Turbulence and CFD models: Theory and applications
Roadmap to Lecture 9

1. Favre averaging
2. Wall functions for heat transfer
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4. Surface roughness
5. Non-linear eddy viscosity models
1. Favre averaging
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When dealing with compressible flows (or variable density flows), besides the velocity and pressure fluctuations, we must also account for density and temperature fluctuations. If we use the Reynolds decomposition and time-averaging additional fluctuating correlations arise. To illustrate this, let us consider the conservation of mass equations for a compressible flow,

\[ \frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0 \]

Now, let us use the Reynolds decomposition for the primitive variables (density and velocity),

\[ \phi(x, t) = \bar{\phi}(x) + \phi'(x, t) \quad \text{or} \quad \phi(x, t) = \bar{\phi}(x, t) + \phi'(x, t) \]
Favre averaging

- Substituting the Reynolds decomposition into the continuity equation yields,

\[
\frac{\partial (\bar{\rho} + \rho')}{\partial t} + \nabla \cdot (\bar{\rho} \mathbf{u} + \rho' \mathbf{u} + \bar{\rho} \mathbf{u}' + \rho' \mathbf{u}') = 0
\]

- By time averaging the previous equation and using the Reynolds averaging rules, we arrive to the Reynolds-averaged continuity equation for compressible flows,

\[
\frac{\partial (\bar{\rho})}{\partial t} + \nabla \cdot (\bar{\rho} \mathbf{u} + \rho' \mathbf{u}') = 0
\]

- To achieve closure, we need to somehow approximate the correlation between the fluctuating quantities \((\rho' \mathbf{u}')\).

- The situation is more complicated for the momentum and energy equations, where triple correlations involving the density fluctuations appear.
Favre averaging

• To simplify the problem, we introduce the density-weighted averaging procedure suggested by Favre [1].

• That is, we introduce the mass-weighted average of the quantity $\phi$, as follows,

$$\bar{\phi} = \lim_{T \to \infty} \frac{1}{T} \int_{t}^{t+T} \rho(x, t) \phi(x, t) dt = \frac{\rho \phi}{\bar{\rho}}$$

• For example, the mass-weighted average of the velocity field is given as follows,

$$\bar{\mathbf{u}} = \frac{\rho \mathbf{u}}{\bar{\rho}}$$

• In our notation, the overbar denotes Reynolds averaging and the tilde denotes Favre averaging.

• If we expand the RHS of equation 1 (that is, we substitute the Reynolds decomposition and use the Reynolds averaging rules), we obtain,

$$\bar{\rho} \bar{\mathbf{u}} = \bar{\rho} \mathbf{u} + \rho' \mathbf{u}'$$

Favre averaging

- If we substitute the following relation,

\[ \bar{\rho} \bar{u} = \bar{\rho} \bar{u} + \rho' u' \]

- Into the Reynolds averaged compressible continuity equation,

\[ \frac{\partial (\bar{\rho})}{\partial t} + \nabla \cdot (\bar{\rho} \bar{u} + \rho' u') = 0 \]

- We obtain the following equation,

\[ \frac{\partial (\bar{\rho})}{\partial t} + \nabla \cdot (\bar{\rho} \bar{u}) = 0 \]

- This is the Favre averaged compressible continuity equation.

- Which looks very similar to the incompressible Reynolds averaged equations.

- As for the Reynolds averaged equations, we simply eliminated the correlation of the fluctuating quantities.

- We can proceed in a similar fashion for the momentum and energy equations.
Favre averaging

- Like the Reynolds decomposition, we can introduce a Favre decomposition of the variable $\phi$, as follows,

$$\phi = \tilde{\phi} + \phi''$$

- And to form a Favre average, we simply multiply by the density and do time average (in the same way as in Reynolds average),

$$\rho \phi = \bar{\rho} \tilde{\phi} + \rho \phi''$$

- And recall that the mass-weighted average of the field $\phi$ is given as follows,

$$\tilde{\phi} = \frac{\rho \phi}{\bar{\rho}}$$

- It is important to mention that density and pressure are not mass-weighted averaged.
- For density and pressure, we use Reynolds averaging (that is, Reynolds decomposition).
- The rest of the field variables can be mass-weighted averaged, namely, $u$, $v$, $w$, $T$, $h$, $H$, $e$. 

