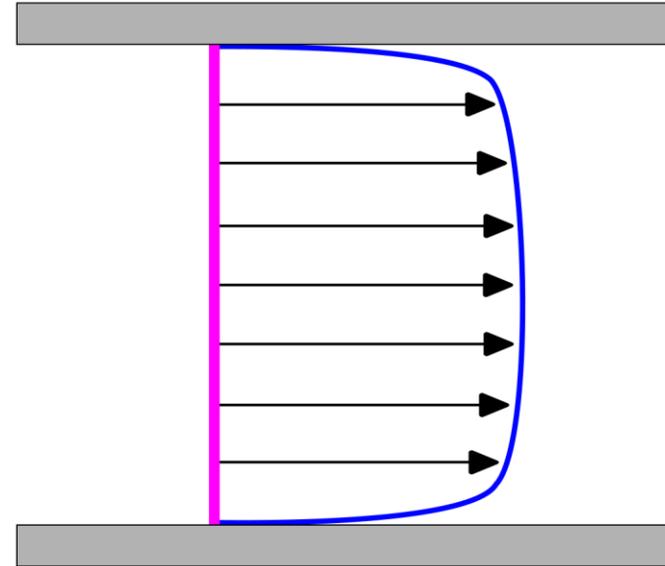
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# Introduction to turbulence modeling – Basic concepts

## Turbulence modeling – Wall bounded and shear free turbulence



Laminar flow in a pipe

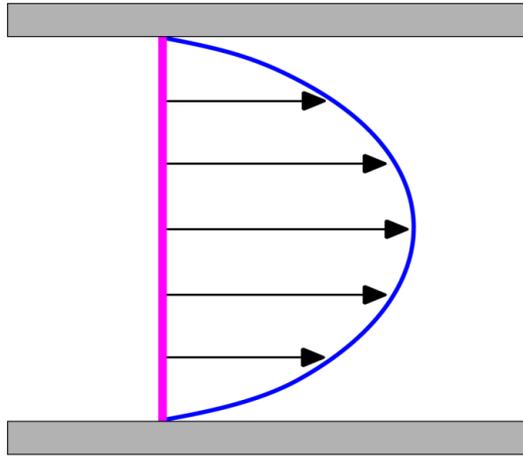


Turbulent flow in a pipe

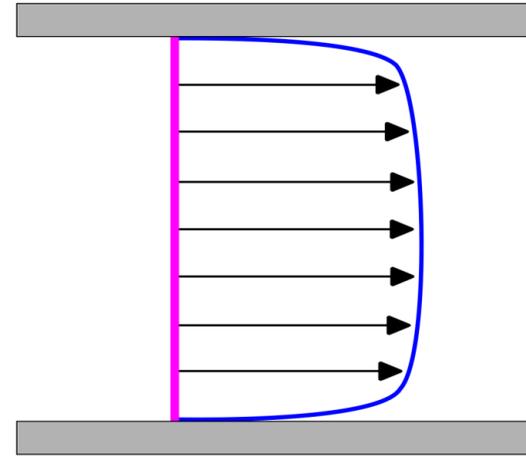
- Turbulence has a direct effect on the velocity profiles and mixing of transported quantities.
  - In the **laminar case**, the velocity gradient close to the walls is small (therefore the shear stresses are lower).
  - The **turbulent case** shows two regions. One thin region close to the walls with very large velocity gradients (hence large shear stresses), and a region far from the wall where the velocity profile is nearly uniform.
  - In the illustration, the velocity profile of the turbulent case has been averaged.
  - In reality, random fluctuations of the velocity field and transported quantities are present.

# Introduction to turbulence modeling – Basic concepts

## Turbulence modeling – Wall bounded and shear free turbulence



Laminar flow in a pipe



Turbulent flow in a pipe

- Turbulence has a direct effect on the velocity profiles and mixing of transported quantities.
  - The larger the velocity gradient close to the walls, the larger the wall shear stresses will be.
  - In a laminar flow or in the viscous sub-layer\*, the wall shear stress  $\tau_{wall}$  can be approximated as follows,

$$\tau_{wall} = \mu \left. \frac{\partial u}{\partial y} \right|_{y=0}$$

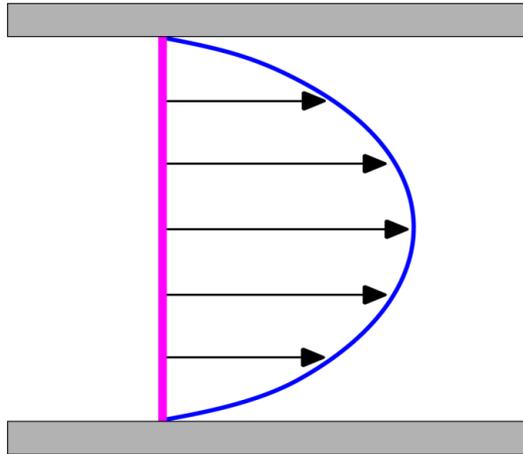
**Note:**

This approximation is valid for 2D boundary layers

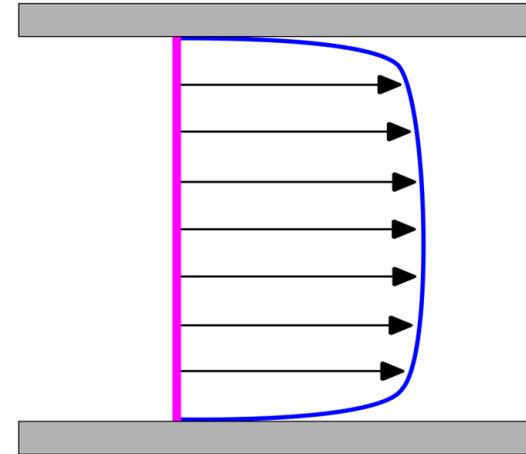
\* The viscous sub-layer is region of the turbulent boundary layer very close to the wall where the flow is laminar.

# Introduction to turbulence modeling – Basic concepts

## Turbulence modeling – Wall bounded and shear free turbulence



Laminar flow in a pipe



Turbulent flow in a pipe

- Turbulence has a direct effect on the velocity profiles and mixing of transported quantities.
  - In a turbulent flow, the wall shear stress  $\tau_{wall}$  cannot be approximated using the same relation as for laminar flows.
  - We need to add a correction to take into account the effects of the increased mixing, randomness, agitation, of turbulence flows.

$$\tau_{wall} = \mu \left. \frac{\partial u}{\partial y} \right|_{y=0}$$

$$+ \tau^R$$

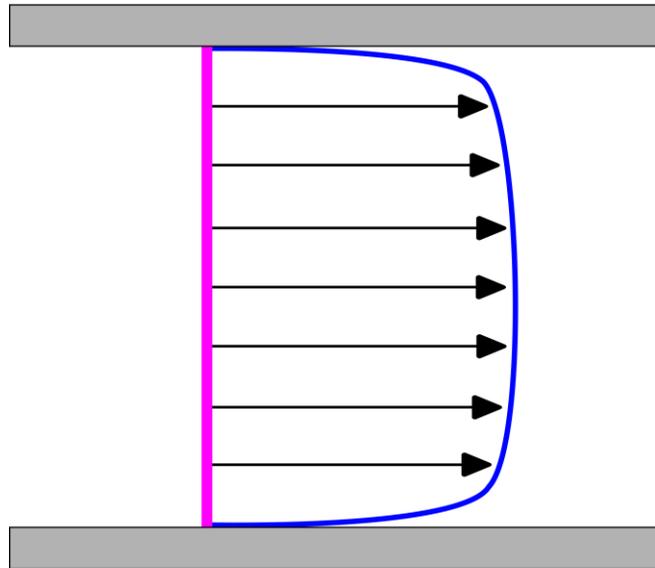
Turbulence modeling is about how to approximate/model this term

**Note:**

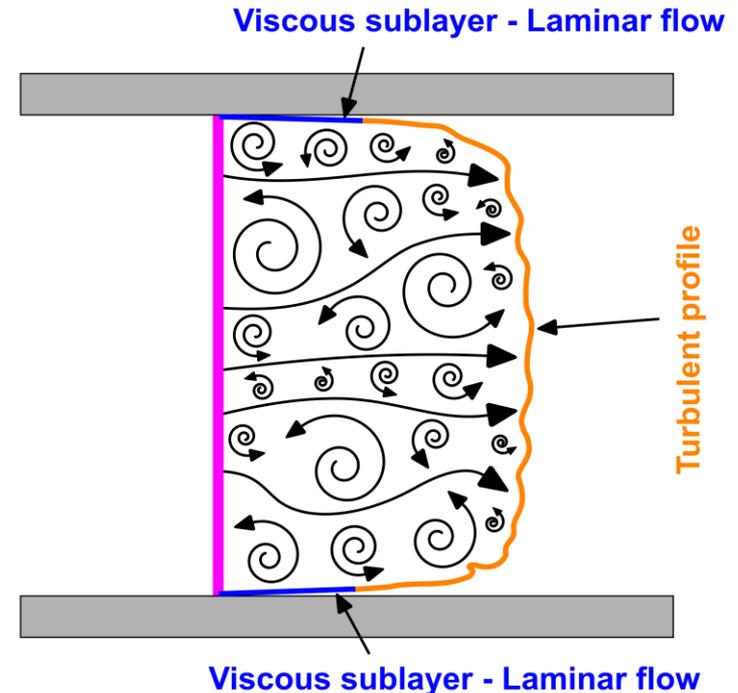
This approximation is valid for 2D boundary layers and where  $\tau^R = \overline{u'v'}$

# Introduction to turbulence modeling – Basic concepts

## Turbulence modeling – Wall bounded and shear free turbulence



Averaged turbulent flow

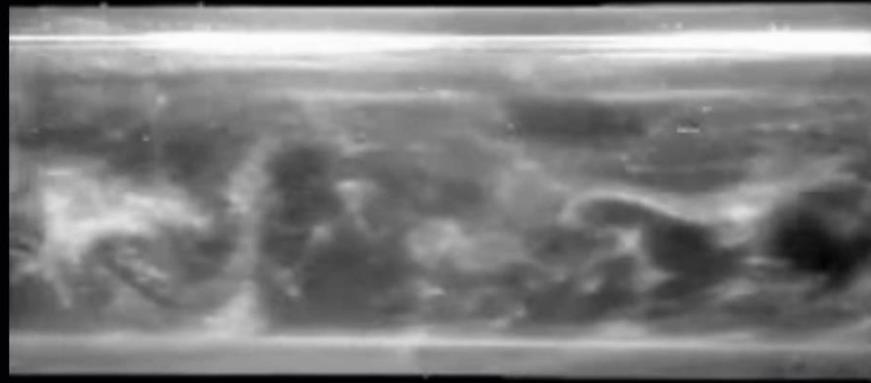


Instantaneous turbulent flow

- In the left figure, the velocity profile has been averaged.
- In reality, the velocity profile fluctuates in time (right figure).
- The thin region close to the walls has very large velocity gradients and is laminar.
- Far from the flows, the flow becomes turbulent.
- Turbulence increases the wall shear stresses and enhances mixing.

# Introduction to turbulence modeling – Basic concepts

## Turbulence modeling – Fluctuations of transported quantities



Turbulent flow in a pipe

[www.wolfdynamics.com/training/turbulence/video-pipe1.gif](http://www.wolfdynamics.com/training/turbulence/video-pipe1.gif)



Laminar flow in a pipe

[www.wolfdynamics.com/training/turbulence/video-pipe2.gif](http://www.wolfdynamics.com/training/turbulence/video-pipe2.gif)

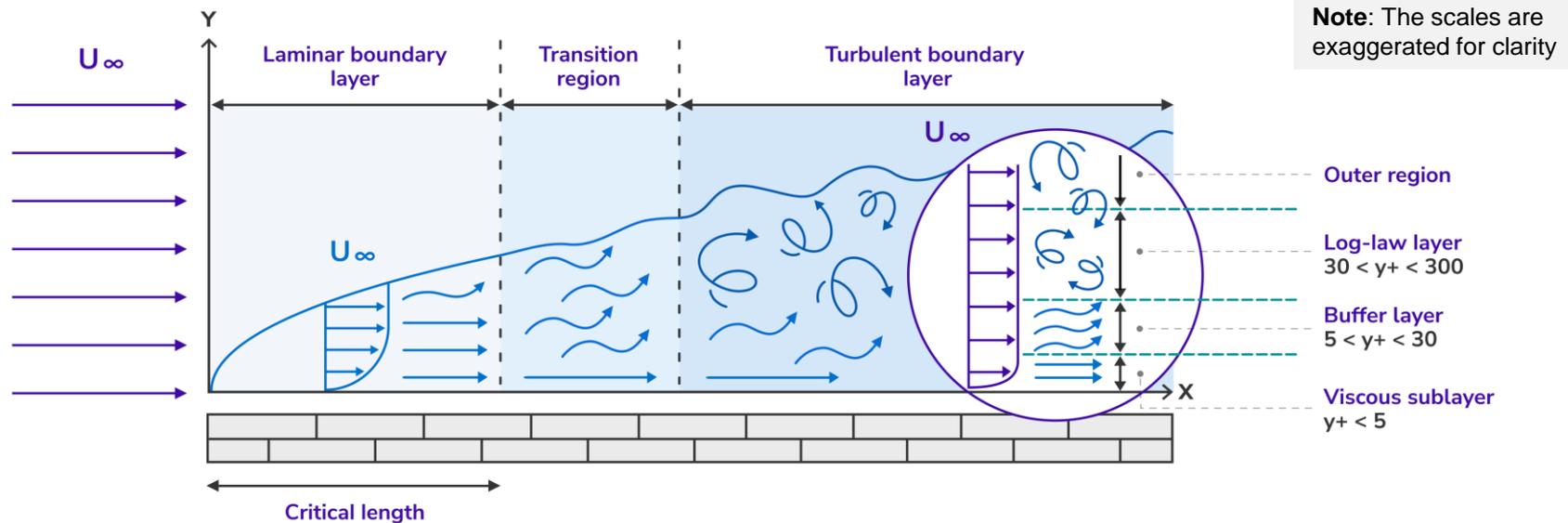
**Video credit:** <https://gfm.aps.org/meetings/dfd-2017/59997842b8ac316d3884197e>