Notice that this fluctuating quantity also includes the effects of density fluctuations.
Favre averaging

At this point, the rules of Favre averaging are summarized as follows,

\[ \bar{\phi} = \tilde{\phi} \]

\[ \bar{\rho \phi} = \bar{\rho \phi} \]

\[ \bar{\rho \phi''} = 0 \]

\[ \bar{\phi''} = -\frac{\rho' \phi'}{\bar{\rho}} \neq 0 \]

\[ \bar{\rho \phi \psi} = \bar{\rho \phi \psi} + \bar{\rho \phi'' \psi''} \]

\[ \bar{\rho \phi} = \bar{\rho \phi} \]

Plus, the Reynolds averaging rules.

Finally, if the density is constant, \( \tilde{\phi} = \bar{\phi} \) and \( \phi'' = \phi' \), and we recast the incompressible RANS equations.
Favre averaging

- The Favre-averaged governing equations can be written as follows (using index notation),

\[
\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x_i} (\rho \tilde{u}_i) = 0
\]

\[
\frac{\partial \rho \tilde{u}_i}{\partial t} + \frac{\partial (\rho \tilde{u}_j \tilde{u}_i)}{\partial x_j} = -\frac{\partial P}{\partial x_i} + \frac{\partial}{\partial x_j} \left[ \tau_{ji} - \frac{\rho u''_j u''_i}{2} \right]
\]

\[
\frac{\partial}{\partial t} \left[ \tilde{\rho} \left( \tilde{e} + \frac{\tilde{u}_i \tilde{u}_i}{2} \right) + \frac{\rho u''_i u''_i}{2} \right] + \frac{\partial}{\partial x_j} \left[ \rho \tilde{u}_j \left( \tilde{h} + \frac{\tilde{u}_i \tilde{u}_i}{2} \right) + \tilde{u}_j \frac{\rho u''_i u''_i}{2} \right] =
\]

\[
\frac{\partial}{\partial x_j} \left[ -q_{Lj} - \rho u''_j h'' + \tau_{ji} u''_j - \rho u''_j \frac{1}{2} u''_i u''_i \right] + \frac{\partial}{\partial x_j} \left[ \tilde{u}_i \left( \tilde{\tau}_{ij} - \frac{\rho u''_i u''_j}{2} \right) \right]
\]

\[ P = \tilde{\rho} R \tilde{T} \]

- These are the exact FANS equations (Favre-averaged Navier-Stokes).
- As for the RANS equations, we need to add approximations to derive the solvable equations.
Favre averaging

- Let us review the most commonly used approximations for compressible flows.
  - The Reynolds-Stress tensor (or Favre-Stress tensor), can be modeled as follows,

\[
\bar{\rho} \tau_{i,j}^F = -\bar{\rho} u''_i u''_i = \mu_T \left( \frac{\partial \tilde{u}_i}{\partial x_j} + \frac{\partial \tilde{u}_j}{\partial x_i} - \frac{2}{3} \frac{\partial \tilde{u}_k}{\partial x_k} \delta_{ij} \right) - \frac{2}{3} \bar{\rho} k \delta_{ij}
\]

- This is the Boussinesq assumption but formulated for compressible flows.
Favre averaging

- Let us review the most commonly used approximations for compressible flows.
  - Turbulent heat-flux vector,

\[ q_{Tj} = \rho u_j'' h'' = -\frac{\mu_T c_p}{Pr_T} \frac{\partial \tilde{T}}{\partial x_j} = -\frac{\mu_T}{Pr_T} \frac{\partial \tilde{h}}{\partial x_j} \]

- Molecular diffusion and turbulent transport,

\[ \frac{\tau_{ji} u_i''}{\mu} - \rho u_j'' \frac{1}{2} u_i'' u_i'' = \left( \mu + \frac{\mu_T}{\sigma_k} \right) \frac{\partial k}{\partial x_j} \]

- These two terms are modeled using the gradient diffusion hypothesis.
Favre averaging

- It is important to mention that for compressible flows, the non-zero divergence of the Favre averaged velocity modifies the mean strain rate term in the RHS of the Reynolds-Stress tensor.

- Therefore, the Reynolds-Stress tensor is manipulated in such a way to guarantee that its trace is equal to $-2k$.