**DOI:** <https://doi.org/10.1103/APS.DFD.2017.GFM.V0013>

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## Turbulence modeling – Boundary layer

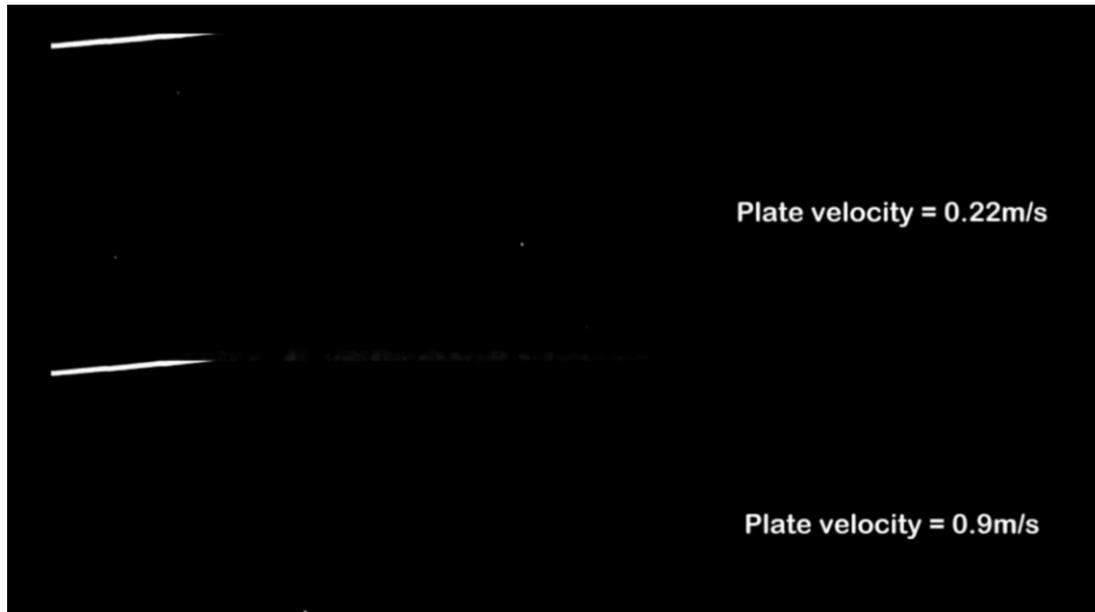


### Boundary layer (Laminar-Transitional-Turbulent flow)

- In this case, a laminar boundary layer starts to form at the leading edge.
- As the flow proceeds further downstream, large shear stresses and velocity gradient develop within the boundary layer. At one point the flow becomes turbulent.
- The turbulent motion increases the mixing and the boundary layer mixing.
- What is happening in the transition region is not well understood. The flow can become laminar again or can become turbulent.
- As for the pipe flow, the velocity profiles in the laminar and turbulent regions are different.

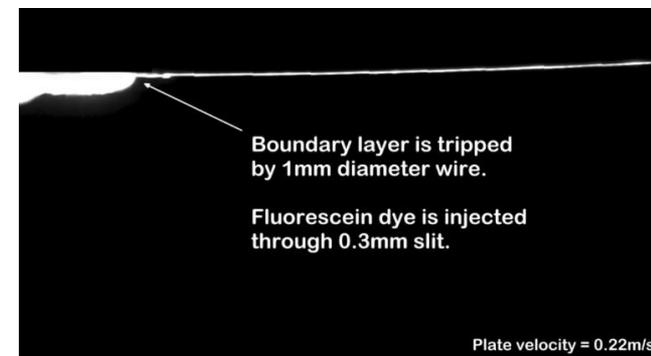
# Introduction to turbulence modeling – Basic concepts

## Turbulence modeling – Boundary layer and fluctuations of transported quantities



Turbulent boundary layer on a flat plate

[www.wolfdynamics.com/training/turbulence/video-bl1.mp4](http://www.wolfdynamics.com/training/turbulence/video-bl1.mp4)



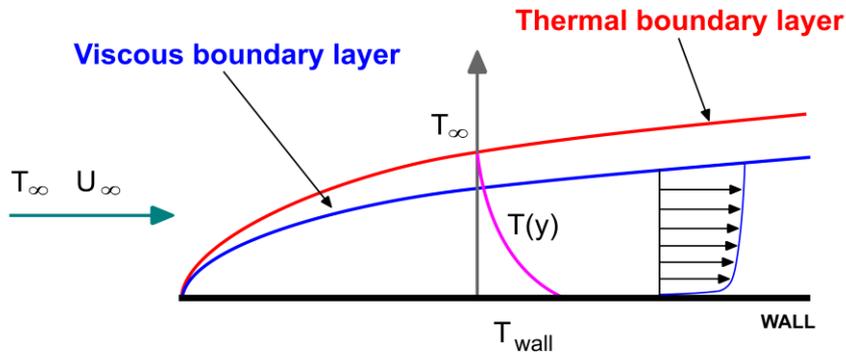
**Video credit:** <https://www.youtube.com/watch?v=e1TbkLIDWys>

**arXiv:** <https://arxiv.org/abs/1210.3881>

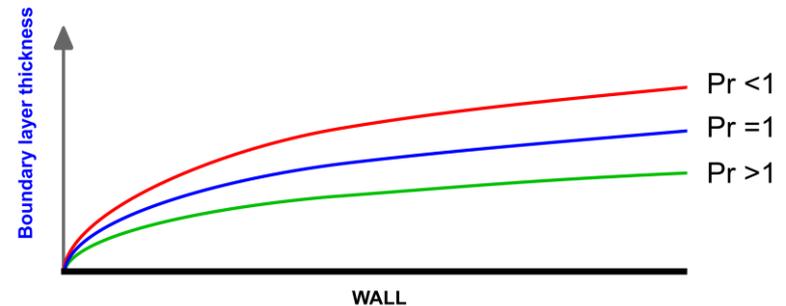
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## Turbulence modeling – Thermal boundary layer



Thermal boundary layer vs. Viscous boundary layer  
Forced convection

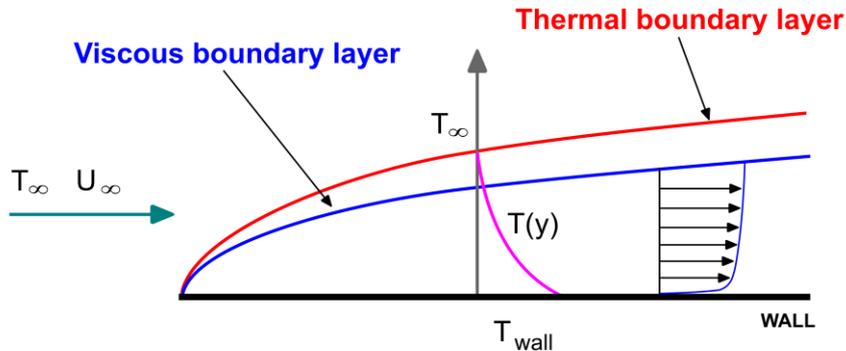


Thermal boundary layer in function of Prandtl number (Pr)

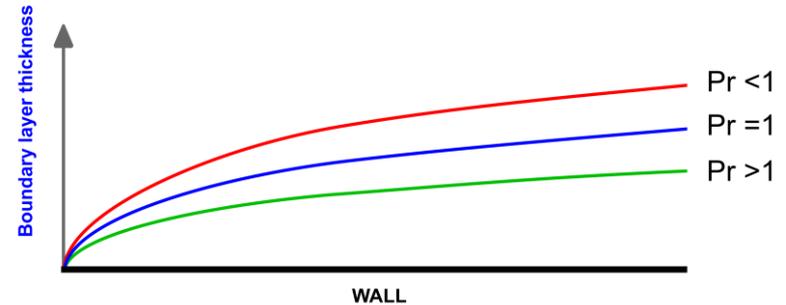
### Momentum and thermal boundary layer

- Just as there is a viscous boundary layer in the velocity distribution (or momentum), there is also a thermal boundary layer.
- Thermal boundary layer thickness is different from the thickness of the viscous sublayer (momentum), and is fluid dependent.
- The thickness of the thermal sublayer for a high Prandtl number fluid (e.g., water) is much less than the momentum sublayer thickness.

## Turbulence modeling – Thermal boundary layer



Thermal boundary layer vs. Viscous boundary layer  
Forced convection

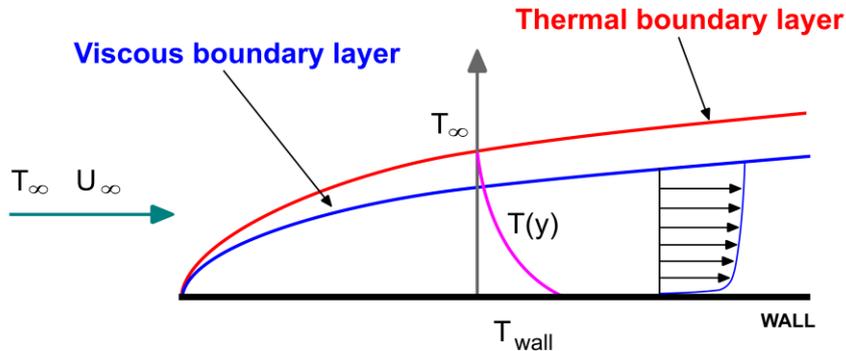


Thermal boundary layer in function of Prandtl number (Pr)

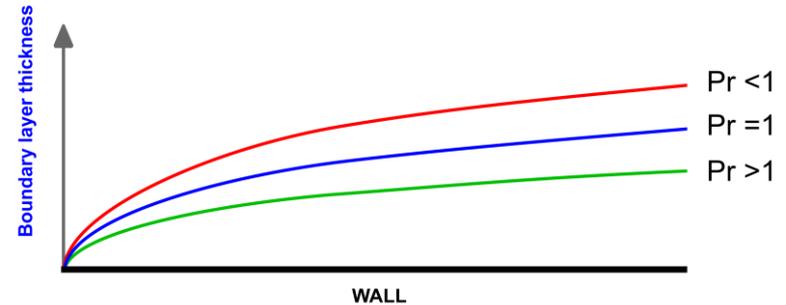
### Momentum and thermal boundary layer

- For fluids of low Prandtl numbers (e.g., air), the thermal sublayer is much larger than the momentum sublayer thickness.
- For Prandtl number equal 1, the thermal boundary layer is equal to the momentum boundary layer.
- Note that the thickness of the thermal sublayer for a high Prandtl number fluid (e.g., water) is much less than the momentum sublayer thickness.
- Therefore, the mesh requirements close to the walls need to be corrected for the thinner thermal boundary layer.

## Turbulence modeling – Thermal boundary layer



Thermal boundary layer vs. Viscous boundary layer  
Forced convection



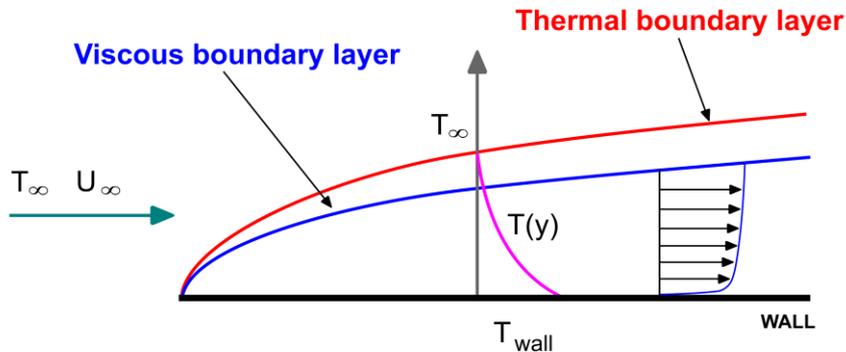
Thermal boundary layer in function of Prandtl number (Pr)

### Momentum and thermal boundary layer

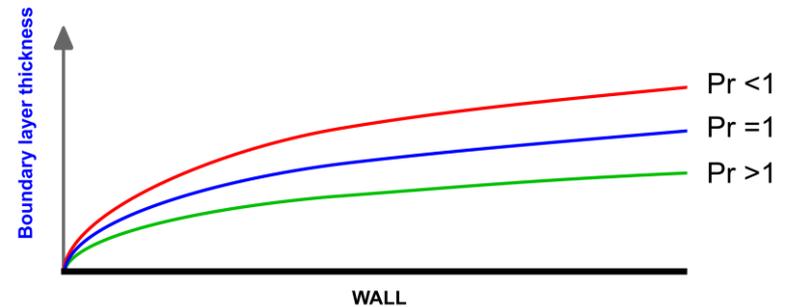
- Using the following relationships, the  $y^+$  value, and therefore the distance from to wall to the first mesh node normal to the wall, can be corrected as follows,

$$\frac{\delta_{\text{hydrodynamic b.l.}}}{\delta_{\text{thermal b.l.}}} \approx \frac{y_{\text{viscous s.l.}}}{y_{\text{thermal s.l.}}} \approx \sqrt{Pr} \quad \text{therefore} \quad y^+ \approx \frac{1}{\sqrt{Pr}}$$