- This implies that the second eddy viscosity is equal to,

  \[ \frac{2}{3} \mu_T \]

- The turbulent kinetic energy can be computed as follows,

  \[ \bar{\rho}k = \frac{1}{2} \rho u''u'' \]

- The viscous stress tensor $\tau_{ij}$ and the molecular heat flux $q_L$ (or laminar) are computed as follows,

  \[ \tau_{ij} = \mu \left( \frac{\partial \tilde{u}_i}{\partial x_j} + \frac{\partial \tilde{u}_j}{\partial x_i} \right) - \frac{2}{3} \mu \frac{\partial \tilde{u}_k}{\partial x_k} \delta_{ij} \]
  \[ q_L = -\kappa \frac{\partial \tilde{T}}{\partial x_j} \]
Favre averaging

- As it can be seen, the Favre averaging is very similar to the Reynolds averaging.
- To derive the solvable equations, we must approximate all the terms that involve correlations of fluctuating quantities.
- Similar to the incompressible equations, we can derive the exact transport equations for the turbulent kinetic energy and Reynolds stresses.
- Favre averaging is used for compressible flows, mixture of gases, species concentration, and combustion.
- Favre averaging eliminates density fluctuations from the averaged equations.
- However, it does not remove the effect the density fluctuations have on the turbulence.
- Favre averaging is a mathematical simplification, not a physical one.
- Remember, when using Favre averaging, the density and pressure are not mass-weighted averaged.
  - For density and pressure, we use Reynolds averaging (that is, Reynolds decomposition).
  - The rest of the field variables can be mass-weighted averaged, namely, $u$, $v$, $w$, $T$, $h$, $H$, $e$. 
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Wall functions for heat transfer

• As for the momentum (or viscous) wall functions, there is also a treatment for the thermal wall functions.
• Depending on the value of $y^*$, the value of the non-dimensional temperature $T^*$ (equivalent to the concept of $u^*$), can be computed as follows,

$$T^* = \begin{cases} 
Pr \; y^* & y^* < 5 \\
Pr_t \left[ \frac{1}{\kappa} \ln (E y^*) + P \right] & y^* > 30
\end{cases}$$

<table>
<thead>
<tr>
<th>Molecular (or laminar) Prandtl number</th>
<th>$Pr$</th>
</tr>
</thead>
<tbody>
<tr>
<td>Turbulent Prandtl number</td>
<td>$Pr_t$</td>
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Thermal viscous sublayer where conduction is important

Logarithmic law for the turbulent region where effects of turbulence dominate conduction
Wall functions for heat transfer

• The following nondimensional temperature relation (in the log-law region),

\[ T^* = Pr \left[ \frac{1}{\kappa} \ln (E y^*) + P \right] \]

• It is used to relate the temperature at the cell center \( T_p \) to the heat flux at the wall \( q_w \).
• This is similar to what we did with the viscous wall function, where we related \( U_p \) to \( \tau_w \).
Wall functions for heat transfer

- When using thermal wall functions, we are interested in computing the thermal diffusivity used to approximate the wall heat transfer $q_w$.

\[
q_w = k \frac{\partial T}{\partial y} = \rho c_p \alpha \frac{\partial T}{\partial y} = \rho c_p \alpha \frac{T_w - T_p}{y_p - y_w}
\]

- We need to relate the temperature at the cell center $T_p$ to the heat flux at the wall $q_w$. 

- $y_p, T_p$
Wall functions for heat transfer

- Recall that in the momentum boundary layer, the velocity at the walls is zero.
- In the thermal boundary layer, the temperature at the wall can be higher or lower than the freestream temperature.
- Therefore, we can have very different temperature profiles growing from the walls.
- The temperature at the walls also has an influence of the wall shear stresses.
Just as there is a viscous boundary layer in the velocity distribution (or momentum), there is also a thermal boundary layer.

Thermal boundary layer thickness is different from the thickness of the viscous sublayer (momentum) and is fluid dependent.

The thickness of the thermal sublayer for a high Prandtl number fluid (e.g., water) is much less than the momentum sublayer thickness.

For fluids of low Prandtl numbers (e.g., air), it is much larger than the momentum sublayer thickness.

For Prandtl number equal 1, the thermal boundary layer is equal to the momentum boundary layer.
Wall functions for heat transfer

- The normalized temperature plot ($T^+$ vs. $y^+$), depends on the Prandtl number.
- Different values of Prandtl number will result in different plots, with different intersection points between the viscous sublayer and the log-law region.
- The intersection point of the viscous sublayer and the log-law region is known as the non-dimensional thermal sublayer thickness or $y_l^*$. 

![Graph showing temperature and normalized thickness](graph.png)

$y_l^* \approx 8.08$

$y_l^* \approx 11.47$
Wall functions for heat transfer

- The thermal diffusivity coefficient \( \alpha \) is computed as follows,

\[
\alpha_w = \begin{cases} 
\alpha & y^* < y_l^* \\
\frac{u_\tau y_p}{Pr_t \left[ \frac{1}{\kappa} \ln (Ey^*) + P \right]} & y^* > y_l^*
\end{cases}
\]

- Remember, the value of \( y_l^* \) depends on the Prandtl number.
- At this point, the heat flux \( q_w \) at the wall can be computed as follows,

\[
q_w = \rho c_p \alpha_w \frac{T_w - T_p}{y_p - y_w}
\]

- The turbulent Prandtl number \( Pr_t \) is usually equal to 0.85, but it highly depends on the flow properties and the flow physics.
Wall functions for heat transfer

• Let us revisit the nondimensional temperature function $T^*$,

$$T^* = Pr_t \left[ \frac{1}{\kappa} \ln (Ey^*) + P \right] \quad y^* > 30$$

• The term $P$ appearing in this relation, has a strong dependence on the Prandtl number (molecular and turbulent).

• One way to approximate this term is by using Jayatilleke function [1],

$$P = 9.24 \left[ \left( \frac{Pr}{Pr_t} \right)^{3/4} - 1 \right] \left[ 1 + 0.28e^{-0.007Pr/Pr_t} \right]$$


Wall functions for heat transfer

- Let us summarize the steps needed to compute the wall heat flux $q_w$ using wall functions,
  - Compute $y^*$.
  - Compute the Prandtl number,
    \[ Pr = \frac{\nu}{\alpha} \]
  - Compute the intersection point $y_i^*$.
  - Compute the thermal diffusivity at the wall.
    \[ \alpha_w = \begin{cases} \alpha & y^* < y_i^* \\ \frac{u_\tau y_p}{Pr_t \left[ \frac{1}{\kappa} ln (E y^*) + P \right]} & y^* > y_i^* \end{cases} \]
  - Compute the heat flux at the wall.
    \[ q_w = \rho c_p \alpha_w \frac{T_w - T_p}{y_p - y_w} \]
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When studying the boundary layer, heat transfer rate, compressibility, pressure gradient, mach number, and surface roughness (among many factors), they all have an effect on the velocity profile.

It is not obvious what effect each of these parameters have on the velocity profile.

Hereafter, we present a few observations or general guidelines (use with care).
Wall functions – Additional observations

- Effect of adverse pressure gradient on the law of the wall.

![Graph showing the effect of pressure gradient on the law of the wall.]

- The boundary layer thickens, and the skin friction decreases as the adverse pressure gradient is increased.
Wall functions – Additional observations

- Effect of compressibility on the law of the wall.

- Increasing compressibility causes the skin friction to decrease.
Wall functions – Additional observations

- Effect of heat transfer on the law of the wall.

Notice that depending on the Prandtl number, the boundary layer can be thicker or thinner.
- A cold wall creates a thinner boundary layer and increases the skin friction
- A hot wall thickens the boundary layer and decreases the skin friction.
Wall functions – Additional observations

- Effect of surface roughness on the law of the wall.

- Surface roughness increases the skin friction.
- It shifts the velocity profile downwards.

![Graph showing the effect of surface roughness on the law of the wall](image)

The graph illustrates the effect of surface roughness on the law of the wall. The log-law, $U^+ = \frac{1}{K} \ln y^+ + C^+$, is shown, where $U^+$ is the friction velocity and $y^+$ is the normalized distance from the wall. Increasing surface roughness is indicated by the green line, which deviates from the log-law line, showing an increase in skin friction.
Wall functions – Additional observations

- When dealing with high-speed flows and heat transfer, the coefficients appearing in the law of the wall relations and closure relations, have a strong dependence on the Mach number and the heat transfer rate.