## Turbulence modeling – Thermal boundary layer



Thermal boundary layer vs. Viscous boundary layer  
Forced convection



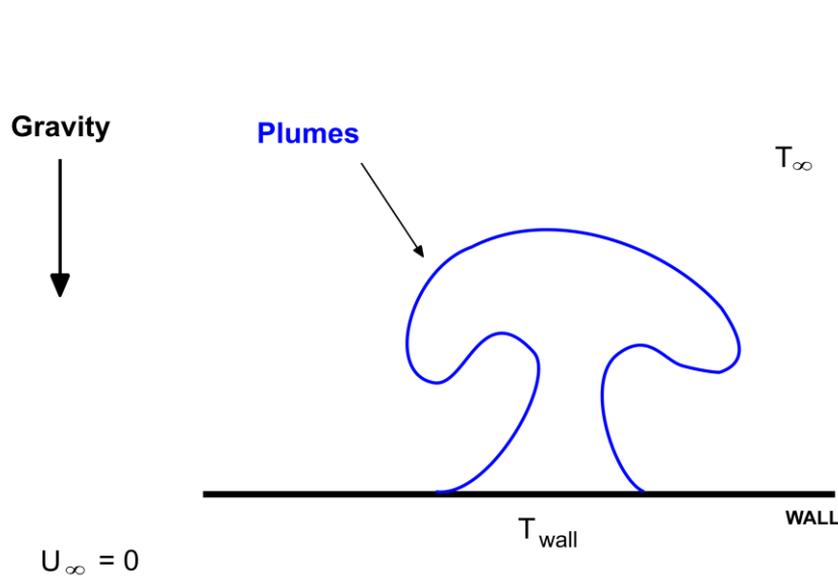
Thermal boundary layer in function of Prandtl number (Pr)

### Momentum and thermal boundary layer

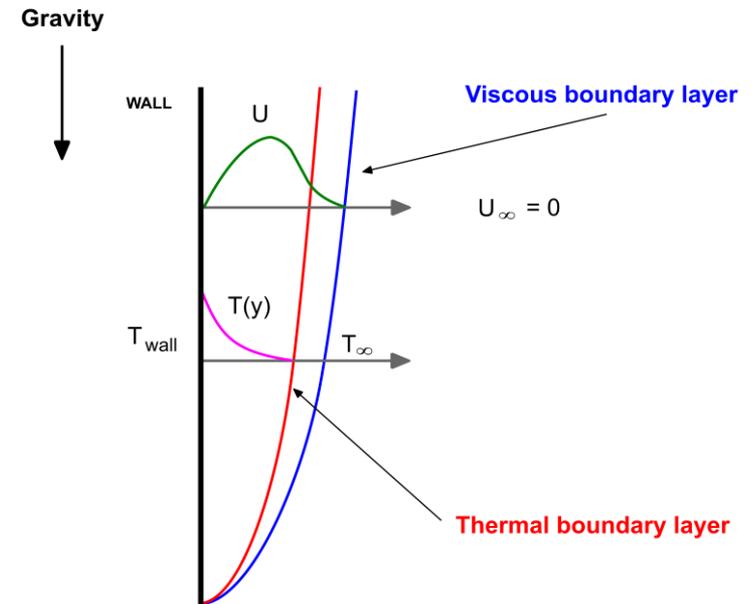
- A similar situation exists when working with multispecies transport and using the Schmidt number (Sc).
- If the Schmidt number is considerably larger than unity, then the thickness of the thermal diffusion sublayer is much less than the momentum sublayer thickness.
- Using the Schmidt number, the  $y^+$  value, and therefore the distance from to wall to the first mesh node normal to the wall, can be corrected as follows,

$$y^+ \approx \frac{1}{\sqrt[3]{Sc}}$$

## Turbulence modeling – Thermal boundary layer



Horizontal heated plate immersed in a quiescent fluid.  
Natural convection



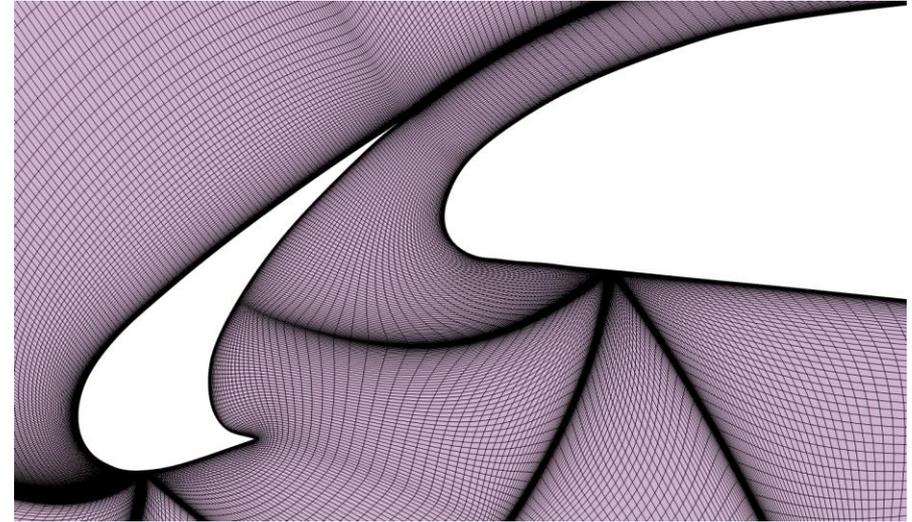
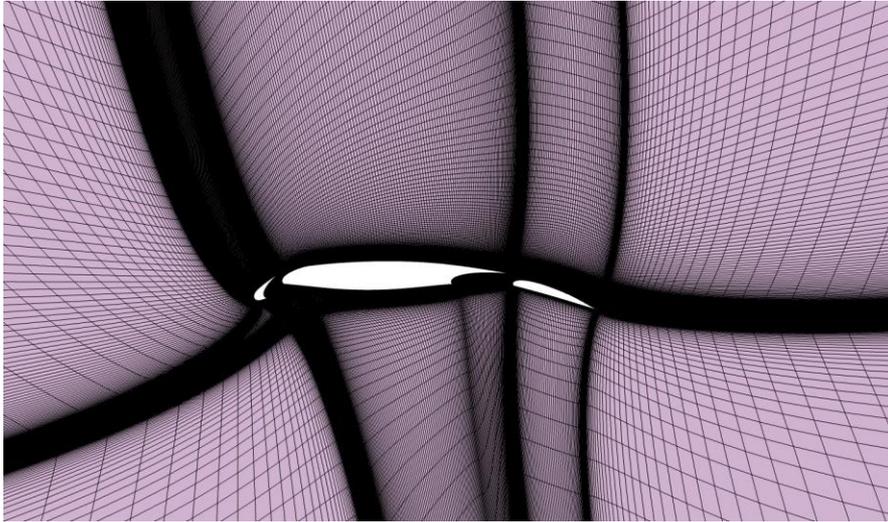
Vertical heated plate immersed in a quiescent fluid.  
Natural convection.

### Natural convection in a heated plate

- As the fluid is warmed by the plate, its density decreases, and a buoyant force arises which induces flow motion in the vertical or horizontal direction.
- The force is proportional to  $(\rho - \rho_{\infty}) \times g$ , therefore gravity must be considered.

# Introduction to turbulence modeling – Basic concepts

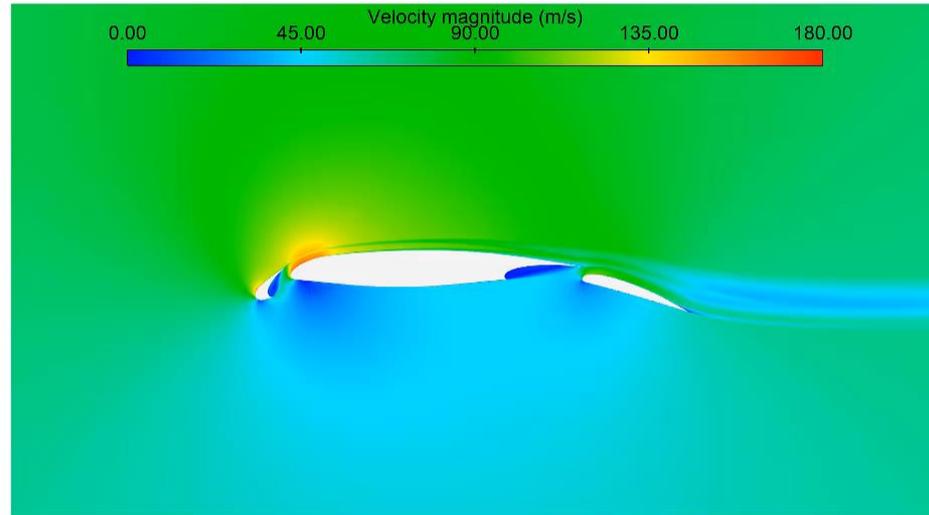
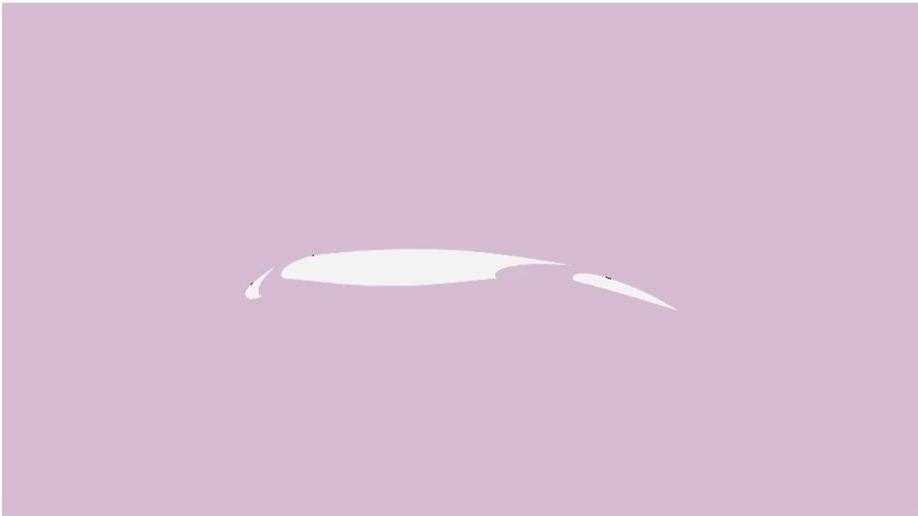
## Turbulence modeling – Laminar separation bubbles and transition to turbulence



- Maybe, the most challenging topic of turbulence modeling is the prediction of transition to turbulence.
- Trying to predict transition to turbulence in CFD requires very fine meshes and well calibrated models.
- Many traditional turbulence models assume that the boundary layer is turbulent in all its extension.
- But assuming that the boundary layer is entirely turbulent might not be a good assumption, as in some regions the boundary layer might still be laminar, so we may be overpredicting drag forces or predicting wrong separation points.
- In many applications, transition to turbulence is preceded by laminar separation bubbles (LSB), which are laminar recirculation areas that separate from the wall and reattach in a very short distance and are very sensitive to disturbances.
- After the LSB, the flow becomes turbulent.

# Introduction to turbulence modeling – Basic concepts

## Turbulence modeling – Laminar separation bubbles and transition to turbulence

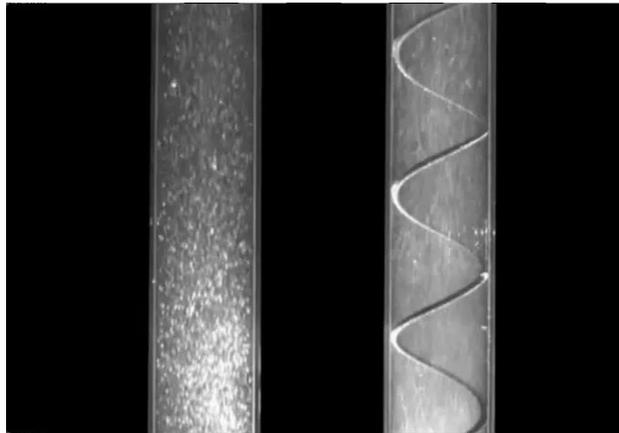


Laminar separation bubbles

<http://www.wolfdynamics.com/images/airfoil.mp4>

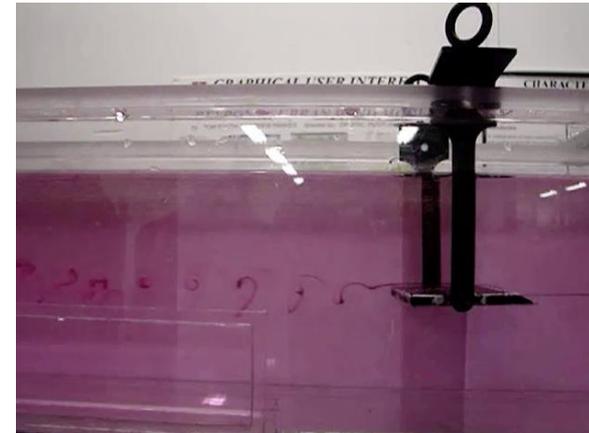
# Introduction to turbulence modeling – Basic concepts

## Turbulence flows videos



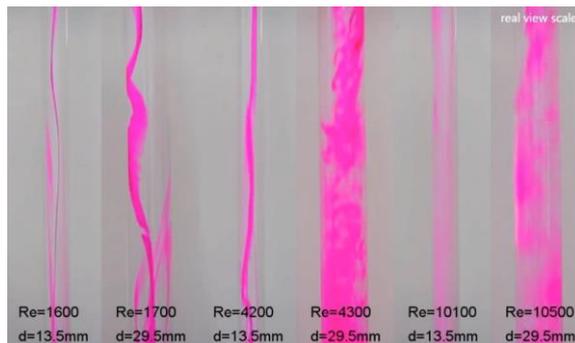
Laminar-Turbulent flow in a pipe  
Smooth vs corrugated tube

<https://www.youtube.com/watch?v=WG-YCpAGgQQ>



Flow over a flat plate  
Attached and separated boundary layer

[https://www.youtube.com/watch?v=zsO5BQA\\_CZk](https://www.youtube.com/watch?v=zsO5BQA_CZk)