- No need to mention that the physical properties also depend on the Mach number and heat transfer rate.

\[
u^* = \begin{cases} 
  y^* & y^* < 11.225 \\
  \frac{1}{\kappa} \ln (y^*) + C & y^* > 11.225
\end{cases}
\]

\[
T^* = \begin{cases} 
  Pr y^* & y^* < 5 \\
  Pr_t \left[ \frac{1}{\kappa} \ln (E y^*) + P \right] & y^* > 30
\end{cases}
\]

Figure 5.3: Computed and measured velocity profiles for compressible flat-plate boundary layers: — Wilcox (2006) k-\(\omega\); - - - Chien k-\(\varepsilon\); ○ Coles; □ Watson.
Wall functions – Additional observations

- In the case of pressure gradients and flow separation (non-equilibrium conditions), the law of the wall can be sensitized to pressure gradients effects [1].

\[
\frac{\tilde{U}C_{\mu}^{1/4}k^{1/2}}{\frac{\tau_w}{\rho}} = \frac{1}{\kappa} \ln \left( \frac{E\rho C_{\mu}^{1/4}k^{1/2}y}{\mu} \right)
\]

- Where,

\[
\tilde{U} = U - \frac{1}{2} \frac{dp}{dx} \left[ \frac{y_v}{\rho \kappa k^{1/2}} \ln \left( \frac{y}{y_v} \right) + \frac{y - y_v}{\rho \kappa k^{1/2}} + \frac{y_v^2}{\mu} \right]
\]

\[
y_v = \frac{\mu y^*_v}{\rho C_{\mu}^{1/4}k_p^{1/2}} \quad \quad y^*_v = 11.225
\]

- This correction is recommended for use in complex flows involving separation, reattachment, and impingement where the mean flow and turbulence are subjected to pressure gradients and rapid changes.

- In such flows, improvements can be obtained, particularly in the prediction of wall shear (skin-friction coefficient) and heat transfer (Nusselt or Stanton number).

The non-dimensional temperature $T^*$, can be further improved by adding the viscous heating contribution [1],

$$T^* = T_c^* + \frac{D}{q}$$

Where,

$$T_c^* = \begin{cases} Pr y^* & y^* < y_i^* \\ PrT \left[ \frac{1}{\kappa} \ln (Ey^*) + P \right] & y^* > y_i^* \end{cases}$$

$$D = \begin{cases} \rho u^* \frac{1}{2} Pr U_p^2 & y^* < y_i^* \\ \rho u^* \frac{1}{2} \left[ Pr_t U_p^2 + (Pr - Pr_t) U_c^2 \right] & y^* > y_i^* \end{cases}$$

Where $U_c$ is the mean velocity at the intersection point $y_i^*$.

This correction is recommended for highly compressible flows, where heating by viscous dissipation can have a strong influence in the temperature distribution in the near-wall region.

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Surface roughness

- So far, we have only considered smooth walls.
- In reality, every wall and material is characterized by small irregularities, which we refer to as roughness.
- The roughness has a characteristic height $h$, as shown in the figure below.
- Wall roughness increases the wall shear stress and heat transfer rate.

Examples of wall roughness. (a) Surface of an aluminum pipe: $h_{rms} \approx 0.16 \, \mu m$. (b) Scanned surface (1.4 x 1.1 mm$^2$) of a non-rusted commercial steel pipe: $h_{rms} \approx 5 \, \mu m$. (c) Scales of the great white shark: $h_{rms} \approx 0.1 \, mm$. (d) Aerial views of tropical forest in Gabon (h ≈ 0.1-10 m). (d) Barcelona landscape (h ≈ 10-100 m). (f) The Namib desert (h ≈ 10-500 m). Adapted from reference [1].

Surface roughness

- In CFD, the roughness must be modeled.
- In theory, it can be resolved with very fine meshes but the computational requirements are too high.
- Wall roughness increases the wall shear stress and heat transfer rate.
- It also breaks up the viscous sublayer.
- By looking at the nondimensional velocity plot, the wall roughness shifts the nondimensional velocity downwards by a factor of $\Delta B$. 

![Graph showing the effect of wall roughness on nondimensional velocity](image)
Surface roughness

• There are many ways to add roughness to the solution.
• Let us study maybe the most common wall function for roughness.
• This implementation is based on the standard wall functions.

\[ U^+ = \frac{1}{\kappa} \ln (E_y^+) - \Delta B \]

STEP 1.

\[ U^+ = \frac{1}{\kappa} \ln (E_y^+) - \ln (e^{\Delta B}) \]

STEP 2.

\[ U^+ = \frac{1}{\kappa} \ln \left( \frac{E_y^+}{e^{\Delta B}} \right) \]

STEP 3.

• Where we used the following logarithm rules to derive the previous relations,

\[ \ln (e^x) = x \quad \ln (x) - \ln (y) = \ln \left( \frac{x}{y} \right) \]
Surface roughness

- If we introduce the following relation,

\[ E' = \frac{E}{e^{\Delta B}} \]

- Into the relation corrected for wall roughness,

\[ U^+ = \frac{1}{\kappa} \ln \left( \frac{E y^+}{e^{\Delta B}} \right) \]

- We obtain the following equation,

\[ U^+ = \frac{1}{\kappa} \ln \left( E' y^+ \right) \]

- Which is identical to the standard wall function formulation (except for the variable \( E' \)).
- We now have a way to work with smooth and rough walls using the same log-law relation.
Surface roughness

- Let us now address the roughness correction factor $\Delta B$.
- This factor can be computed as follows [1, 2],

$$\Delta B = 0 \quad K_s^+ < 2.25$$

$$\Delta B = \frac{1}{\kappa} \left( \frac{K_s^+ - 2.25}{87.75} + C_s K_s^+ \right) \times \ldots$$

$$\ldots \times \sin \left[ 0.4258 \left( \ln K_s^+ - 0.811 \right) \right] \quad 2.25 < K_s^+ < 90$$

$$\Delta B = \frac{1}{\kappa} \ln \left( 1 + C_s K_s^+ \right) \quad K_s^+ > 90$$

- Notice that $\Delta B$ is a function of the nondimensional roughness height $K_s^+$ and the roughness constant $C_s$.

The hydraulically smooth condition exists when roughness heights are so small that the roughness is buried in the viscous sublayer.

The fully rough flow condition exists when the roughness elements are so large that the sublayer is completely eliminated, and the flow can be considered as independent of molecular viscosity; that is, the velocity shift is proportional to $\ln(K_s^+)$.

The transitional region is characterized by reduced sublayer thickness, which is caused by diminishing effectiveness of wall damping.

Because molecular viscosity still has some role in the transitional region, the geometry of roughness elements has a relatively large effect on the velocity shift.
Surface roughness

- The nondimensional roughness height can be computed as follows,

\[ K_s^+ = \frac{\rho K_s u^*}{\mu} \]

- Where $K_s$ is the typical roughness height (sand grain diameter).
- The roughness constant $C_s$ is often equal to 0.5. This constant represents the shape and distribution of the roughness elements (sand grains).
- It is recommended to fix $C_s$ and adjust $K_s^+$.
- Remember, in our discussion, the roughness regime is subdivided into the three regimes.
  - Hydraulically smooth.
  - Transitional.
  - Fully rough.
Surface roughness

- The subdivision of the roughness regime and the dependence of the constant $C$ (law of the wall) and the roughness correction factor $\Delta B$ are supported on experimental data (Nikuradse’s data [1]).
- The constant $C$ and the roughness correction factor depend on the roughness parameters $K_s^+$ and $C_s$.

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**Figure 1:**

- **Left graph:** Constant in the law of the wall as a function of surface roughness. Based on measurements of Nikuradse [1]. Adapted from [2].
- **Right graph:** Effect of wall roughness on the roughness correction factor and universal velocity profiles [3].

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Surface roughness

- Plots of mean velocity distribution for uniform roughness at several $K_s^+$ values.

Plots of mean velocity distribution for uniform roughness at several values of nondimensional roughness height [1].

Plot of roughness mean velocity profiles [2].

Surface roughness

- There is no universal roughness function valid for all types of roughness.
- Many methods to take into account the surface roughness are available in the literature, just to name a few,

Surface roughness

- Finally, as we have seen, a rough wall increases friction.
- But it happens that special rough surfaces can increase drag reduction.
- Well designed riblets can shift the nondimensional velocity profile upwards, and closer to the viscous law nondimensional profile.
- It appears that small riblets that are aligned with the flow direction can achieve a significant drag reduction up to 10%.
- The maximum drag reduction occurs for a rib spacing $s$ between 14 and 20 viscous wall units, i.e., $14 < s^+ < 20$, as illustrated in the figure.
- This is an example of biomimetics, since the development and application of ribbed surfaces has been inspired by the presence of ribbed scales on sharks.

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Besides using riblets for drag reduction, a similar effect can be achieved by polymer additives.

Small amounts of certain polymer additives to fluids can achieve a significant reduction of friction drag, which is known as the Toms effect [1, 2, 3].

The figure below shows experimental data of the measured velocity profiles for various flows with polymer additives.