Reynolds' dye experiment

Various types of flow - Laminar-Transitional-Turbulent

<https://www.youtube.com/watch?v=ontHCul6eB4>



Laminar-Turbulent vortex shedding

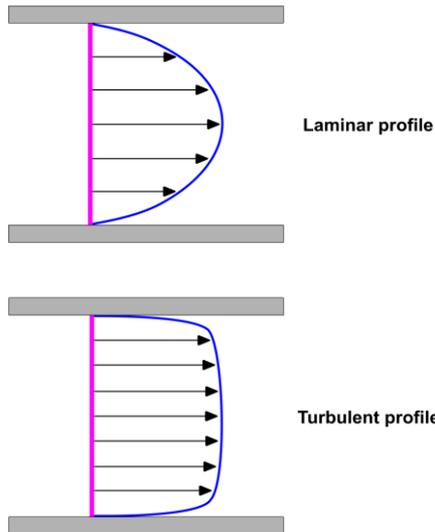
<https://www.youtube.com/watch?v=Jl0M1gVnhbw>

# Roadmap to Lecture 2

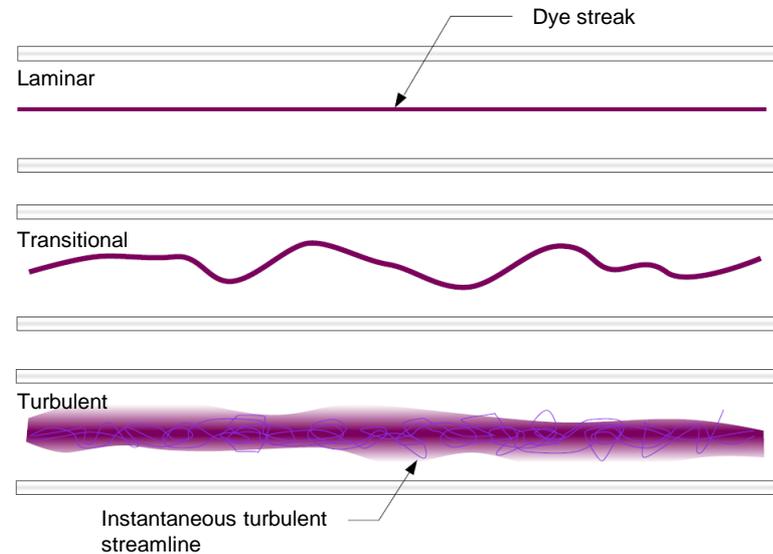
- ~~1. The turbulent world around us~~
- ~~2. Turbulence, does it matter?~~
- ~~3. Introduction to turbulence modeling – Basic concepts~~
- 4. Wall bounded flows and shear flows**
- ~~5. A peek to the turbulence closure problem, some correlations in turbulence modeling, and the energy cascade~~

# Wall bounded flows and shear flows

## Wall bounded and shear free flows



Wall bounded turbulence

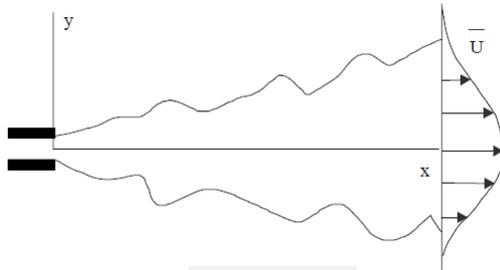


Shear free turbulence

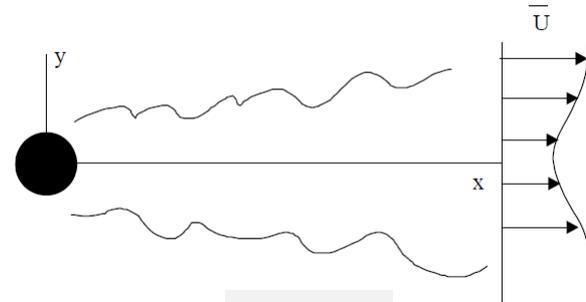
- Flows (laminar or turbulent), can originate at the walls. When this is the case, we talk about wall bounded turbulence (boundary layers).
- They can also originate in the absence of walls (not bounded to walls), or far from walls. When this is the case, we talk about shear free turbulence (jets, har wakes, mixing layers, thermal plumes, atmospheric flows).

# Wall bounded flows and shear flows

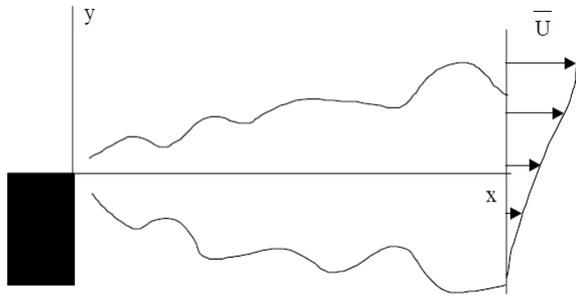
## Shear free flows samples



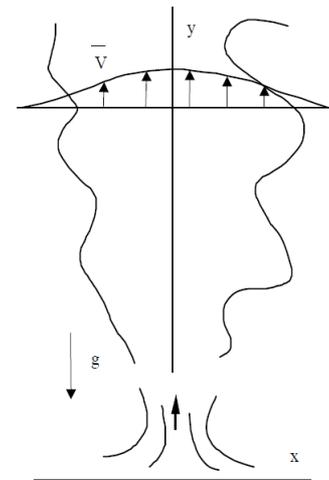
Jet



Far wake



Mixing layer

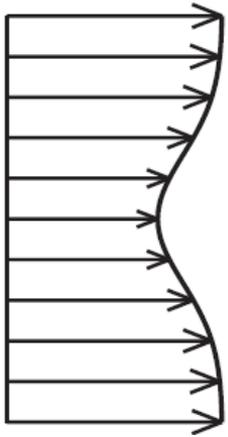


Thermal plume

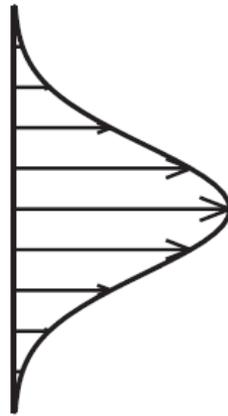
# Wall bounded flows and shear flows

## Shear free flows samples

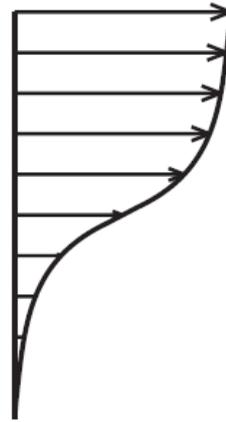
Different velocity profiles of shear free flows



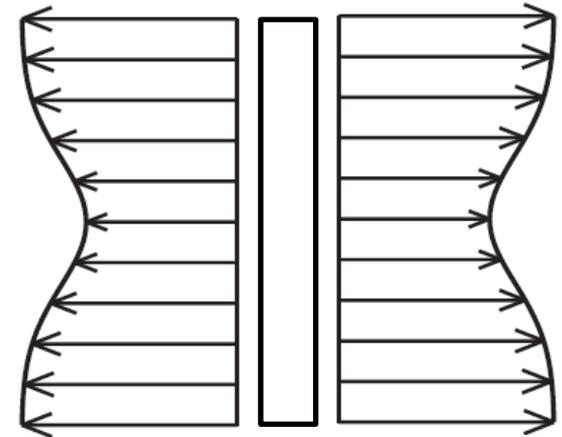
Wake



Plane Jet



Mixing layer

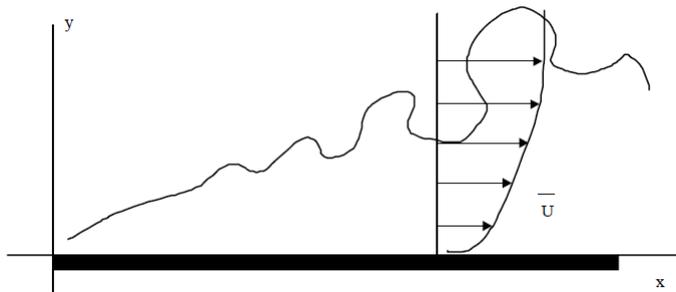


Radial jet

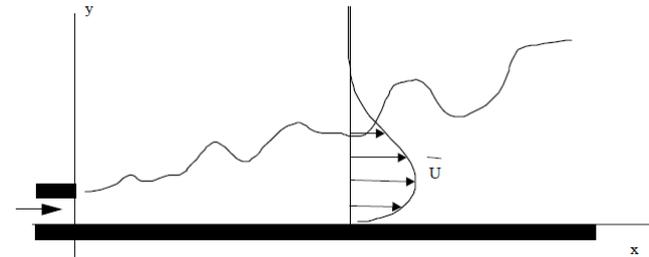
- Under certain conditions, many of these flows have analytical solutions.
- Therefore, turbulence models can be calibrated or validated using these solutions.
- Sample of analytical solutions (self-similarity solutions):
  - Far wake (Schlichting-Gersten, 2017)
  - Mixing layer (Liepmann and Laufer, 1947)
  - Plane jet (Witze and Dwyer, 1976).

# Wall bounded flows and shear flows

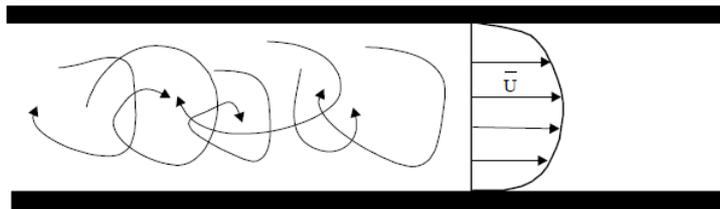
## Wall bounded flows samples



Turbulent boundary layer on a flat plate



Turbulent wall jet

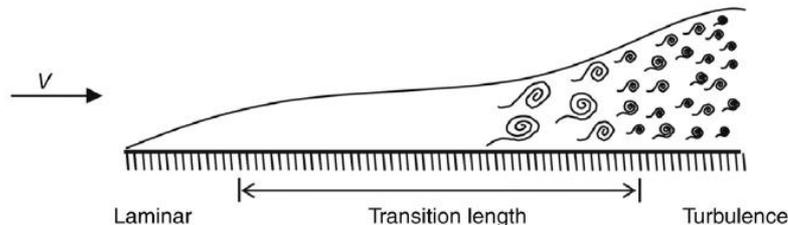
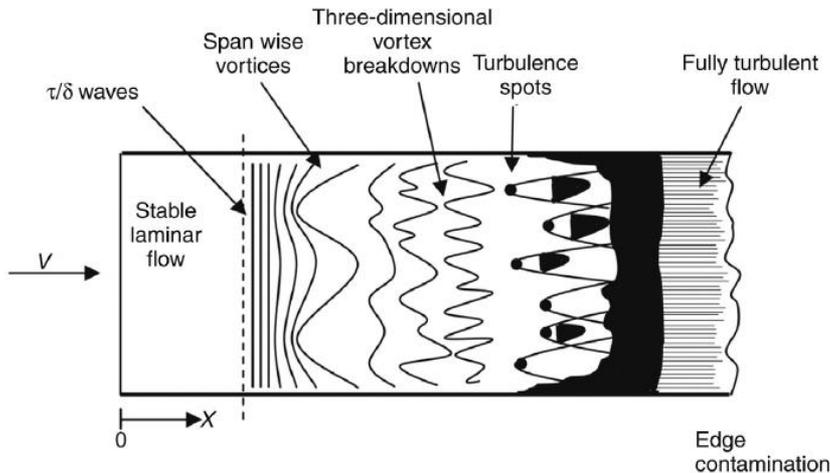


Turbulent flow in a channel or pipe

- Walls can be heated, which adds buoyancy and thermal diffusivity to the physics.
- Walls can also be rough, which will affect the boundary layer.
- Do you think in something else?

# Wall bounded flows and shear flows

## Wall bounded flows samples

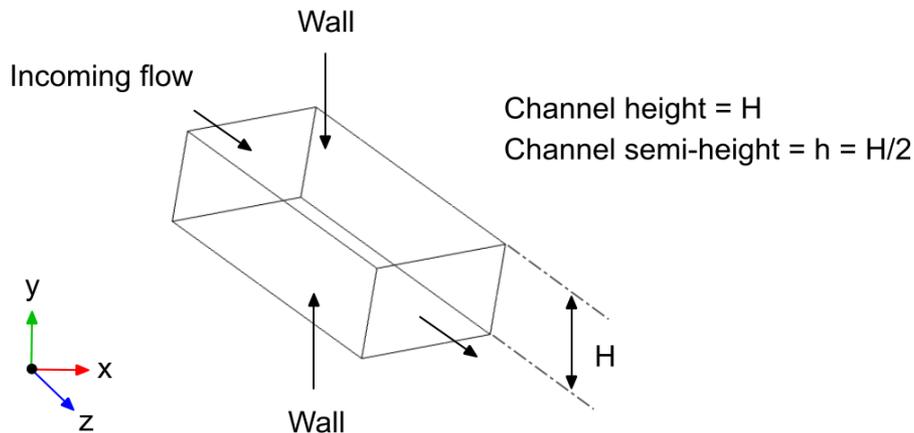


- In these cases, the no-slip boundary condition must be enforced at the walls, and we expect to find a boundary layer similar to the one depicted in the figure.
- The transition to turbulence can follow three different paths:
  - Natural.
  - Bypass.
  - Forced.
- Under certain conditions, these flows have analytical solutions.
- Therefore, turbulence models can be calibrated or validated using these solutions.
- Sample of analytical solutions:
  - Channel flows (Pope, 2000).
  - Boundary layers (Prandtl, 1925; Bradshaw et al. 1995; Pope, 2000).
  - Couette flow (Schlichting-Gersten, 2017)

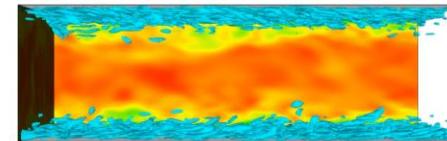
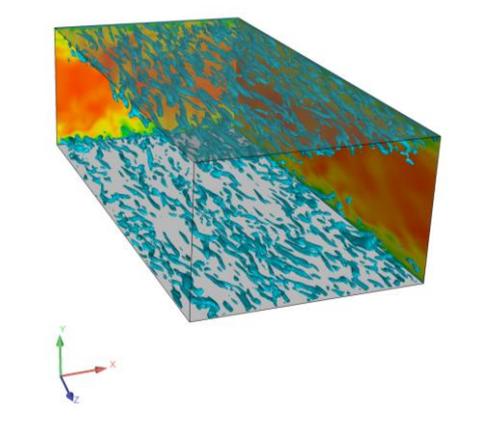
# Wall bounded flows and shear flows

## Wall bounded flow – Channel flow

- You will find many research on the channel flow as it has an analytical solution under very specific conditions.



Periodic boundary conditions in the streamwise direction ( $x$ ) and spanwise direction ( $z$ )



# Wall bounded flows and shear flows

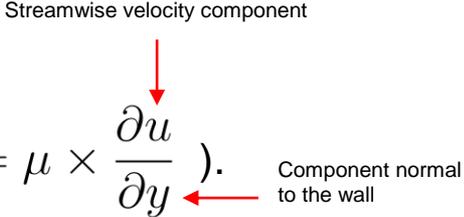
## Wall bounded flow – Channel flow

- The channel flow is usually characterized using the  $Re_\tau$ , which is defined as follows,

$$Re_\tau = \frac{U_\tau \times h}{\nu} \quad Re \approx 20 \times Re_\tau$$

- Where  $h$  is the channel semi-height,  $\nu$  is the kinematic viscosity, and  $U_\tau$  is the shear velocity and is defined as follows,

$$U_\tau = \left( \frac{\tau_{wall}}{\rho} \right)^{0.5}$$

- In the previous equation,  $\tau_{wall}$  is the shear stress at the wall ( $\tau_{wall} = \mu \times \frac{\partial u}{\partial y}$ ). 
- With these conditions and according to the theory of equilibrium for channels, the equilibrium between the imposed pressure drop and the wall shear stresses is given by,

$$\frac{\partial P}{\partial x} h = -\tau_{wall}$$

- At this point, we only need to set a pressure drop.

# Wall bounded flows and shear flows

## Wall bounded flow – Channel flow

- The following DNS simulation was conducted at a  $Re_\tau$  equal to,

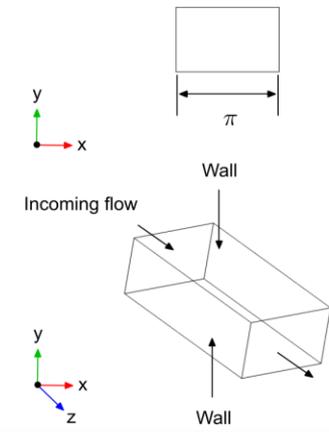
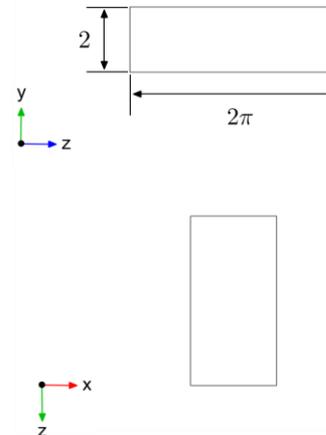
$$Re_\tau = \frac{U_\tau \times h}{\nu} = 590$$

- With the following parameters,

$$\rho = 1 \frac{kg}{m^3}$$

$$\mu = 0.001695 \frac{kg}{m \cdot s}$$

$$h = 1 \text{ m}$$



Periodic boundary conditions in the streamwise direction (x) and spanwise direction (z)

- Where  $h$  is the channel semi-height.
- Notice that this is an incompressible flow.

# Wall bounded flows and shear flows

## Wall bounded flow – Channel flow

- Periodic boundary conditions in the streamwise (z) and spanwise (x) directions were used.
- The top and bottom walls are no-slip walls.
- To onset the fluid flow we imposed a pressure drop equal to 1 Pa, such as,

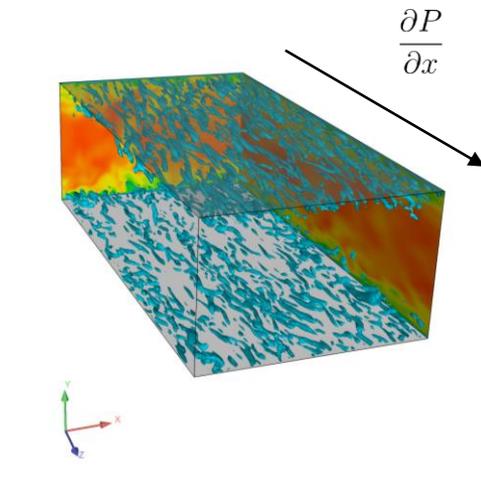
$$\frac{\partial P}{\partial x} = -1 \frac{Pa}{m}$$

- Therefore, the shear stresses at the wall are equal to,

$$\tau_{wall} = 1 Pa$$

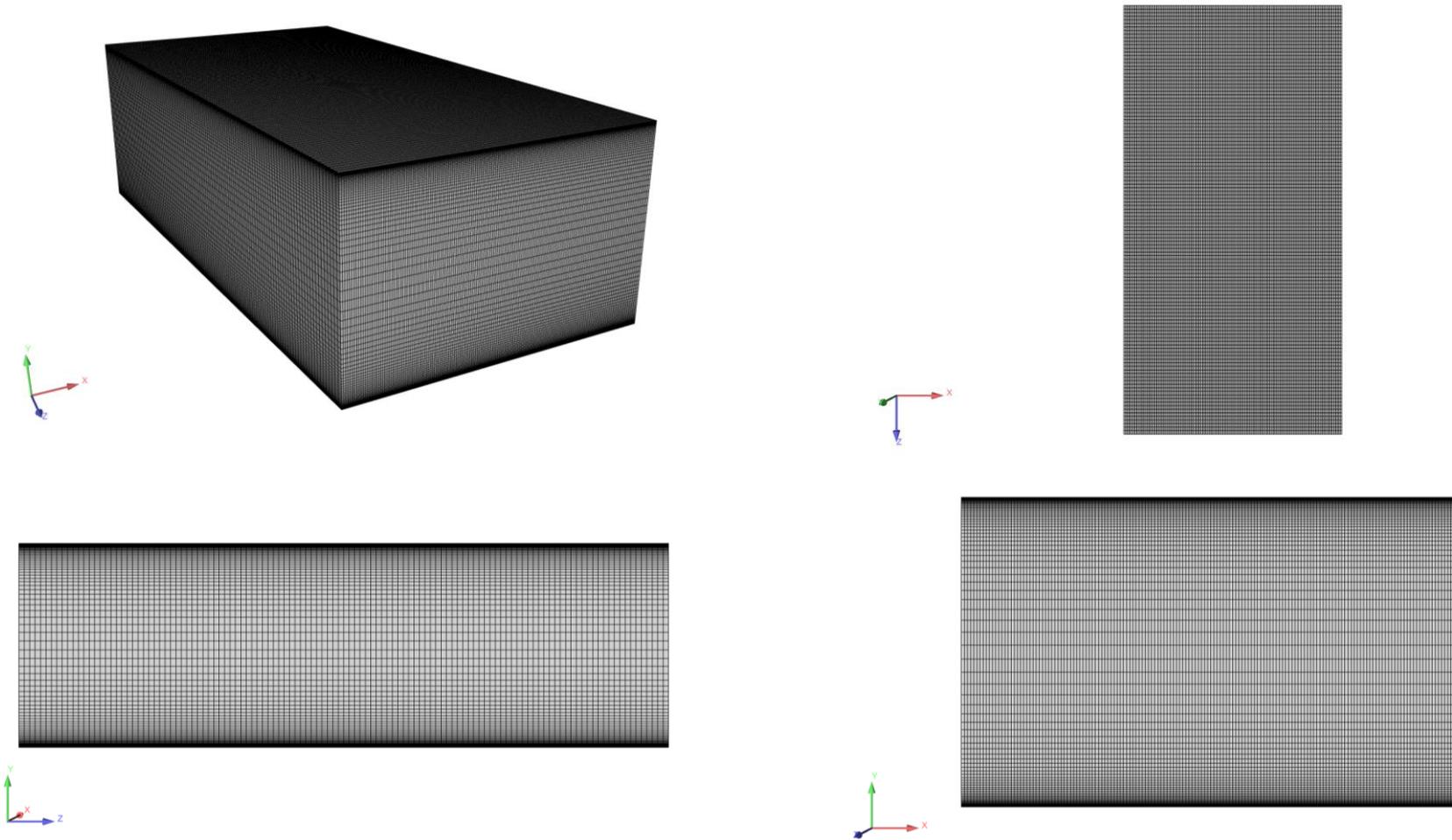
- Finally, the shear velocity is equal to,

$$U_{\tau} = \left( \frac{\tau_{wall}}{\rho} \right)^{0.5} = 1 \frac{m}{s}$$



# Wall bounded flows and shear flows

## Wall bounded flow – Channel flow

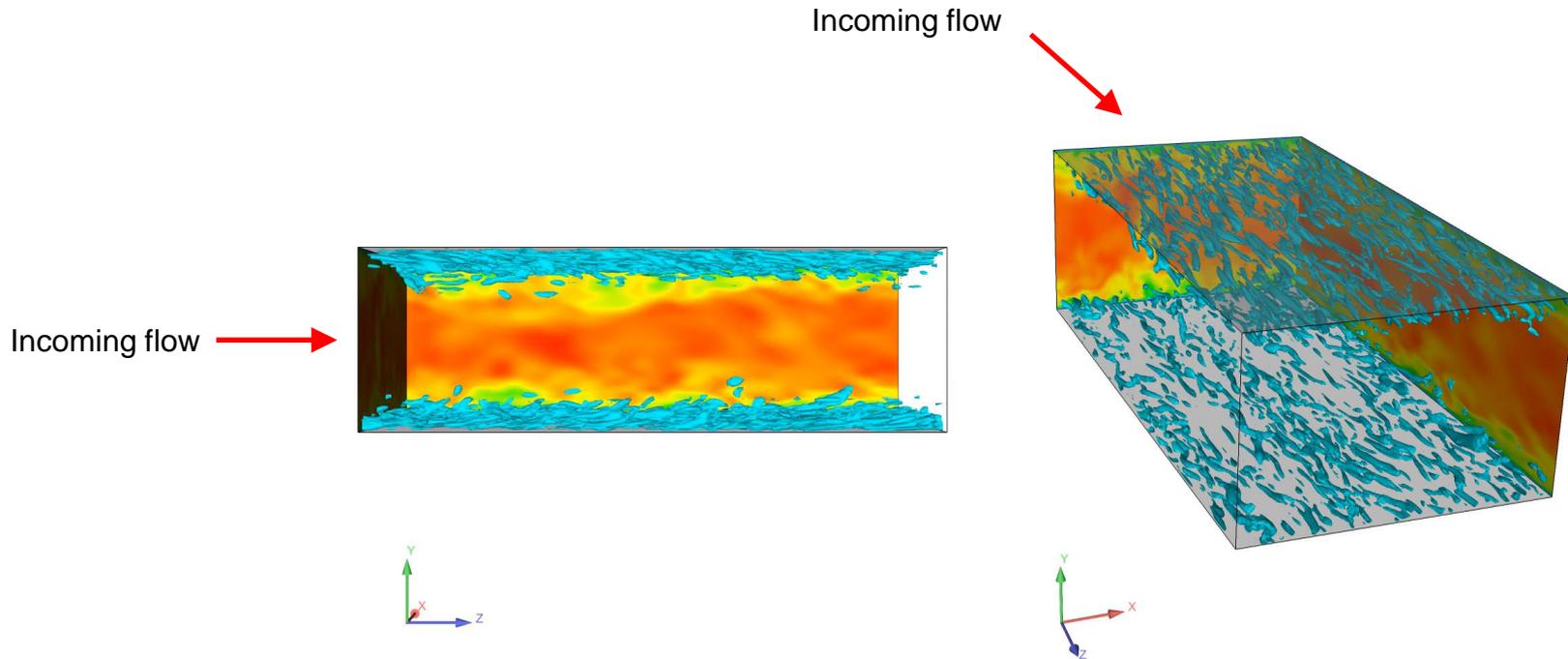


Mesh

Orthogonal hexahedral mesh – Approximately 1.8 million elements

# Wall bounded flows and shear flows

## Wall bounded flow – Channel flow

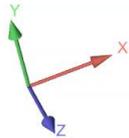
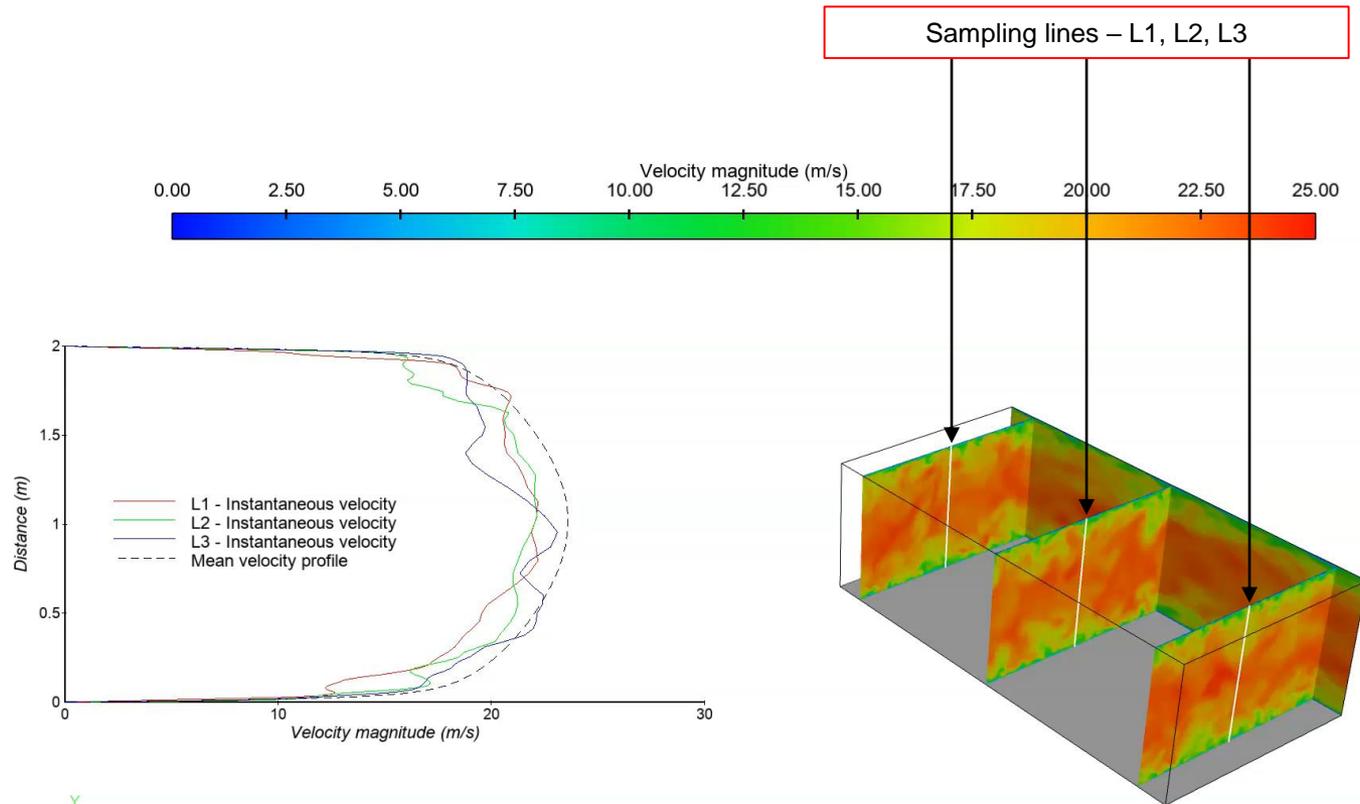