- The profiles for drag-reducing flows have logarithmic profiles with the same slope as for a Newtonian fluid, but with an offset, or effective slip.

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Non-linear eddy viscosity models

• One approach to achieving a more appropriate description of the Reynolds-stress tensor without introducing any additional transport equations (as in the RSM models) is to add extra high order terms to the Boussinesq approximation.

\[ \rho u_i' u_j' = \frac{2}{3} \rho k \delta_{ij} - 2 \mu_t S_{ij} + f(S_{ij}, \Omega_{ij}) \]

• Where \( f(S_{ij}, \Omega_{ij}) \) is a nonlinear function dependent on the mean strain rate \( S_{ij} \) tensor and spin tensor (rotation) \( \Omega_{ij} \).

• Recall that the mean strain rate tensor and spin tensor are defined as follows,

\[ S_{ij} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \quad \Omega_{ij} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} - \frac{\partial u_j}{\partial x_i} \right) \]

• These models are known as nonlinear eddy viscosity models (NLEVM).

• This idea was originally proposed by Lumley [1,2], and many NLEVM has been proposed since then.

Non-linear eddy viscosity models

- The NLEVM approach can be seen as a remedy to the deficiencies of the EVM.
- Where the main deficiencies of the EVM are:
  - Inability to properly describe the anisotropic behavior in shear layers. In the EVM the normal stresses are isotropic, $u'^2 = v'^2 = w'^2 = (2/3)k$.
  - Flow in ducts with secondary motions.
  - Overpredicting production of turbulent kinetic energy in stagnation points.
  - Failure to reproduce the asymmetric behavior of the velocity profiles in the presence of streamlined geometries (strong curvature).
  - Underpredicting turbulent viscosity in the presence of system rotation (strong vortices).
- In comparison to the EVM, the NLEVM models are more computational expensive (as they need to solve more terms and are wall resolving).
- They are also harder to convergence.
- However, they do offer improved prediction capabilities for certain complex turbulent flows.
- Despite the many apparent advantages of NLEVM, they are not widely used.
- EVM still are the workhorse of turbulence modeling.
Non-linear eddy viscosity models

- The NLEVM are usually quadratic or cubic.
- Let us briefly discussed the NLEVM by Shih et al [1], which is cubic.
- In this model, the Reynolds stresses are computed as follows,

$$-\rho u'_i u'_j = -\frac{2}{3} \rho k \delta_{ij} + \mu_t 2 S^*_{ij} + A_3 \frac{\rho k^3}{\varepsilon^2} \left[ \bar{S}_{ik} \bar{\Omega}_{kj} - \bar{\Omega}_{ik} \bar{S}_{kj} \right]$$

$$-2A_5 \frac{\rho k^4}{\varepsilon^3} \left[ \bar{\Omega}_{ik} \bar{S}_{kj}^2 - \bar{S}_{ik} \bar{\Omega}_{kj} + \bar{\Omega}_{ik} \bar{S}_{km} \bar{\Omega}_{mj} - \frac{1}{3} \bar{\Omega}_{kl} \bar{S}_{lm} \bar{\Omega}_{mk} \delta_{ij} + I_s S^*_{ij} \right]$$

- Where $I_s$, $S^*_{ij}$, and $S^2_{ij}$ are given by the following relationships,

$$I_s = \frac{1}{2} \left[ \bar{S}_{kk} \bar{S}_{mm} - \bar{S}_{kk}^2 \right] \quad S^*_{ij} = \bar{S}_{ij} - \frac{1}{3} \bar{S}_{kk} \delta_{ij} \quad S^2_{ij} = S_{ik} S_{kj}$$

Non-linear eddy viscosity models

• This model is particularly suited for swirling flows.
• It was developed to deal with aircraft engine combustors that generally involve turbulent swirling flows in order to enhance fuel-air mixing and flame stabilization.
• The model includes third order terms, so it offers extra accuracy.
• The method also satisfy the constraints of rapid distortion theory (RDT) and realizability.
• All the coefficients appearing in the nonlinear constitutive equation are calibrated using DNS and experimental data.
• The coefficient $C_{\mu}$ is not constant, it depends on the strain rate tensor.
• The value of the turbulent kinetic energy $k$ and the dissipation rate $\epsilon$ are obtained from low-RE $k - \epsilon$ turbulence models (wall resolving).
• Also, the value of the turbulent eddy viscosity is computed using the relations from low-RE $k - \epsilon$ turbulence models.