Wall bounded flow – Channel flow

<http://www.wolfdynamics.com/training/turbulence/channel1.mp4>

# Wall bounded flows and shear flows

## Wall bounded flow – Channel flow

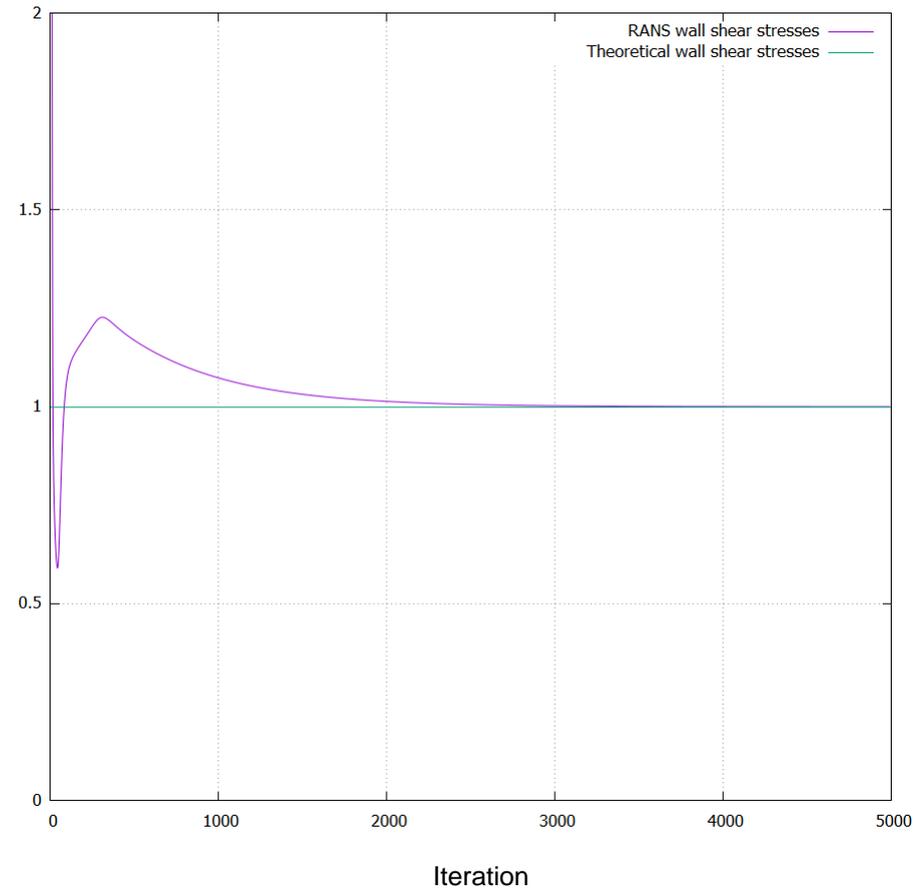
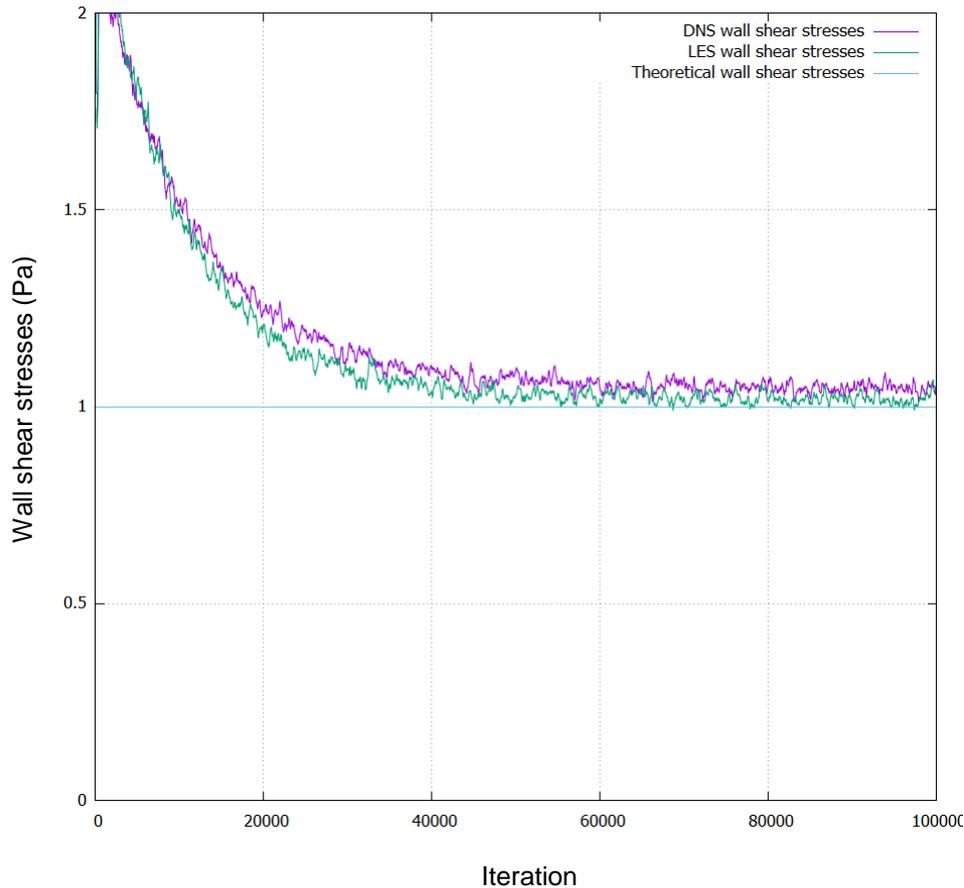


Wall bounded flow – Channel flow

<http://www.wolfdynamics.com/training/turbulence/channel2.mp4>

# Wall bounded flows and shear flows

## Wall bounded flow – Channel flow



- The DNS both took approximately 150 hours on 8 cores ( $CFL < 1$ ).
- The RANS simulation took approximately 1 hour on 1 core.

# Wall bounded flows and shear flows

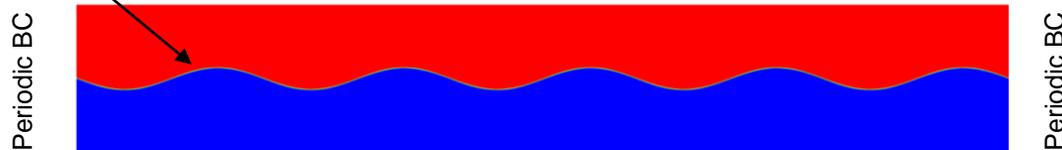
## Shear free flow – Kelvin-Helmholtz instability



### Kelvin Helmholtz Clouds

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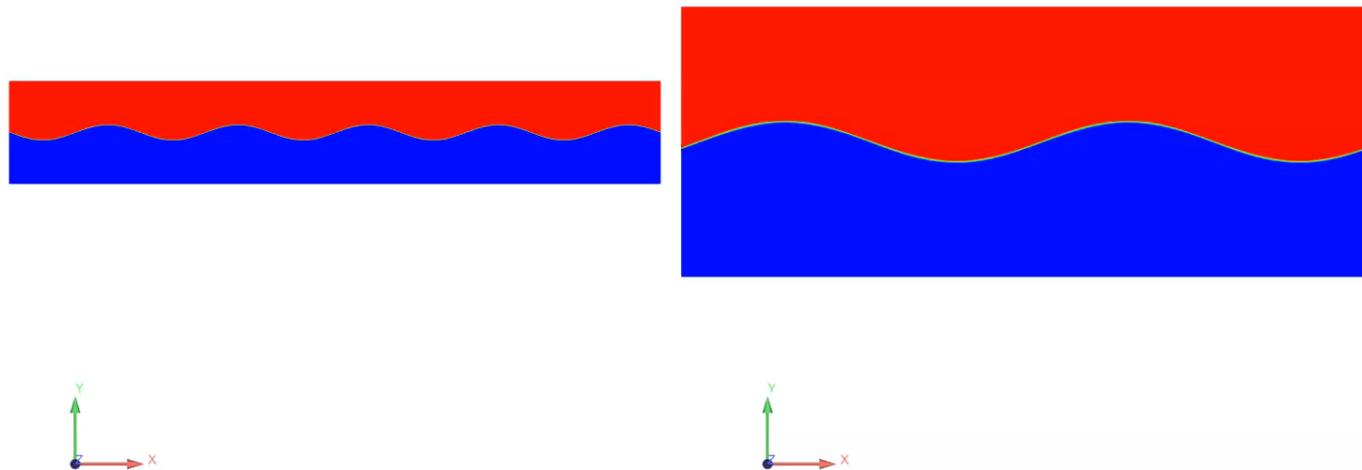
Velocity perturbation



Initialization for the numerical simulation

# Wall bounded flows and shear flows

## Shear free flow – Kelvin-Helmholtz instability

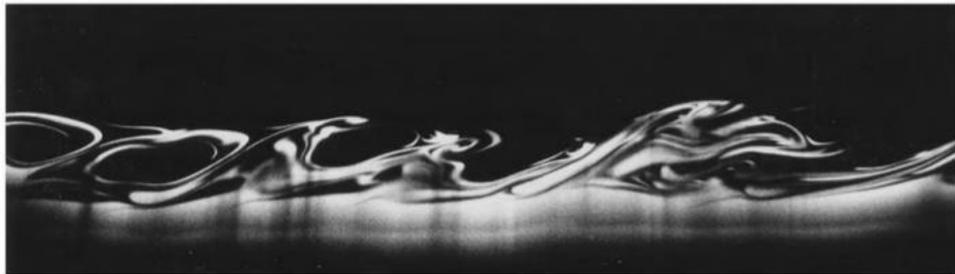
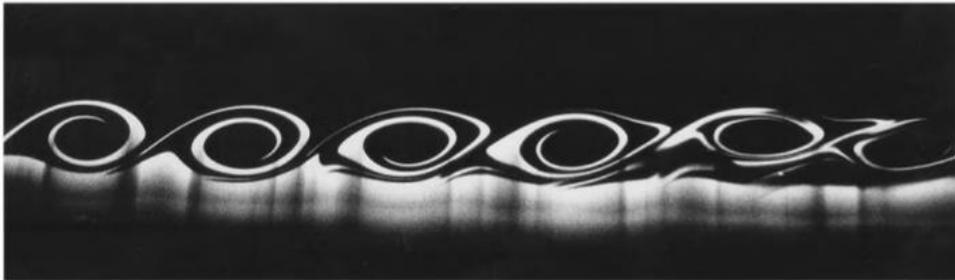
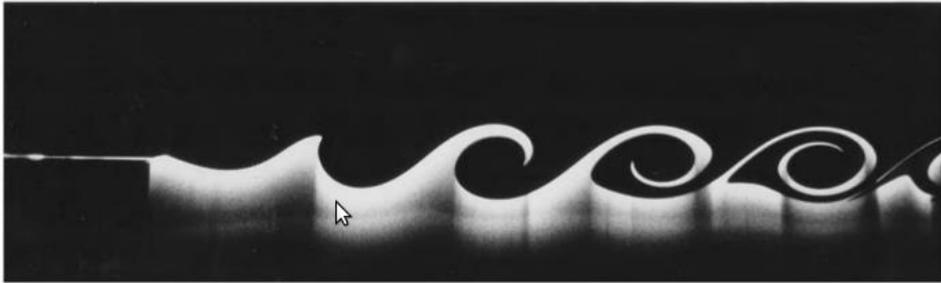


Numerical simulation of the Kelvin-Helmholtz instability

[www.wolfdynamics.com/training/turbulence/KH.mp4](http://www.wolfdynamics.com/training/turbulence/KH.mp4)

# Wall bounded flows and shear flows

## Shear free flow – Kelvin-Helmholtz instability

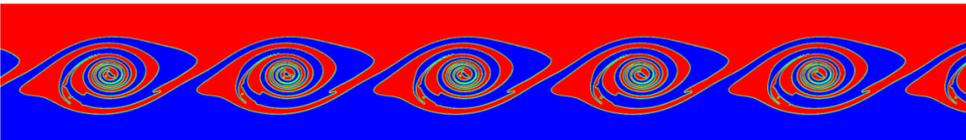


### Development of a Kelvin-Helmholtz instability in the laboratory.

The upper and faster moving layer is slightly less dense than the lower layer. At first, waves form and overturn in a two-dimensional fashion but, eventually, three-dimensional motions appear that lead to turbulence and complete mixing.

B. Cushman-Roisin, J. Beckers, Introduction to Geophysical Fluid Dynamics - Physical and Numerical Aspects (Academic Press, 2009), 393-401.

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Outcome of the numerical simulation for similar conditions

# Roadmap to Lecture 2

- ~~1. The turbulent world around us~~
- ~~2. Turbulence, does it matter?~~
- ~~3. Introduction to turbulence modeling – Basic concepts~~
- ~~4. Wall bounded flows and shear flows~~
- 5. A peek to the turbulence closure problem, some correlations in turbulence modeling, and the energy cascade**

## Turbulence modeling – Starting equations

- For an incompressible flow, the exact Navier-Stokes equations (NSE) are written as follows,

$$\nabla \cdot (\mathbf{u}) = 0$$
$$\frac{\partial \mathbf{u}}{\partial t} + \nabla \cdot (\mathbf{u}\mathbf{u}) = \frac{-\nabla p}{\rho} + \nu \nabla^2 \mathbf{u}$$

- These equations are valid for laminar and turbulent flows.
- However, as we will see later, using the exact NSE to tackle a turbulent flow, is too expensive from the computational point of view.
- Therefore, the need of using turbulence models to reduce the computational cost, and at the same time, getting physically realistic results.
- By the way, when we solve the exact NSE we are doing what is called direct numerical simulations (DNS).

# A peek to the turbulence closure problem and some correlations

## Turbulence modeling – Governing equations

- Let us introduce the incompressible Reynolds-averaged Navier-stokes equations (RANS) used in turbulence modeling.

If we retain this term, we talk about URANS equations and if we drop it, we talk about RANS equations

Reynolds stress tensor  
This term requires modeling

$$\nabla \cdot (\bar{\mathbf{u}}) = 0$$
$$\frac{\partial \bar{\mathbf{u}}}{\partial t} + \nabla \cdot (\bar{\mathbf{u}}\bar{\mathbf{u}}) = \frac{-\nabla \bar{p}}{\rho} + \nu \nabla^2 \bar{\mathbf{u}} - \frac{1}{\rho} \nabla \cdot \tau^R$$

- These equations are known as the exact RANS equations.
- The differences between the exact NSE and the exact RANS equations are the overbar on top of the primitive variables and the extra term  $\tau^R$ .
- The overbar over the primitive variables in the RANS equations means that the quantities have been averaged to remove the fluctuations.
- We will talk more about these equations later.

## Turbulence modeling – Governing equations

- Our goal, at this point, is to model somehow the Reynolds stress tensor,

$$\tau^R = -\rho (\overline{\mathbf{u}'\mathbf{u}'}) = - \begin{pmatrix} \overline{\rho u' u'} & \overline{\rho u' v'} & \overline{\rho u' w'} \\ \overline{\rho v' u'} & \overline{\rho v' v'} & \overline{\rho v' w'} \\ \overline{\rho w' u'} & \overline{\rho w' v'} & \overline{\rho w' w'} \end{pmatrix}$$

- The Reynolds stress tensor basically correlates the velocity fluctuations.
- In CFD we do not want to resolve these velocity fluctuations, as it requires very fine meshes and very small time-steps.
- The RANS/URANS approach to turbulence modeling requires the Reynolds stresses to be appropriately modeled. For example, by using the Boussinesq hypothesis.
- The rest of the terms appearing in the governing equations, can be computed from the mean flow.

# A peek to the turbulence closure problem and some correlations

## Turbulence modeling – Governing equations

- By using the Boussinesq hypothesis (we will talk about this later), we can write down the solvable RANS equations starting from the exact RANS equations,

$$\nabla \cdot (\bar{\mathbf{u}}) = 0$$
$$\frac{\partial \bar{\mathbf{u}}}{\partial t} + \nabla \cdot (\bar{\mathbf{u}}\bar{\mathbf{u}}) = -\frac{1}{\rho} \left( \nabla \bar{p} + \frac{2}{3} \rho \nabla k \right) + \nabla \cdot \left[ \frac{1}{\rho} (\mu + \mu_t) \nabla \bar{\mathbf{u}} \right]$$

Effective viscosity

Turbulent viscosity

Normal stresses arising from the Boussinesq approximation

- The problem now reduces to computing the turbulent eddy viscosity  $\mu_T$  in the momentum equation.
- The turbulence eddy viscosity is an artificial quantity (non-physical) derived from the turbulence model.
- This is the closure problem in turbulence modeling.

# A peek to the turbulence closure problem and some correlations

## Turbulence modeling – Governing equations

- The turbulent eddy viscosity can be computed using turbulence models.
- There are many models, each having different requirements and limitations. We will talk more about models later.
- For example, we can compute the turbulent eddy viscosity using the  $k - \omega$  turbulence model\*, which reads as follows,

$$\begin{aligned} \nabla_t k + \nabla \cdot (\bar{\mathbf{u}}k) &= \tau^R : \nabla \bar{\mathbf{u}} - \beta^* k \omega + \nabla \cdot [(\nu + \sigma^* \nu_t) \nabla k] \\ \nabla_t \omega + \nabla \cdot (\bar{\mathbf{u}}\omega) &= \alpha \frac{\omega}{k} \tau^R : \nabla \bar{\mathbf{u}} - \beta \omega^2 + \nabla \cdot [(\nu + \sigma \nu_t) \nabla \omega] \end{aligned}$$

The diagram illustrates the constant coefficients in the  $k - \omega$  turbulence model equations. Red arrows point from 'Constant' boxes to the coefficients  $\alpha \frac{\omega}{k}$ ,  $\beta^*$ , and  $\sigma^*$  in the first equation, and  $\alpha$ ,  $\beta$ , and  $\sigma$  in the second equation.

- We will elaborate more on the closure constants (or coefficients) later.

\*The equations correspond to the k-w 1988 version by Wilcox.

[1] D. C. Wilcox. Reassessment of the Scale-Determining Equation for Advanced Turbulence Models. AIAA Journal, 1988.

[2] D. C. Wilcox. Turbulence Modeling for CFD. DCW Industries, 2010.

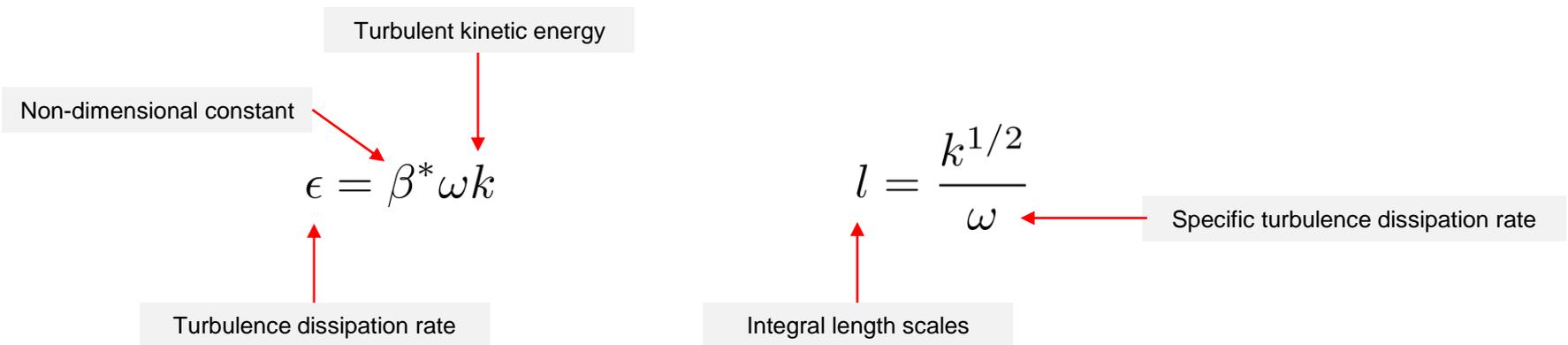
# A peek to the turbulence closure problem and some correlations

## Turbulence modeling – Governing equations

- In the  $k - \omega$  turbulence model, the turbulent eddy viscosity is computed as follows,

$$\nu_t = \frac{k}{\omega}$$

- The turbulent eddy viscosity is not a physical property. It has been introduced to take into account the increased mixing and shear stresses due to the turbulence.
- The following auxiliary relationships are also used in the  $k - \omega$  turbulence model,



- These auxiliary relationships, including that of the turbulence eddy viscosity, can be derived using dimensional analysis.

# A peek to the turbulence closure problem and some correlations

## Turbulence modeling – Governing equations

- If you check the dimensions of the previous auxiliary relationships, you will confirm that the base dimensions match.

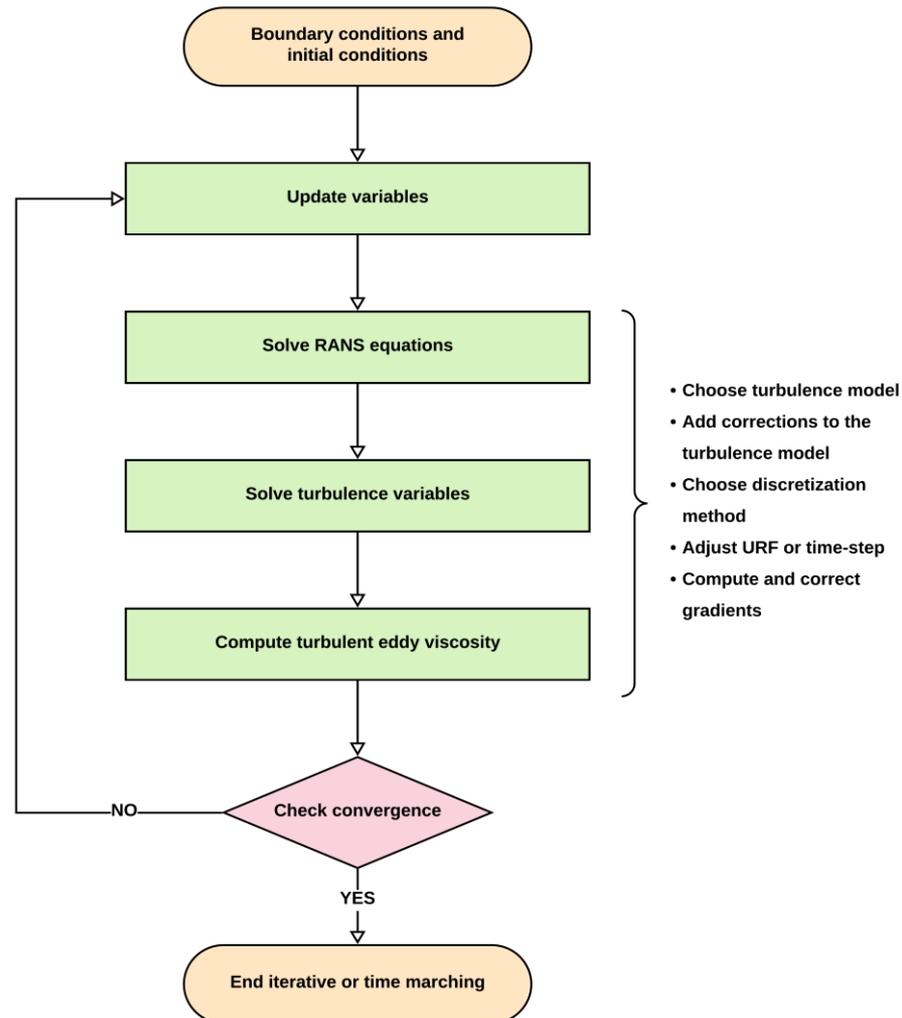
Derived quantity	Symbol	Dimensional units	SI units
Density	$\rho$	$ML^{-3}$	$kg/m^3$
Kinematic viscosity	$\nu$	$L^2T^{-1}$	$m^2/s$
Dynamic viscosity	$\mu$	$ML^{-1}T^{-1}$	$kg/m\cdot s$
Turbulence dissipation rate	$\epsilon$	$L^2T^{-3}$	$m^2/s^3$
Turbulent kinetic energy	$k$	$L^2T^{-2}$	$m^2/s^2$
Specific turbulence dissipation rate	$\omega$	$T^{-1}$	$1/s$

- However, we should always be aware that while dimensional analysis is extremely useful, it unveils nothing about the physics underlying its implied relationships.
- The physics is in the choice of the variables and the correctness of the hypotheses taken.

# A peek to the turbulence closure problem and some correlations

## A naïve CFD loop for turbulence modeling

- The first step consist in defining the boundary and initial conditions of all variables. Including the variables related to the turbulence model.
- The loop will solve first the RANS equations.
- Then, it will move to the next step, where it solves the equations of the turbulence model using the mean values of the RANS equations.
- It will then compute the turbulent eddy viscosity.
- Different turbulent models will compute the eddy viscosity in different ways.
- At this point, it will check the convergence.
- If it is necessary to keep iterating, it will update the variables and it will do another sweep.



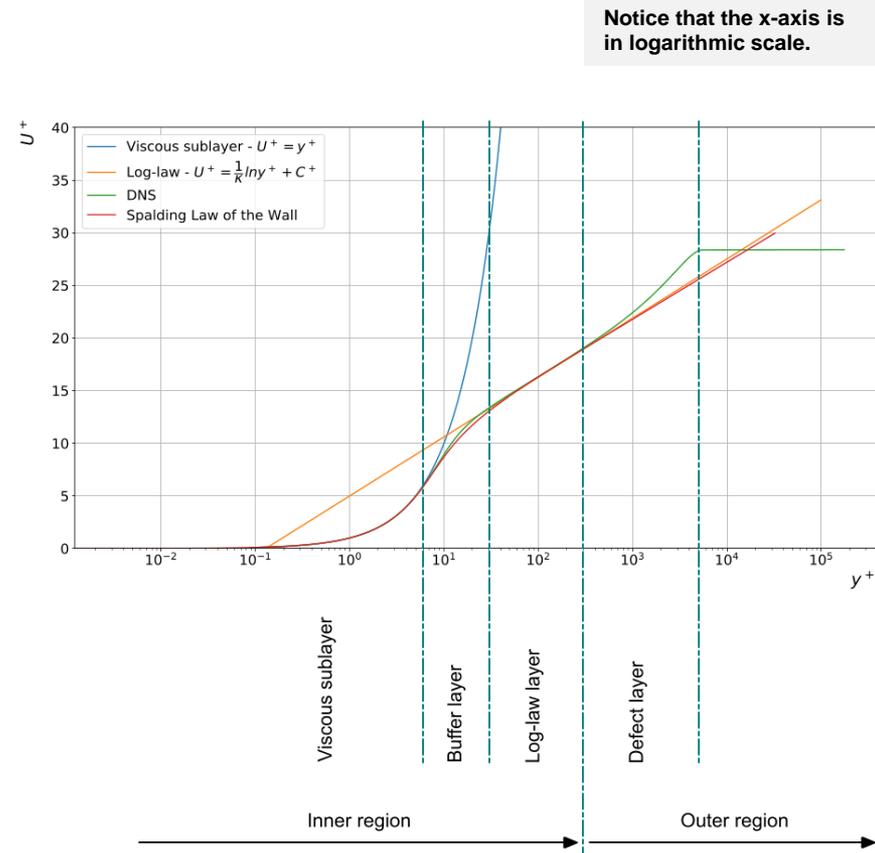
# A peek to the turbulence closure problem and some correlations

## Turbulence near the wall – Law of the wall

- Let us briefly explore the following plot.
- We will talk a lot about this plot later.
- In the plot,  $U^+$  and  $y^+$  are non-dimensional quantities that we will define later.
- The law of the wall, is one of the most famous empirically determined relationships in turbulent flows near solid boundaries.

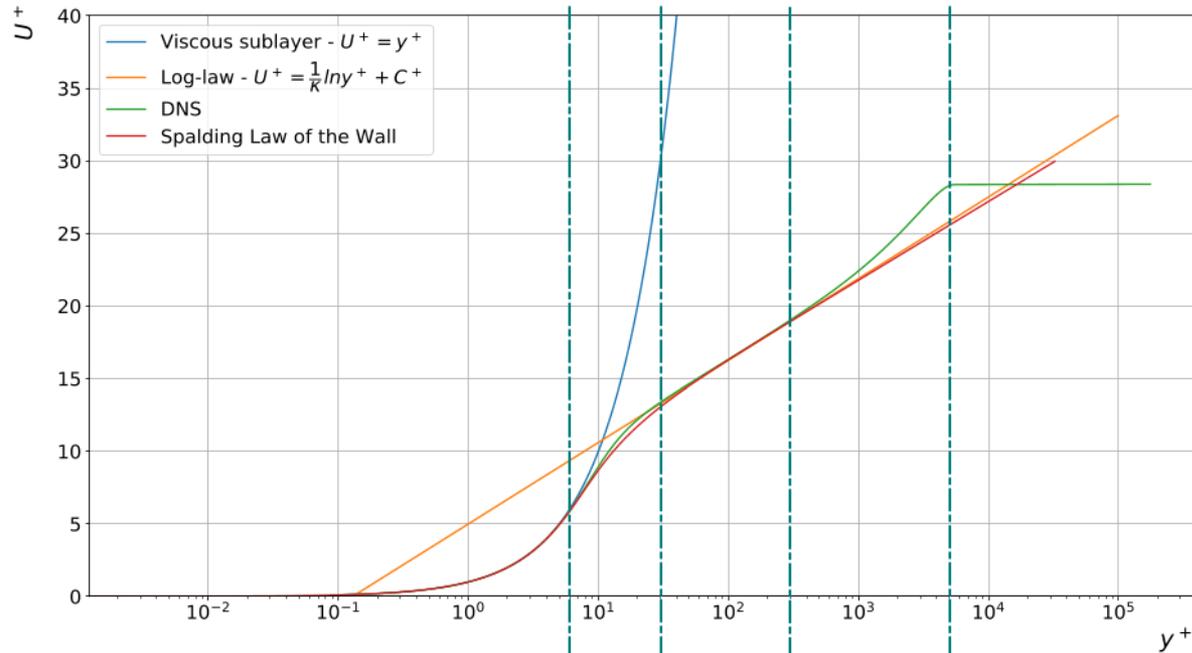
$$U^+ = f_w(y^+)$$

- In the viscous sublayer, the streamwise velocity varies linearly.
- And in the log-law layer, the streamwise velocity varies logarithmically.
- This behavior has been measured in experiments and numerical simulations, for both, internal and external flows.
- Note that the x-axis is in logarithmic scale.



# A peek to the turbulence closure problem and some correlations

## Turbulence near the wall – Law of the wall



Note that the x-axis is in logarithmic scale.

Viscous sublayer

Buffer layer

Log-law layer

Defect layer

Inner region

Outer region

Viscous sublayer

$$y^+ < 5$$

$$u^+ = y^+$$

Buffer layer

$$5 < y^+ < 30$$

$$u^+ \neq y^+$$

$$u^+ \neq \frac{1}{\kappa} \ln y^+ + C^+$$

Log-law layer

$$30 < y^+ < 300$$

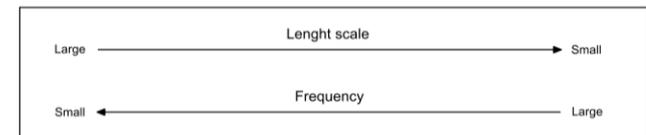
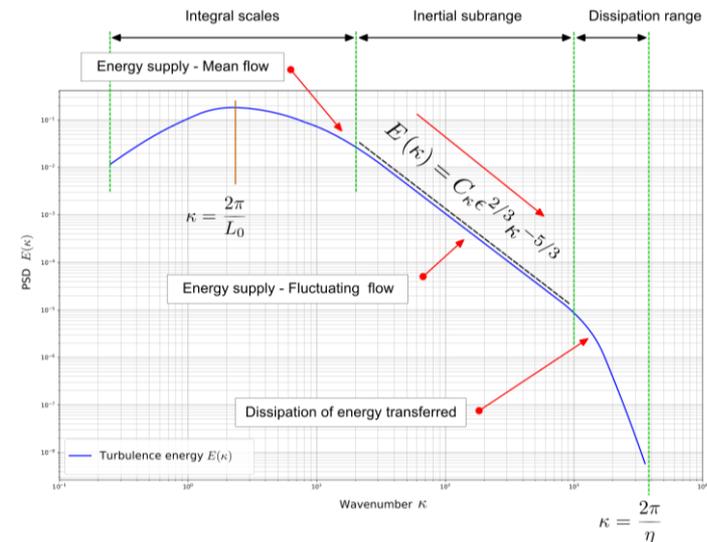
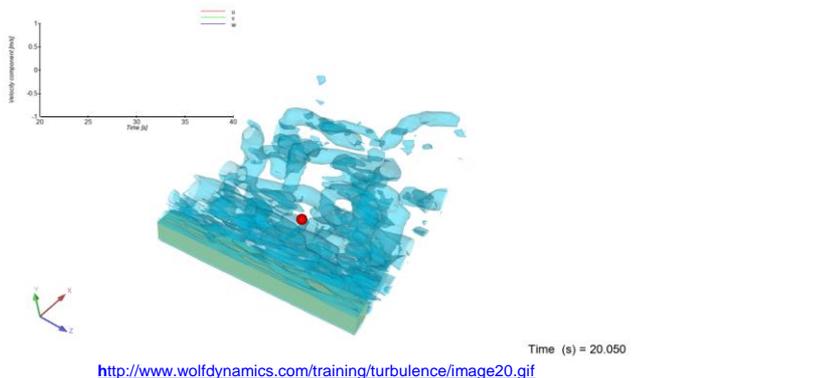
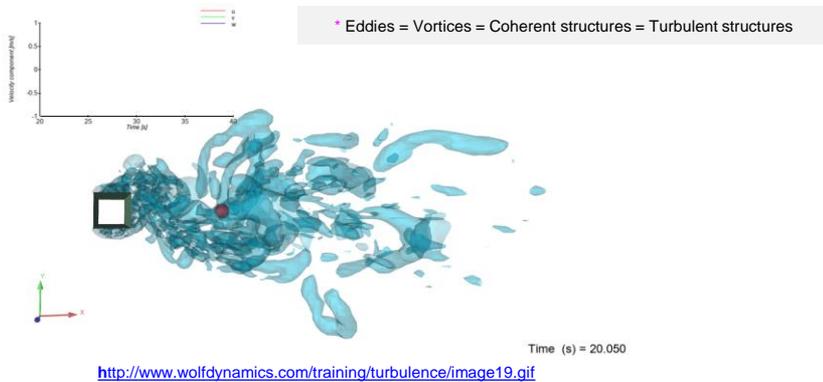
$$u^+ = \frac{1}{\kappa} \ln y^+ + C^+$$

$\kappa$  and  $C^+$  are empirical constants

# A peek to the turbulence closure problem and some correlations

## The turbulence kinetic energy spectrum

- Let us briefly explore the energy cascade and the universal equilibrium theory of turbulence (K41).
- These concepts are related to the energy spectrum of the turbulent kinetic energy or TKE (more on TKE later).
- The turbulent power spectrum or energy spectrum (right figure) represents the distribution of TKE across the various length scales or frequencies, measured in a location in space (red point in the left figure).
- In other words, it represent the energy contained in the eddies\*.

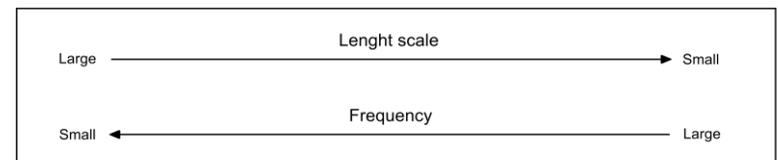
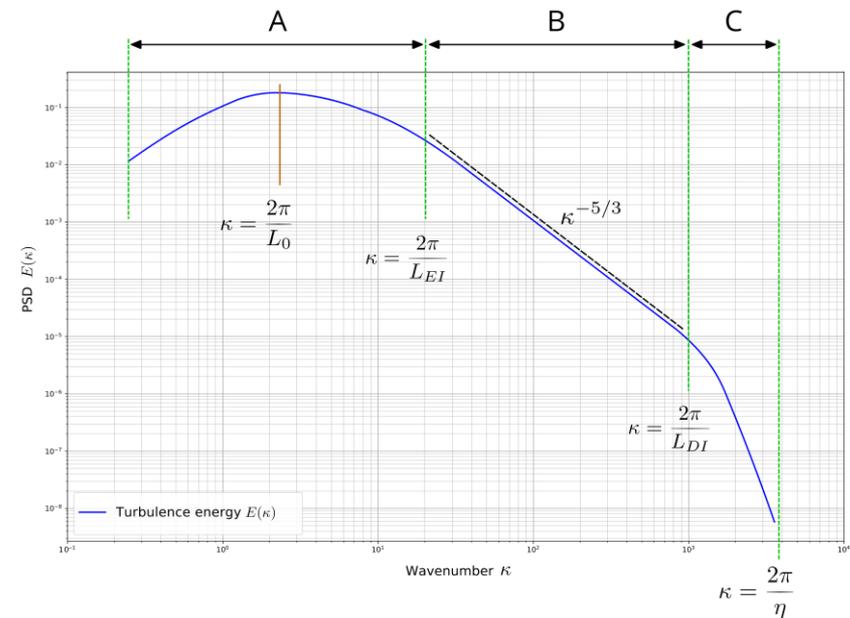
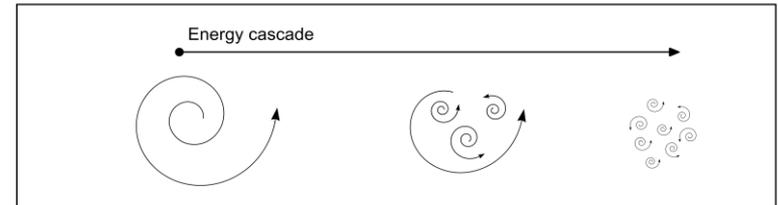


# A peek to the turbulence closure problem and some correlations

## The turbulence kinetic energy spectrum

- Let us briefly explore the energy cascade and the universal equilibrium theory of turbulence (K41).
- The energy cascade process consists in the energy transfer from the largest eddies (region A in the figure) down to the smallest eddies (region C in the figure), where turbulence kinetic energy is dissipated.
- According to the K41 theory (more on this later), there is a range of eddy sizes between the largest and smallest (region B in the figure) for which the cascade process is independent of the statistics of the energy containing eddies and of the effect of viscosity.
- As a consequence, a range of wavenumbers exists in which the energy is transferred by inertial effects (region B in the figure), wherefore  $E(\kappa)$  depends only upon  $\epsilon$  (dissipation) and  $\kappa$  (wavenumber),

$$E(\kappa) = C_K \epsilon^{2/3} \kappa^{-5/3}$$



# A peek to the turbulence closure problem and some correlations

## The turbulence kinetic energy spectrum

- This relationship is sometimes known as the -5/3 law because the slope of the inertial sub-range (region B in the figure) is equal to -5/3.
- The existence of this inertial sub-range has been verified by many physical experiments and numerical simulations.
- The energy spectrum equation  $E(\kappa)$  is fundamental in turbulence modeling.
- The turbulent power spectrum represents the distribution of the turbulent kinetic energy across the various length scales.
- It is a direct indication of how energy is dissipated with eddies size.
- In CFD, the mesh resolution determines the fraction of the energy spectrum directly resolved.
- In scale-resolving simulations, the slope of the spectrum in the inertial sub-range should be properly captured (-5/3).

